



An innovative and climate protective waste treatment system



The Herhof Dry Stabilat Process





Advantages of the Herhof technology

- Waste to energy
- No waste material for landfilling
- Biological drying increases calorific value
- Separation of waste into material for energy recovery and material recovery
- 50% of input material transferred into secondary fuel
- Secondary fuel has 2/3 of organic material
- CO₂ savings for 2/3 of the output material (Stabilat)

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Herhof Stabilat® plants:

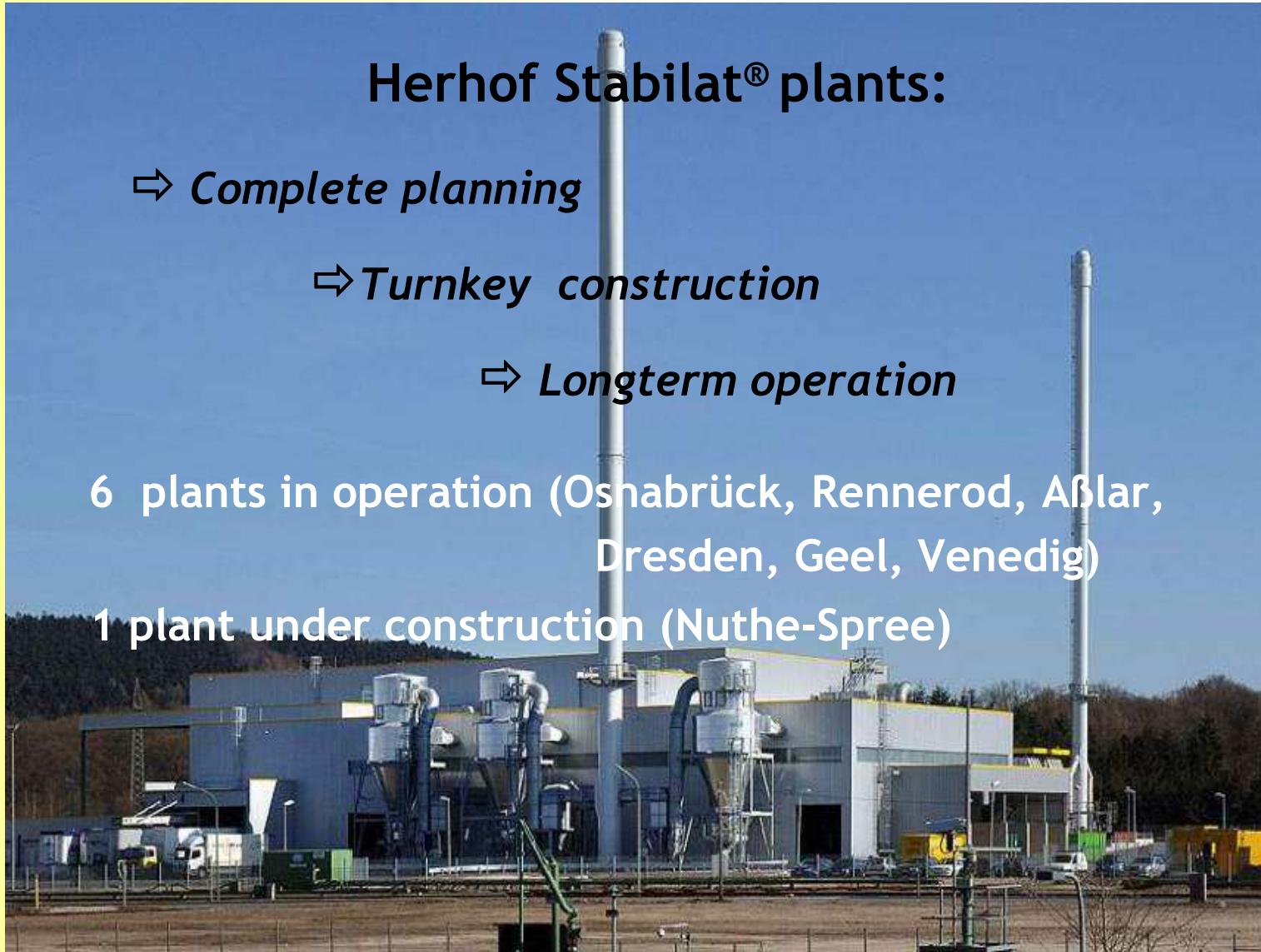
⇒ *Complete planning*

⇒ *Turnkey construction*

⇒ *Longterm operation*

6 plants in operation (Osnabrück, Rennerod, Aßlar,
Dresden, Geel, Venedig)

1 plant under construction (Nuthe-Spree)



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Stabilat® technology - Using MSW as a resource



Material Recovery



Energy Recovery



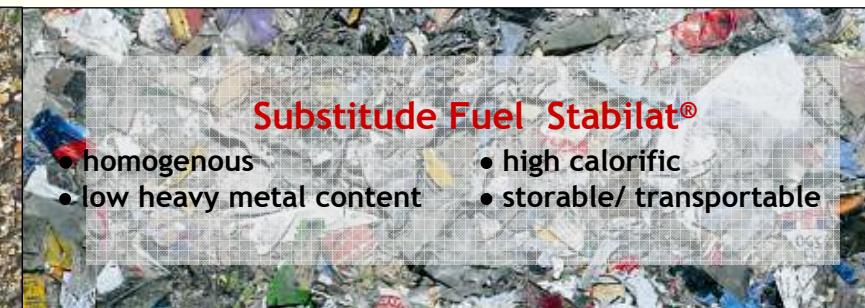
Condensate / Permeate
30%



Metals
Fe NF*
4 % 1%



Inerts/ Glass
12%
Batteries / Electronic scrap



Substitute Fuel Stabilat®

- homogenous
- low heavy metal content

- high calorific
- storable/ transportable

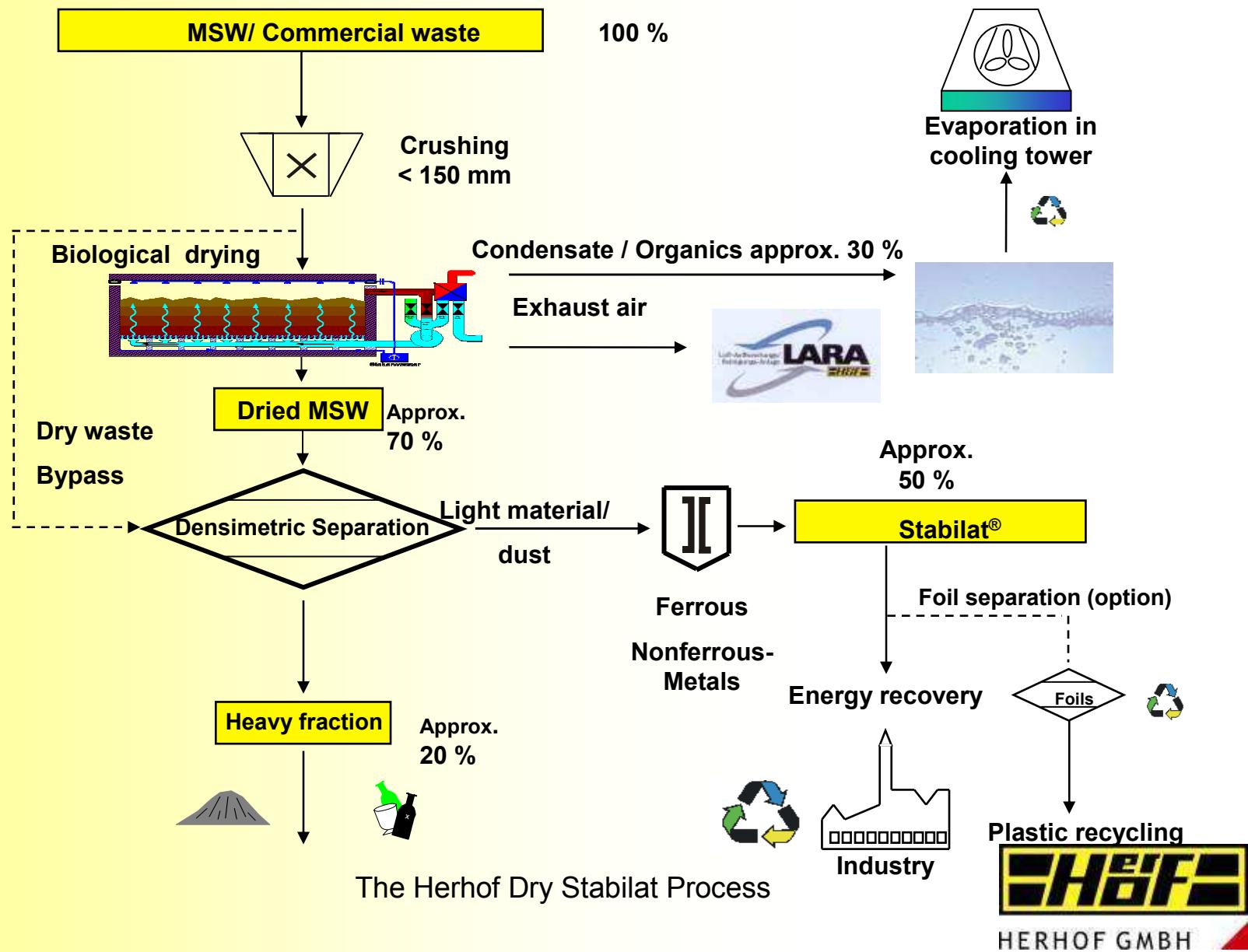
Stabilat®
53%

NF* = Nonferrous

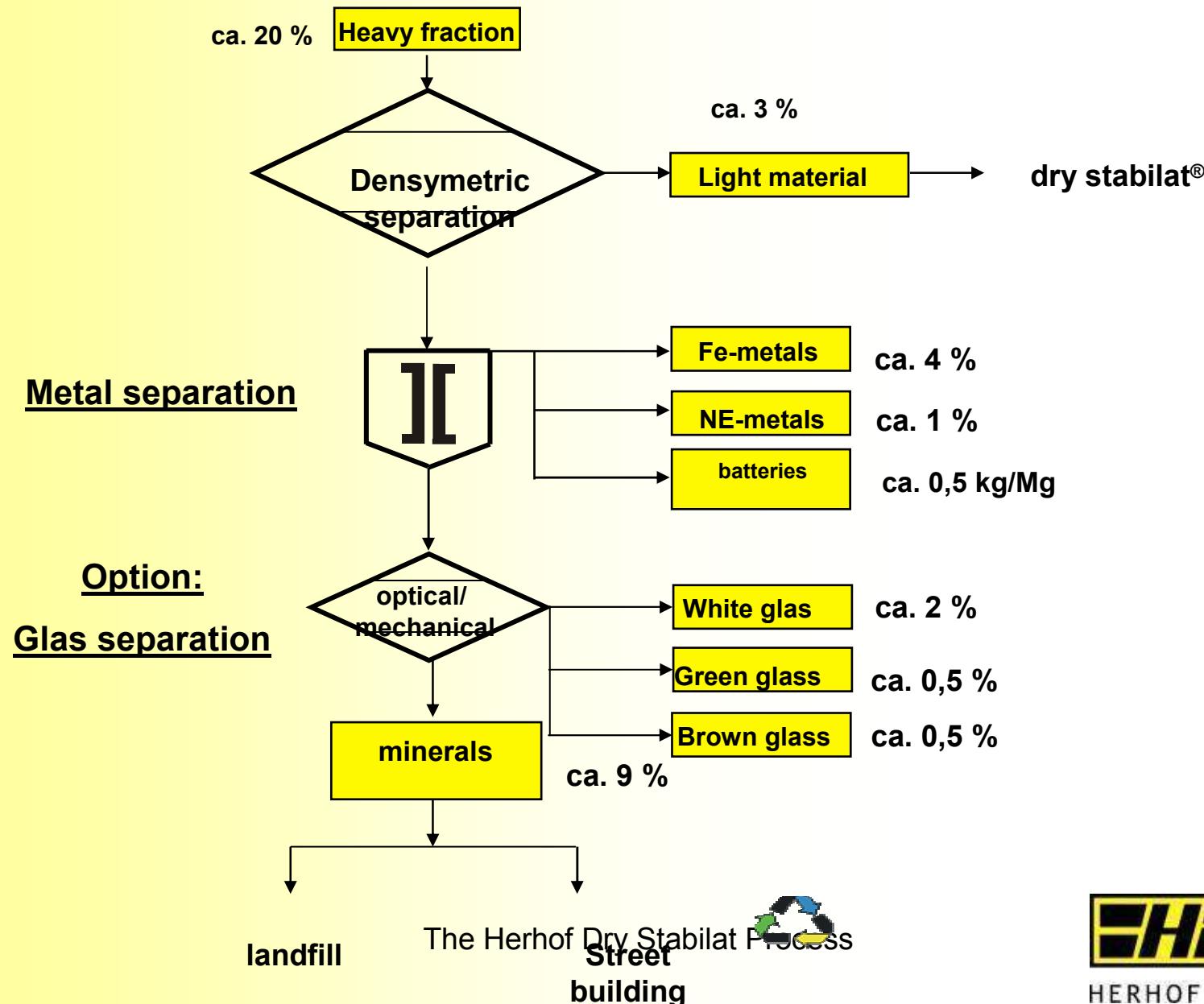
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Herhof Stabilat® Technology

- with glass separation -



Separation of the heavy fraction





View of a plant (MBS Osnabrück)

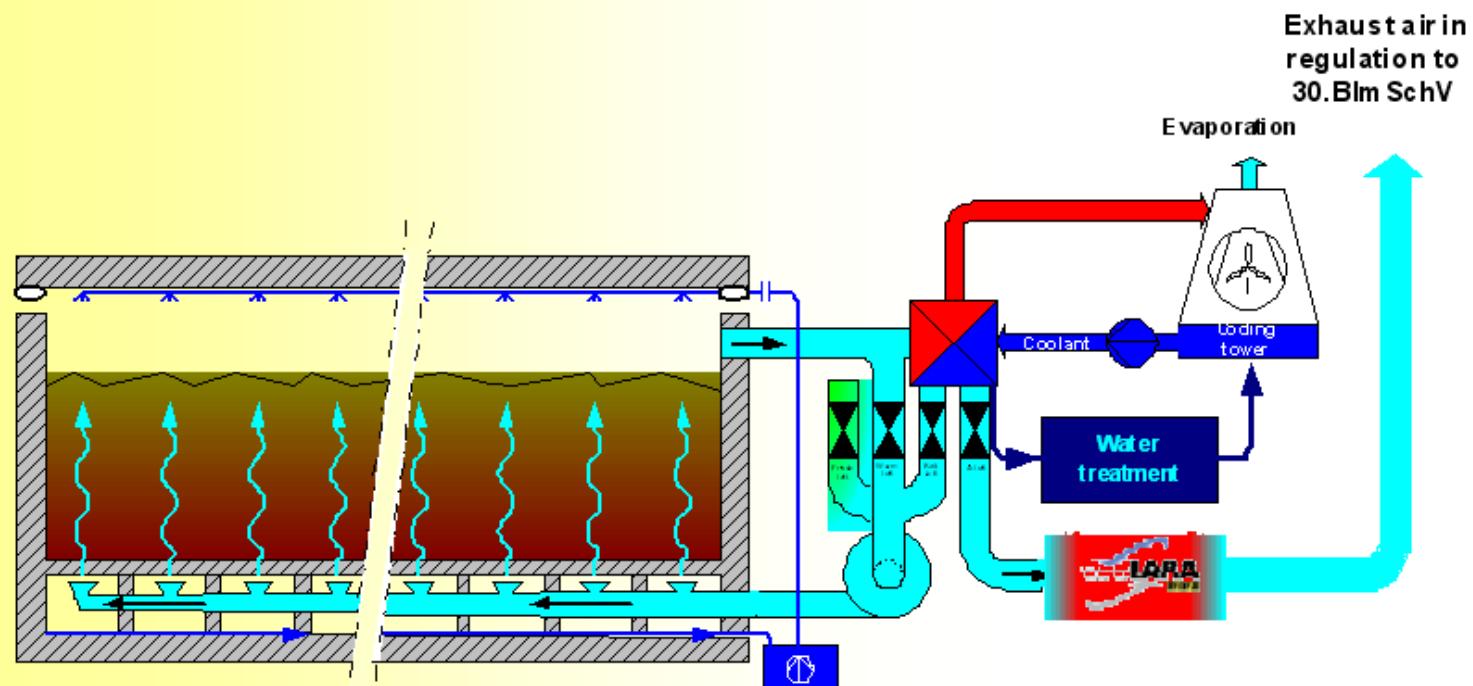


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Composting boxes

Composting / Biological drying process with the Herhof composting box



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Herhof box with process crane



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Ventilation corridor



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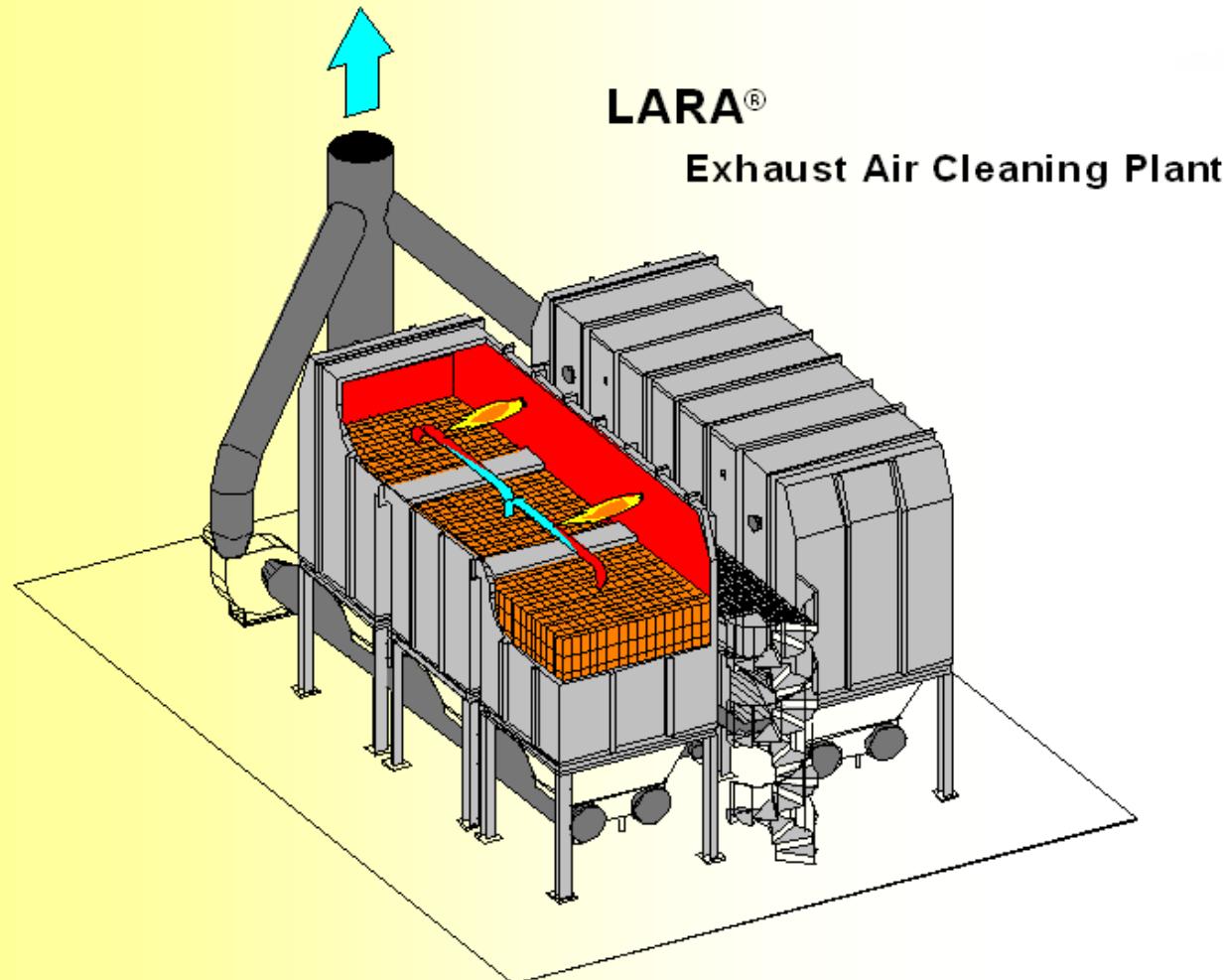


Condensate cleaning



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Exhaust air cleaning



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LARA air cleaning



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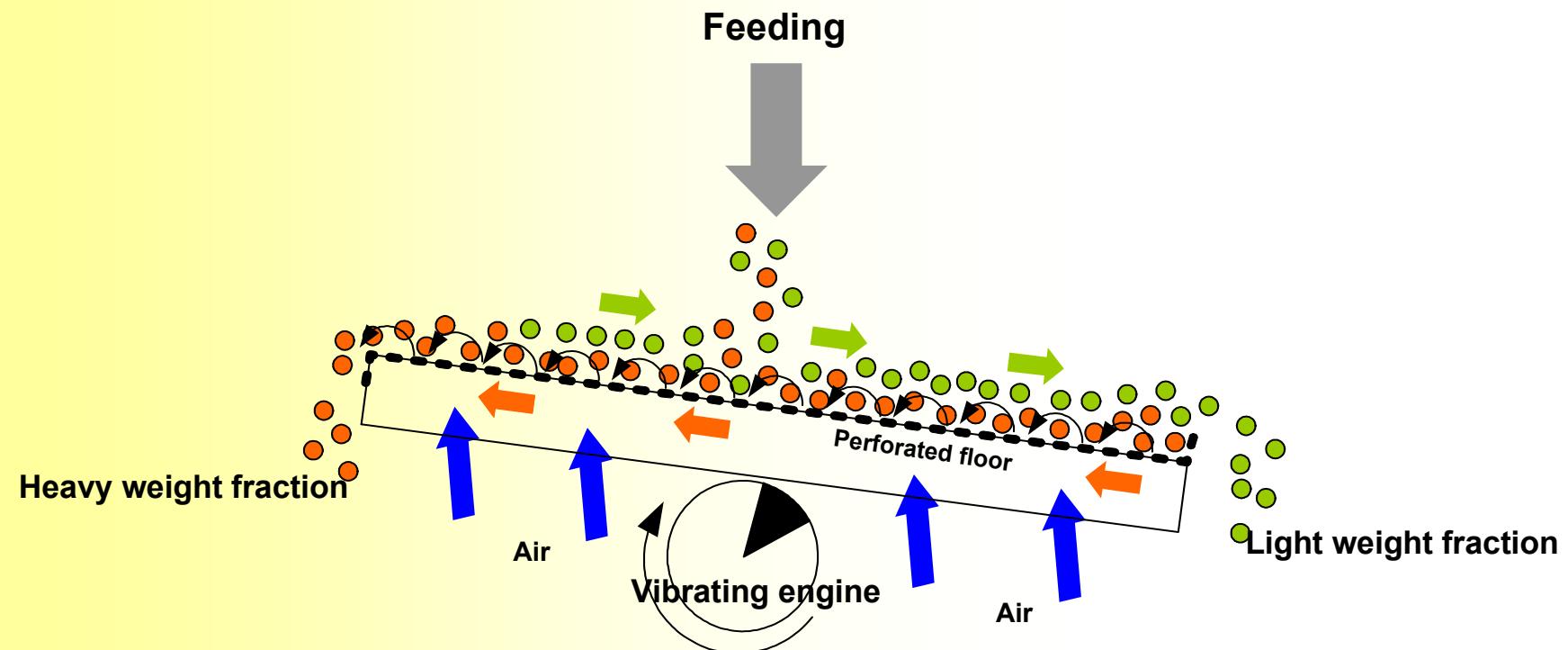
Machinery Hall



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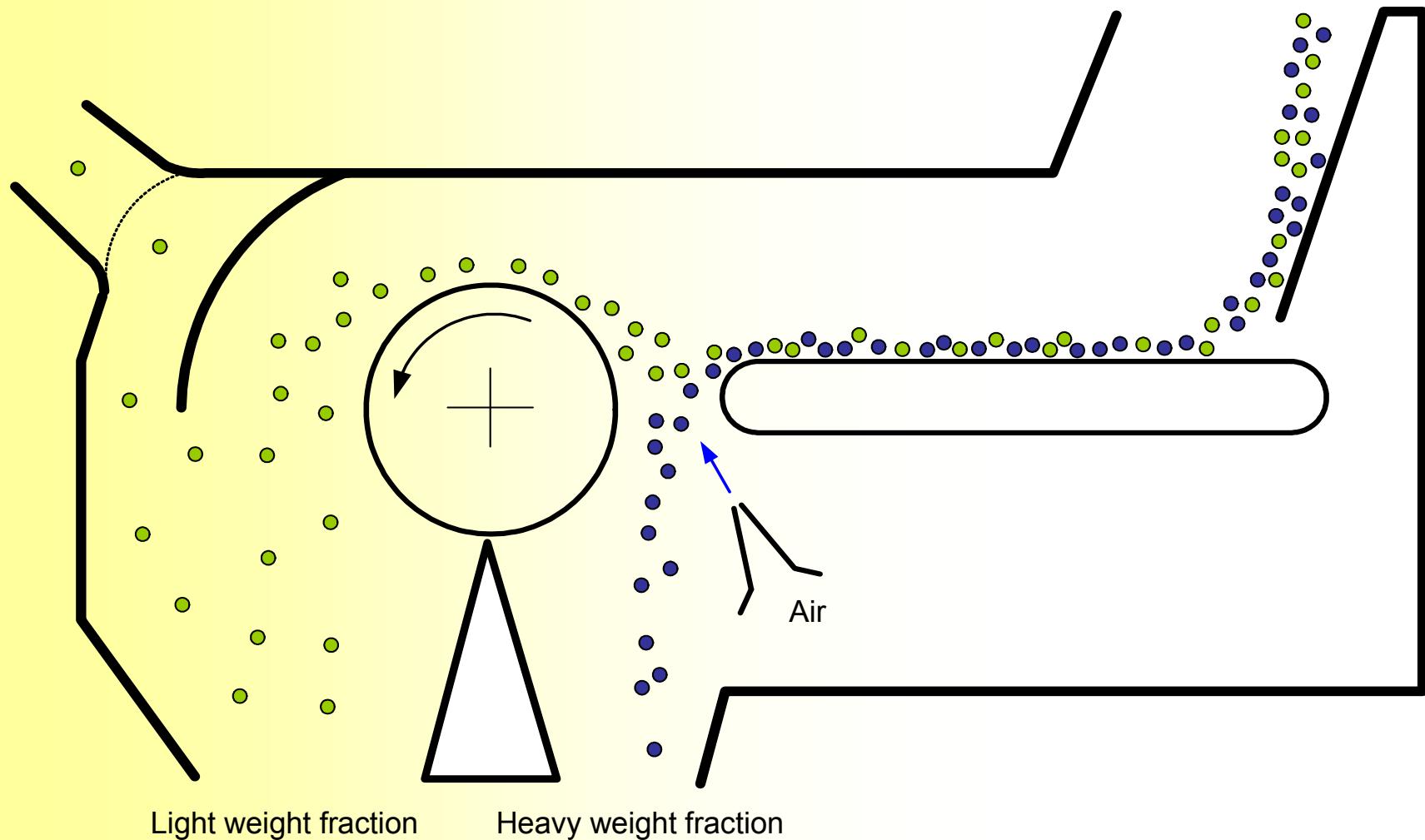
Wind sighter



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Wind sighter



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Batteries



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Stabilat® - Fluff



Stabilat® - Softpellet



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HOF
HERHOF GMBH



Stabilat® - Hardpellet



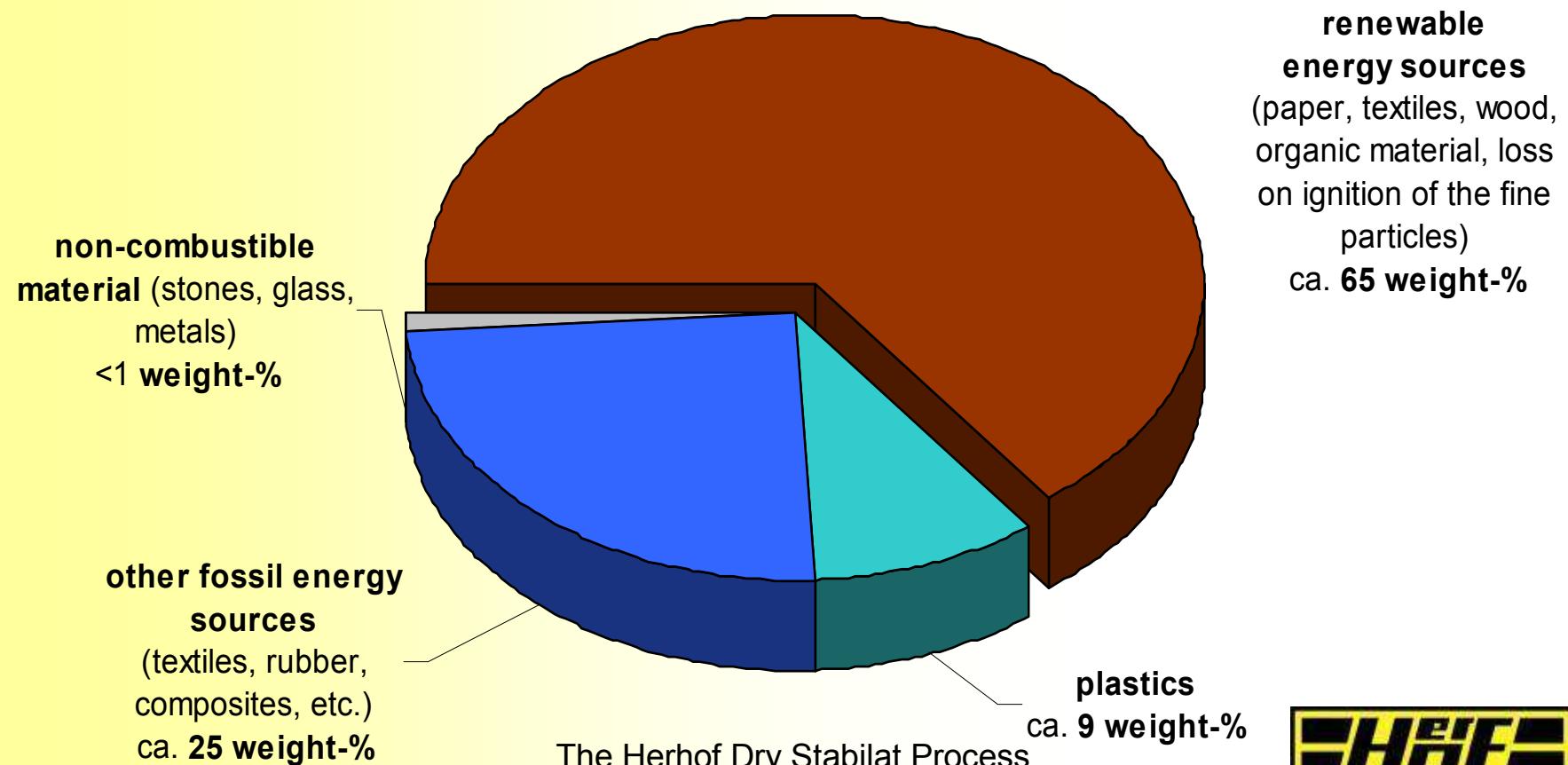
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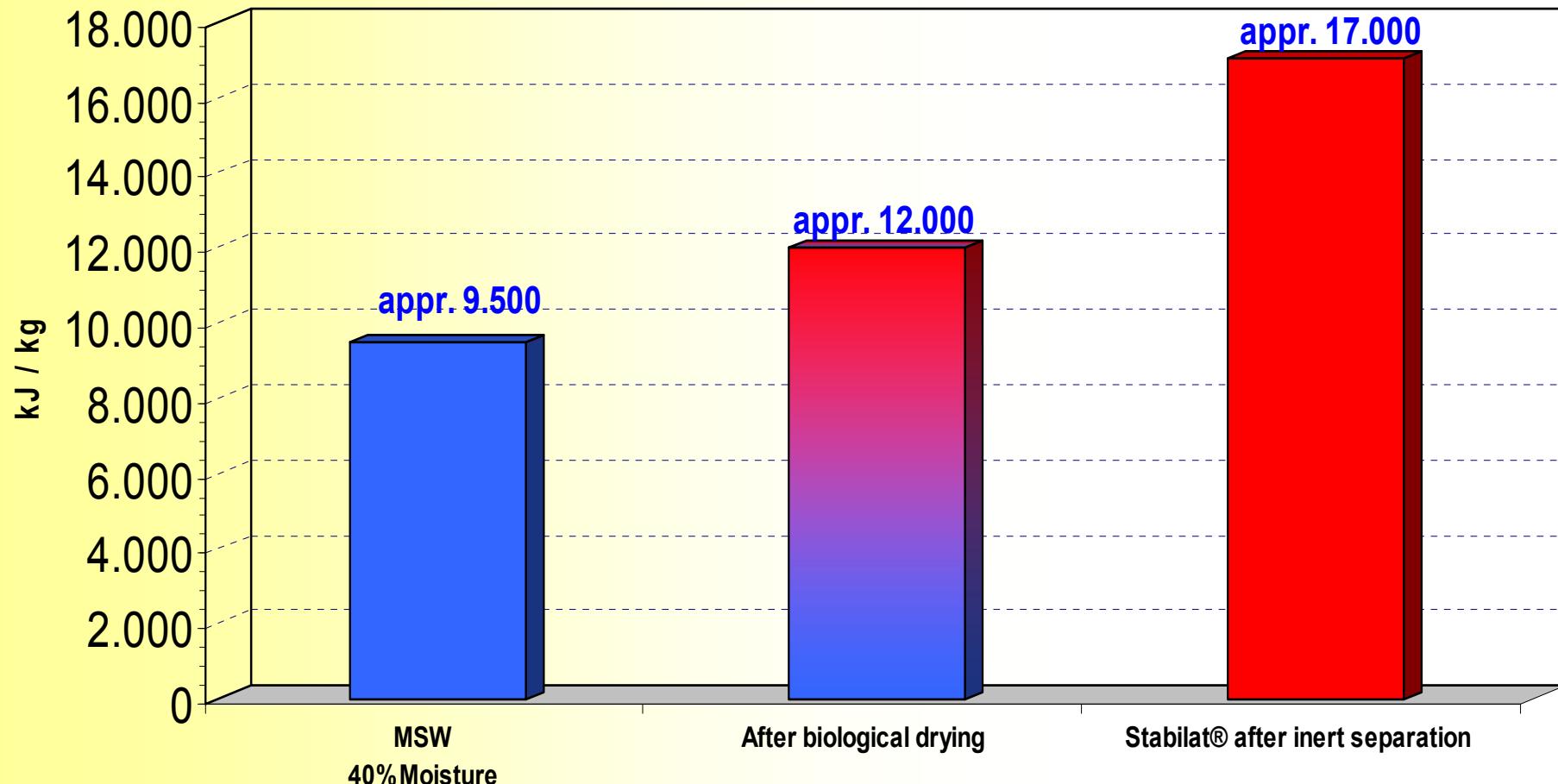
Composition of stabilat®

Heating value : 15 - 18 MJ/kg
Water content : ca. 15 weight-%
Percentage of the total waste throughput : ca. 53 weight-%





Increase of calorific value



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Calorific values of different fuels in comparison

Fuels	Calorific value [kJ/kg]	Calorific value [Btu/lbs]
Lignite	8,000 – 16,000	3,600 – 7,200
Wood	10,500 – 16,500	4,500 – 7,100
Paper	13,500	5,800
Stabilat®	16,000 – 18,000	6,900 – 7,800
Pulverized lignite	20,000	8,600
Hard coal	22,000 – 33,000	9,500 – 14,200
Heating oil	42,000	18,100

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Energy recovery

- 1,000 tons Stabilat equal approx.
 - 447 MJ (heat recocery) and
 - 114 kW (el. Power)

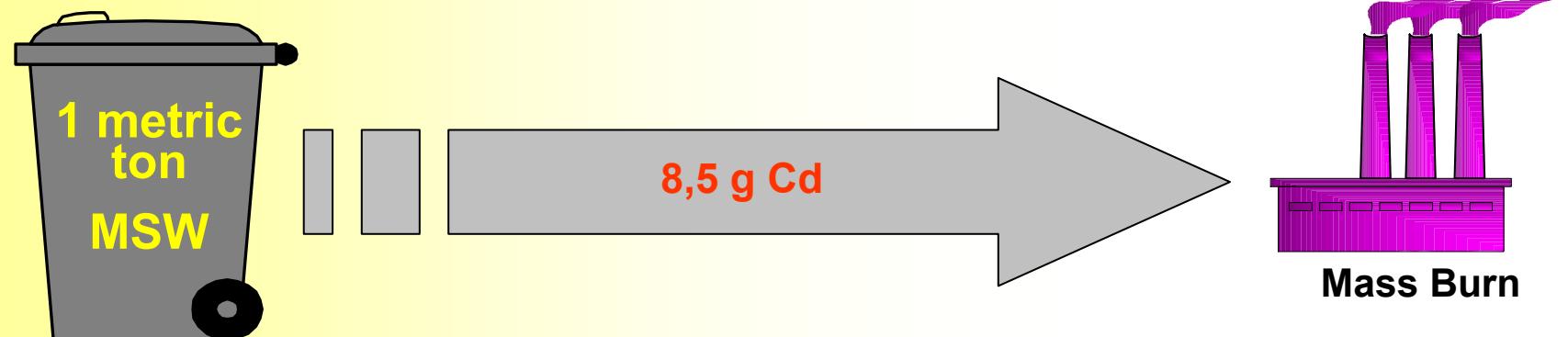
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Comparison of traditional mass burn and the Herhof Stabilat® process in terms of heavy metal reduction

- Cadmium -

Scenario 1: Combustion in incinerator



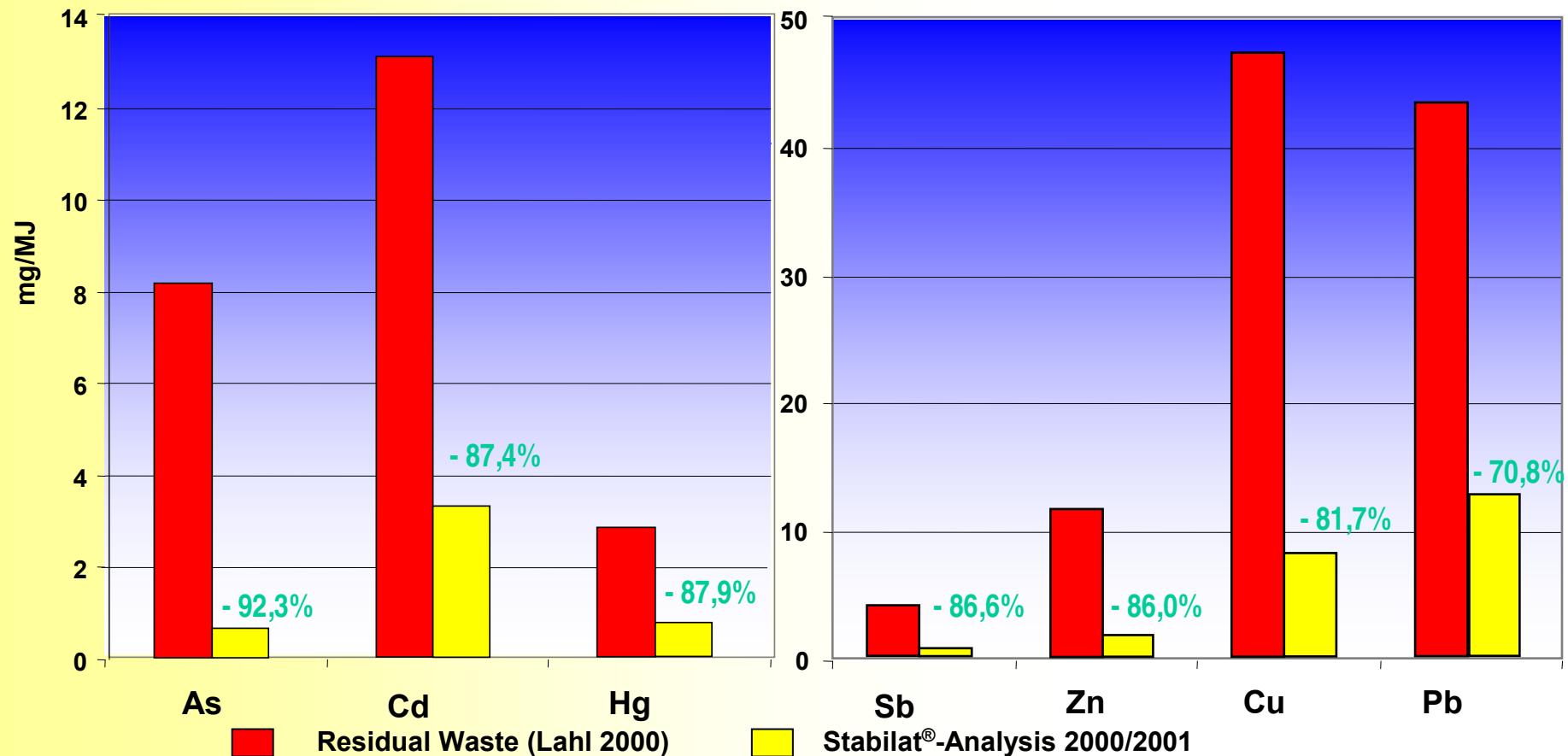
Scenario 2: Recovery by Stabilat® Technology

Cd reduction in fuel -94 %





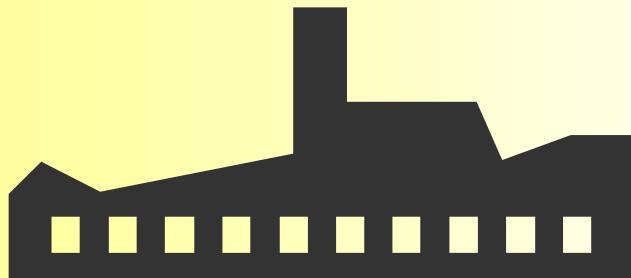
Energy Related Heavy Metal Reduction MSW vs. Stabilat®



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Energy Recovery with Stabilat®



Industrial energy recovery:
Co combustion

- Cement kilns
- Power plants



Material utilisation

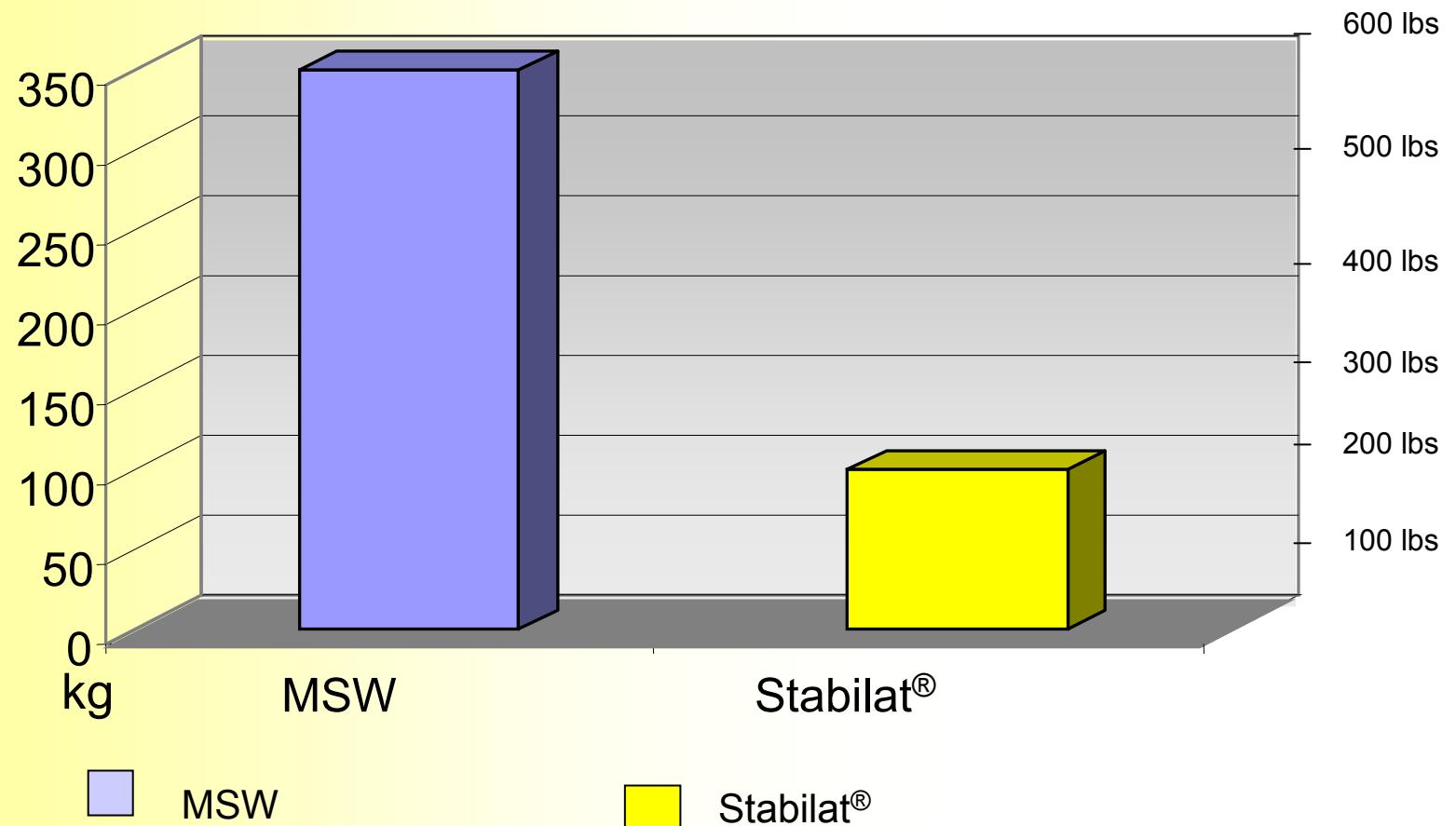
- Gasification with the IPV process
- Production of diesel fuel
- Production of methanol
- Energy and heat generation

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Bottom Ash from 1 metric ton MSW



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Climate effective CO₂-emissions

- comparison of fossil energy sources with stabilat® -

energy source	Overall CO ₂ -	heat value	Overall-CO ₂ -	regenerative	specific	fossil CO ₂ -
	emission factor			energy contingent	fossil CO ₂ -emissions	emission factor
	g CO ₂ /MJ	MJ/kg	g CO ₂ /kg	%-energy contingent	g CO ₂ / kg	g CO ₂ /MJ
brown coal	111	8,6	955	0%	955	111
hard coal	93	29,7	2.762	0%	2.762	93
fuel oil	74	35,4	2.620	0%	2.620	74
natural gas	56	31,7	1.775	0%	1.775	56
stabilat	71	15	1.067	66,8%	354	24

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Status report for the contribution of the waste management to climate protection and possible potentials

Source: Öko Institut e.V. and ifeu Heidelberg GmbH; August 2005
by order of Bundesumweltamt

There are 3 alternative processes for MSW:

1. Conventional MBT with disposal of the rotting residuals in a waste incineration plant
2. MBT with fermentation of the „wet fraction“, drying of the fermentation residuals in a curing area and disposal in a waste incineration plant
3. **Mechanical-Biological Stabilisation (MBS)** with drying of the complete input by means of an intense rotting process; mechanical separation of the dry waste in a secondary fuel fraction, metals and inerts

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Concerning the mentioned criterias there is no basic difference between the three processes.

But it is assumed that the MBS will put the other two processes out of business - under the premise that no residuals will be sent to landfill, because in connection with energy recovery the MBS is the cheapest process.

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