# The role of metals in methane production from shredder waste in landfills

Ehsan Fathi Aghdam<sup>1</sup>, Charlotte Scheutz<sup>1</sup>, Peter Kjeldsen<sup>1</sup>

<sup>1</sup> Department of Environmental Engineering, Technical University of Denmark, 2800 Kgs. Lyngby, Denmark

Corresponding author: ehag@env.dtu.dk; +45 4525 1498

#### Abstract

In this study, different types of shredder waste (i.e. fresh and old samples) were characterized. The role of metals in methane (CH<sub>4</sub>) production from shredder waste was assessed. Shredder waste and sterilized shredder waste were incubated at 37 °C and moisture content of 75 % w/w, and inoculum addition of 30 % of the samples wet weight. Moreover, the ability of metals (iron, aluminum, zinc and copper) contained in shredder waste to produce H<sub>2</sub> was investigated.

Iron, aluminum and zinc produced  $H_2$  in contact with water under anaerobic condition, and the produced  $H_2$  was utilized in biological experiments by hydrogenotrophic methanogens to convert  $CO_2$  to  $CH_4$ . Addition of aluminum and zinc to shredder waste resulted in higher  $CH_4$  production while adding iron and copper to shredder waste resulted in inhibition of  $CH_4$  production. This suggested that aluminum and zinc contribute to high  $CH_4$  production from shredder waste by providing  $H_2$  for hydrogenotrophic methanogens. Gas compositions with higher  $CH_4$  and lower  $CO_2$  observed in landfilled shredder waste are thus most likely due to the consumption of existing  $CO_2$  in the produced biogas and the produced  $H_2$  by biocorrosion of aluminum and zinc by methanogens.

# Keywords

Anaerobic digestion, biocorrosion, elemental metals, anaerobic batch incubation.

# **1. Introduction**

Shredder waste (SW) is the waste produced after mechanical treatment of iron and metal containing wastes including vehicles, bicycles, and white goods. SW consists of mainly plastic, metals, rubber, textile, foam, glass and wood. Significant production of landfill gas has been observed at SW monofills [1, 2]. This is surprising as SW usually contains low fractions of biodegradable waste and the biodegradable fractions have a high content of lignocellulosic components such as wood and cardboard. The reason for high landfill gas production from SW is unknown. Moreover, previous studies have shown gas compositions in SW, which differed from conventional landfill gas—a high  $CH_4$  content and very low or no  $CO_2$  [2, 3]. The reason for the unusual gas composition is also unknown.

Although SW has passed through metal-separation technologies, it still contains metals. We hypothesized that high  $CH_4$  production from SW and unusual gas composition could be due to  $H_2$  production by biocorrosion of metals in the waste, supporting hydrogenotrophic methanogens to convert  $CO_2$  to  $CH_4$ , resulting in higher  $CH_4$  content and lower  $CO_2$ . The objective of this study was to investigate the role of metals contained in SW in  $CH_4$  production from SW.

# 2. Material and methods

# 2.1. Waste sampling, sample preparation and characterization

SW samples were collected from Odense Nord landfill located in Funen, Denmark. SW samples were taken according to the year of deposition: 2009 (SW2009) and 2012 (SW2012). Fresh samples of SW (year 2015) were obtained by sampling the waste on the same day as it was deposited in the waste cell. Samples were taken with an excavator or wheel loader, laid out in a long pile at the landfill, and subdivided three times using the long pile-alternate shovel method.

Fifty kg of each SW sample was transported to the laboratory and kept at 10 °C. In the laboratory, the samples were subdivided three times using the long pile-alternate shovel method, resulting in 5-7 kg of subsamples. Fresh SW (FSW) samples and samples from 2009 and 2012 were mixed together based on equal wet weight to make one composite sample (COM), representative of the whole landfill. Five kg of each sample was dried at 105 °C for 24 hours and total solids (TS) were calculated based on the difference in the weight of the sample before and after drying.

Metals, wires and stones were separated manually from the dried samples. The resulting samples (of about 3-4 kg) were size reduced using a cutter mill with 1 mm sieve. The outcome of the cutter mill was analyzed for volatile solids (VS), total carbon (TC), and total organic carbon (TOC). TS and VS were measured according to APHA Standard Methods. TC and TOC were analyzed using a LECO Induction Furnace CS-200 oven on approximately 0.1 g of dried sample ground to 1 mm according to EN 13137, 2001. All measurements were done in triplicate.

#### 2.2. Biocorrosion experiment

Biocorrosion incubation experiments were conducted to investigate the hypothesis of  $CH_4$  yield enhancement by  $H_2$  production from biocorrosion of metals. According to the conducted literature review iron (Fe), aluminum (Al), zinc (Zn) and copper (Cu) are the main metals in SW [4-6] and thus were examined for their ability to produce  $H_2$ . The experiment had two steps and both were carried out in duplicate in 1 L glass bottles for 20 days in a 37 °C incubator.

In the first step,  $H_2$  production from elemental metals in contact with water was investigated. In this step, 2.5 g of elemental metals was placed in each incubation bottle and 250 mL of tap water was added to each. In step two, the CH<sub>4</sub> production enhancement of inoculum by addition of metals was investigated. In this step, incubation bottles contained 2.5 g of elemental metals and 250 g of inoculum, resulting a concentration of 10 g/L of liquid for each metal. Bottles containing only inoculum were used as blank to calculate CH<sub>4</sub> production from inoculum alone. Bottles were flushed with N<sub>2</sub> for 15 minutes to establish an anaerobic condition, and then sealed with rubber septum.

Gas volumes were converted to STP conditions. Gas samples (0.3 mL) were taken from the headspace of the bottles and directly injected to a thermo-scientific trace gas chromatograph (TRACE 1310 GC, Molsieve, 0.53 mm, 30 m) with a thermal conductivity detector (TCD). Mesophilic inoculum, used in this experiment, was collected from a biogas plant located at Va Syd Sjölunda wastewater treatment plant (WWTP), Malmo, Sweden. Powders of elemental metals were obtained from Sigma-Aldrich.

# 2.3. Batch incubation experiment

Batch incubation experiments were performed in glass bottles with total volumes of 5 L at 37 °C. All bottles were connected to 2 L aluminum gas bags by a PVC tube to collect the produced biogas. All PVC tubes were equipped with a rubber septum for sampling the produced biogas. At each measurement of gas composition, 5 mL gas samples were taken from the rubber septum with a syringe and injected immediately into evacuated glass vials equipped with rubber septa (Exetainer Vail, Labco Ltd, Lampeter, UK), which then were analyzed by a gas chromatograph (490-PRO Micro GC).

In order to investigate the role of metals on the CH<sub>4</sub> production, Fe, Al, Zn, and Cu with dimension of 5 mm  $\times$  5 mm and concentrations of 5, 2, 2, and 2 % of the substrate wet weight (25, 10, 10, 10 g/L of liquid), respectively, were added separately to the incubation bottles containing the COM samples. Moisture content of the samples was adjusted to 75 % w/w, and inoculum (30 % of substrate wet weight) was added to the incubation bottles. One bottle containing only inoculum and water were used as blank to determine CH<sub>4</sub> production from the inoculum alone, which was subtracted from the CH<sub>4</sub> production of waste samples. Mesophilic inoculum collected from the biogas plant located at Va Syd Sjölunda WWTP (Malmo, Sweden) was used in this experiment.

Abiotic control experiments were also performed by sterilizing samples (autoclaving three times for 1 h at 121  $^{\circ}$ C) to measure possible CH<sub>4</sub> production due to non-microbial processes. All reactors were flushed for 20 minutes with nitrogen gas to make an anaerobic condition. The biogas volume was measured using a water

displacement method. Gas volumes were converted to STP conditions.  $CH_4$  and  $CO_2$  concentrations were measured by a 490-PRO Micro GC (Agilent Technologies Denmark Aps, Glostrup, Denmark) with a TCD.

# 3. Results and discussion

# 3.1. Waste characterization

Table 1 shows waste characterization in terms of TS, VS, TC, TOC. Overall, low variation was observed in the TS content of different waste samples. FSW had the highest TS content (91 %), while COM had the lowest (82 %). TC contents of waste samples were from 14 to 24 % with FSW having the highest (24 %) and SW2009 the lowest (14 %). The TS and TC content of the waste samples were comparable to previous studies [7-10].

FSW contained the highest amount of VS, and TOC (32 % and 21 %, respectively), which is reasonable as this sample was fresh and thus had not undergone anaerobic degradation in the landfill. The COM sample was a mix of FSW, SW2012 and SW2009 and it had VS and TOC contents between these substrates. SW2012 and SW2009 had lower VS and TOC contents than FSW, most likely as a result of anaerobic degradation since their deposition in the landfill.

| Tuble 1. Characteristics of different fractions of 5 (). I tuble of a brackets give the standard de fraction. |                        |                        |                        |               |  |
|---|------------------------|------------------------|------------------------|---------------|--|
|   | TS                     | VS                     | TC                     | TOC           |  |
| Shredder waste  | (%, kg/kg wet          | (%, kg/kg wet          | (%, kg/kg dry          | (%, kg/kg dry |  |
|   | waste)                 | waste)                 | waste)                 | waste)        |  |
| SW deposited in 2009 (SW2009)   | 89 (6.54)              | 18 (1.17)              | 14 (0.67)              | 11 (0.93)     |  |
| SW deposited in 2012 (SW2012)   | 83 (1.48)              | 20 (0.35)              | 15 (0.82)              | 14 (0.57)     |  |
| Fresh sample (FSW)  | 91 (0.02)              | 32 (1.15)              | 24 (1.99)              | 21 (1.29)     |  |
| Composite SW sample (COM) <sup><i>a</i></sup>   | 82 (0.71)              | 24 (0.92)              | 18 (1.24)              | 16 (0.60)     |  |
| Composite SW sample (COM) <sup><i>a</i></sup>   | 91 (0.02)<br>82 (0.71) | 32 (1.15)<br>24 (0.92) | 24 (1.99)<br>18 (1.24) | 16 (0.60)     |  |

Table 1. Characteristics of different fractions of SW. Numbers in brackets give the standard deviation

<sup>a</sup> Mix of SW2009, SW2012 and FSW.

#### 3.2. Biocorrosion experiment

Fig. 1 presents the cumulative  $H_2$  (1a) and  $CH_4$  production curves (1b) over a 20-day incubation period. As can be seen from Fig. 1a, Fe in water (Water+Fe incubation) showed the highest  $H_2$  generation, followed by Al and Zn in water, respectively.  $H_2$  was not generated by Cu in water. Accumulation of  $H_2$  was not observed in biological (containing inoculum) incubations (Fig. 1a). This was expected, as hydrogenotrophic methanogenesis is a very fast process, meaning that the generated  $H_2$  is consumed rapidly in the production of  $CH_4$ . This helps to keep the  $H_2$  pressure low, which is needed for successful anaerobic digestion processes to occur.

Fig. 1b shows that adding Fe, Al and Zn to inoculum resulted in higher  $CH_4$  generation than inoculum alone. However, addition of Cu to inoculum (Inoc+Cu incubation) resulted in lower  $CH_4$  generation compared to inoculum alone. These results indicate that  $H_2$  generation from corrosion of Fe, Al, and Zn can be utilized by hydrogenotrophic methanogens to convert  $CO_2$  to  $CH_4$ .  $CH_4$  generation was not observed in incubations containing water and metals, indicating there was no chemical production of  $CH_4$ .

The results of this experiment were in line with previous studies. For instance, Belay and Daniels [11], Hu et al. [12] and Lorowitz et al. [13] observed improvement of  $CH_4$  production from certain types of methanogenic cultures and waste activated sludge by addition of Fe, Al and Zn due to H<sub>2</sub> production by these metals. Inhibition of  $CH_4$  production by addition of Cu was also observed in previous studies [11, 14, 15].



**Fig 1**. Cumulative  $H_2$  (a) and  $CH_4$  production curves (b) in biocorrosion experiment over period of 20 days. Please note that the  $H_2$  production from Water+Cu, Blank, Inoc+Fe, Inoc+Al, Inoc+Zn, Inoc+Cu incubations (Fig. 1a), and the  $CH_4$  production from Water+Fe, Water+Al, Water+Zn and Water+Cu incubations (Fig. 1b) were all zero and thus the curves are on top of each other and not visible on the graph.

#### 3.3. Batch incubation experiment

Fig. 2 shows cumulative  $CH_4$  production curves of all waste samples during 148 days incubation period. Sterilized reactors did not produce  $CH_4$ , indicating there was no abiotic production of  $CH_4$  from SW.



**Fig 2.** Cumulative  $CH_4$  generation from SW samples, biotic and abiotic experiments, during period of 148 days. Please note that  $CH_4$  production from sterilized reactors (starting with "Ste") were all zero and thus the curves are on top of each other and not visible on the graph.

Addition of Zn and Al to the COM sample resulted in higher  $CH_4$  production in comparison to the experiment with COM alone, while adding Fe and Cu resulted in lower  $CH_4$  production. The obtained results for the impact of Al, Zn and Cu on  $CH_4$  production is in line with the biocorrosion experiment. However, adding Fe resulted in lower  $CH_4$  production in this experiment, while it enhanced  $CH_4$  production in the biocorrosion experiment. This could be due to a higher concentration of Fe in this experiment (25 g/L) compared to the biocorrosion experiment (10 g/L).

Iron (Fe<sup>0</sup> and Fe<sup>2+</sup>) is an essential microelement for enzymatic reaction and can enhance anaerobic digestion by activating enzymes or H<sub>2</sub> production, or reducing sulfide toxicity [16-18]. However, at high concentrations it can have an inhibitory impact on microorganisms and on the anaerobic digestion process [19, 20].

Table 2 shows the headspace  $CH_4$  and  $CO_2$  concentrations of the biotic reactors measured on the last day of the experiment. The  $CH_4/CO_2$  ratio in the reactors was significantly different compared to the  $CH_4/CO_2$  ratio of conventional landfill gas. Unusual gas composition from SW (high  $CH_4$  and low  $CO_2$  content) has also been reported in previous studies [2, 3]. When comparing the headspace  $CO_2$  concentrations of COM reactor with COM+Al and COM+Zn reactors, it can be seen that COM+Al and COM+Zn reactors have lower headspace  $CO_2$  concentrations. This could be due to utilization of produced  $H_2$  by corrosion of Al and Zn and existing  $CO_2$  in produced biogas by methanogens, resulting in higher  $CH_4$  and lower  $CO_2$  in the headspace of these reactors.

| experiment (day 148). |   |  |  |  |  |
|-----------------------|---|--|--|--|--|
| $CH_{4}(\%)$          | CO <sub>2</sub> (%)   | CH <sub>4</sub> /CO <sub>2</sub>   |  |  |  |
| 50.4                  | 4.0   | 12.6   |  |  |  |
| 44.5                  | 3.6   | 12.4   |  |  |  |
| 53.3                  | 3.2   | 16.5   |  |  |  |
| 52.9                  | 1.7   | 30.7   |  |  |  |
| 44.7                  | 3.8   | 11.7   |  |  |  |
|                       | CH <sub>4</sub> (%)<br>50.4<br>44.5<br>53.3<br>52.9<br>44.7 | experiment (day 148).   CH <sub>4</sub> (%) CO <sub>2</sub> (%)   50.4 4.0   44.5 3.6   53.3 3.2   52.9 1.7   44.7 3.8 |  |  |  |

Table 2.  $CH_4$  and  $CO_2$  concentrations in the headspace of the biotic reactors measured on the last day of the

#### 4. Conclusions

Different types of SW were characterized in this study and the role of metals in  $CH_4$  production from them was investigated by performing anaerobic batch incubations. It was evident from the incubation experiments that  $CH_4$  production from SW was not abiotic. Al and Zn were found to produce  $H_2$ , and it was observed that the produced  $H_2$  can be consumed by methanogens to convert  $CO_2$  to  $CH_4$ . Moreover, results of the incubation experiments indicated that the unusual gas composition (higher  $CH_4$  and lower  $CO_2$ ), and the relatively high  $CH_4$  production rate from landfilling of SW is most likely due to the consumption of existing  $CO_2$  in the produced biogas and  $H_2$  produced by biocorrosion of Al and Zn by methanogens.

#### Acknowledgments

The authors would like to thank Hector Garcia and Hector Diaz for their technical support throughout the laboratory experiment. We would also like to thank Rasmus Olsen and Ulrik Lønkjær (Odense Nord Miljøcenter) and Max Granqvist (Va Syd, Sjölunda WWTP) for their help during sample collection. This project was partially financed by Odense Renovation A/S company.

#### References

- [1] J. Mønster, J. Samuelsson, P. Kjeldsen, and C. Scheutz, "Quantification of methane emissions from 15 Danish landfills using the mobile tracer dispersion method," *Waste Manag.*, vol. 35, pp. 177–186, 2015.
- [2] C. Scheutz, A. M. Fredenslund, J. Nedenskov, J. Samuelsson, and P. Kjeldsen, "Gas production, composition and emission at a modern disposal site receiving waste with a low-organic content," *Waste Manag.*, vol. 31, no. 5, pp. 946–955, 2011.
- [3] R. Olsen and H. C. Willumsen, "Characterization of Gas, Heat and Humidity Profiles in Landfilled Shredder Residue At Odense Nord Landfill, Denmark," Sardinia 2013, Proc. Fourteenth Int. Waste Manag. Landfill Symp. 30 Sept. 4 October, Sardinia, Italy., 2013.

- [4] N. Ahmed, H. Wenzel, and J. B. Hansen, "Characterization of Shredder Residues generated and deposited in Denmark," *Waste Manag.*, vol. 34, no. 7, pp. 1279–1288, 2014.
- [5] S. Fiore, B. Ruffino, and M. C. Zanetti, "Automobile Shredder Residues in Italy: Characterization and valorization opportunities," *Waste Manag.*, vol. 32, no. 8, pp. 1548–1559, 2012.
- [6] S. Galvagno, F. Fortuna, G. Cornacchia, S. Casu, T. Coppola, and V. K. Sharma, "Pyrolysis process for treatment of automobile shredder residue: Preliminary experimental results," *Energy Convers. Manag.*, vol. 42, no. 5, pp. 573–586, 2001.
- [7] C. Pasel and W. Wanzl, "Experimental investigations on reactor scale-up and optimisation of product quality in pyrolysis of shredder waste," *Fuel Process. Technol.*, vol. 80, no. 1, pp. 47–67, 2003.
- [8] M. Day, Z. Shen, and J. D. Cooney, "Pyrolysis of auto shredder residue: experiments with a laboratory screw kiln reactor," *J. Anal. Appl. Pyrolysis*, vol. 51, no. 1, pp. 181–200, 1999.
- [9] L. Morselli, A. Santini, F. Passarini, and I. Vassura, "Automotive shredder residue (ASR) characterization for a valuable management," *Waste Manag.*, vol. 30, no. 11, pp. 2228–2234, 2010.
- [10] Z. Mou, C. Scheutz, and P. Kjeldsen, "Evaluating the biochemical methane potential (BMP) of loworganic waste at Danish landfills," *Waste Manag.*, vol. 34, no. 11, pp. 2251–2259, 2014.
- [11] N. Belay and L. Daniels, "Elemental metals as electron sources for biological methane formation from CO2," *Antonie Van Leeuwenhoek*, vol. 57, no. 1, pp. 1–7, 1990.
- [12] Y. Hu, X. Hao, D. Zhao, and K. Fu, "Enhancing the CH4 yield of anaerobic digestion via endogenous CO2 fixation by exogenous H2.," *Chemosphere*, vol. 140, pp. 34–9, 2015.
- [13] W. H. Lorowitz, D. P. Nagle, and R. S. Tanner, "Anaerobic oxidation of elemental metals coupled to methanogenesis by Methanobacterium thermoautotrophicum," *Environ. Sci. Technol.*, vol. 26, no. 12, pp. 1606–1610, 1992.
- [14] B. K. Ahring and P. Westermann, "Sensitivity of thermophilic methanogenic bacteria to heavy metals," *Curr. Microbiol.*, vol. 12, no. 5, pp. 273–276, 1985.
- [15] P. Jin, S. K. Bhattacharya, C. J. Williams, and H. Zhang, "Effects of sulfide addition on copper inhibition in methanogenic systems," *Water Res.*, vol. 32, no. 4, pp. 977–988, 1998.
- [16] Y. Feng, Y. Zhang, X. Quan, and S. Chen, "Enhanced anaerobic digestion of waste activated sludge digestion by the addition of zero valent iron," *Water Res.*, vol. 52, pp. 242–250, 2014.
- [17] K. H. Hansen, I. Angelidaki, and B. K. Ahring, "Improving thermophilic anaerobic digestion of swine manure," *Water Res.*, vol. 33, no. 8, pp. 1805–1810, 1999.
- [18] M. Kayhanian and D. Rich, "Pilot-scale high solids thermophilic anaerobic digestion of municipal solid waste with an emphasis on nutrient requirements," *Biomass Bioenergy*, vol. 8, no. 6, pp. 433–444, 1995.
- [19] B. M. Gonzalez-Silva, R. Briones-Gallardo, E. Razo-Flores, and L. B. Celis, "Inhibition of sulfate reduction by iron, cadmium and sulfide in granular sludge," *J. Hazard. Mater.*, vol. 172, no. 1, pp. 400– 407, 2009.
- [20] H. Yang and J. Shen, "Effect of ferrous iron concentration on anaerobic bio-hydrogen production from soluble starch," *Int. J. Hydrogen Energy*, vol. 31, no. 15, pp. 2137–2146, 2006.