

**ATHENS2017**



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# Hydrothermal carbonization of biomass for production of densified solid fuel

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Asli Toptas Tag, Gozde Duman, Jale Yanik  
Ege University, Department of Chemistry,  
Izmir/ Turkey

# What is biochar?



Stable carbon-rich product obtained from the thermochemical conversion of plant- and animal-based biomass in an oxygen-limited environment



- Lower amount of volatile organic compounds (VOCs),
- No water
- Stored for many years without decay.
- The higher energy density

# What is biochar made from?



# How is biochar made?



## Fuel Characteristics

- ✓ High Yield
- ✓ High energy density
- ✓ High combustion reactivity
- ✓ Low volatile matter
- ✓ Low ash content



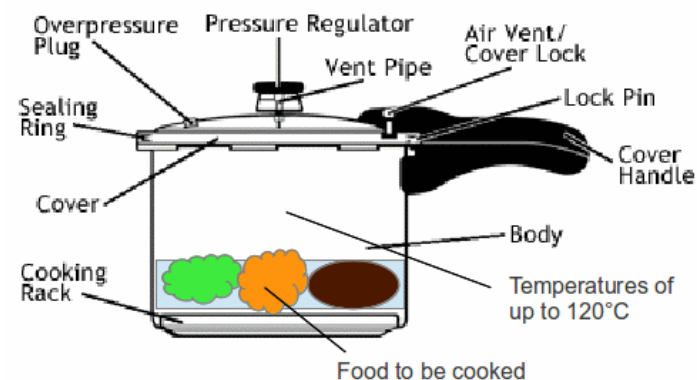
## Pyrolysis

High yield  
High ash content  
Pretreatment of wet biomass

## Hydrothermal Carbonization (HTC)

Under development

Pressure cooker principle



- High yield
- Applicable to wet biomass
- Relatively lower temperatures
- Smaller reactor volumes

# Objective

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⇒ Investigation of biochar obtained from hydrothermal carbonization as energy feedstock.

⇒ Comparison with biochars derived from pyrolysis process

# Feedstock



Sunflower stalk (SS)



Poultry litter (PL)



Seaweed (AB)

	SS	PL	AB
<i>Ultimate analysis (wt.%, dry basis)</i>			
C	34.17	35.70	35.10
H	4.92	5.27	4.00
N	1.48	9.61	1.05
S	0.45	0.24	0.95
O	51.08	40.98	38.10
<i>Proximate analysis (wt.%, dry basis)</i>			
Volatile matter	74.6	68.3	58.4
Ash	7.9	8.2	20.8
Fixed carbon	17.5	23.5	20.8
<i>High heating value (HHV), MJ kg<sup>-1</sup></i>			
	13.50	15.10	11.60

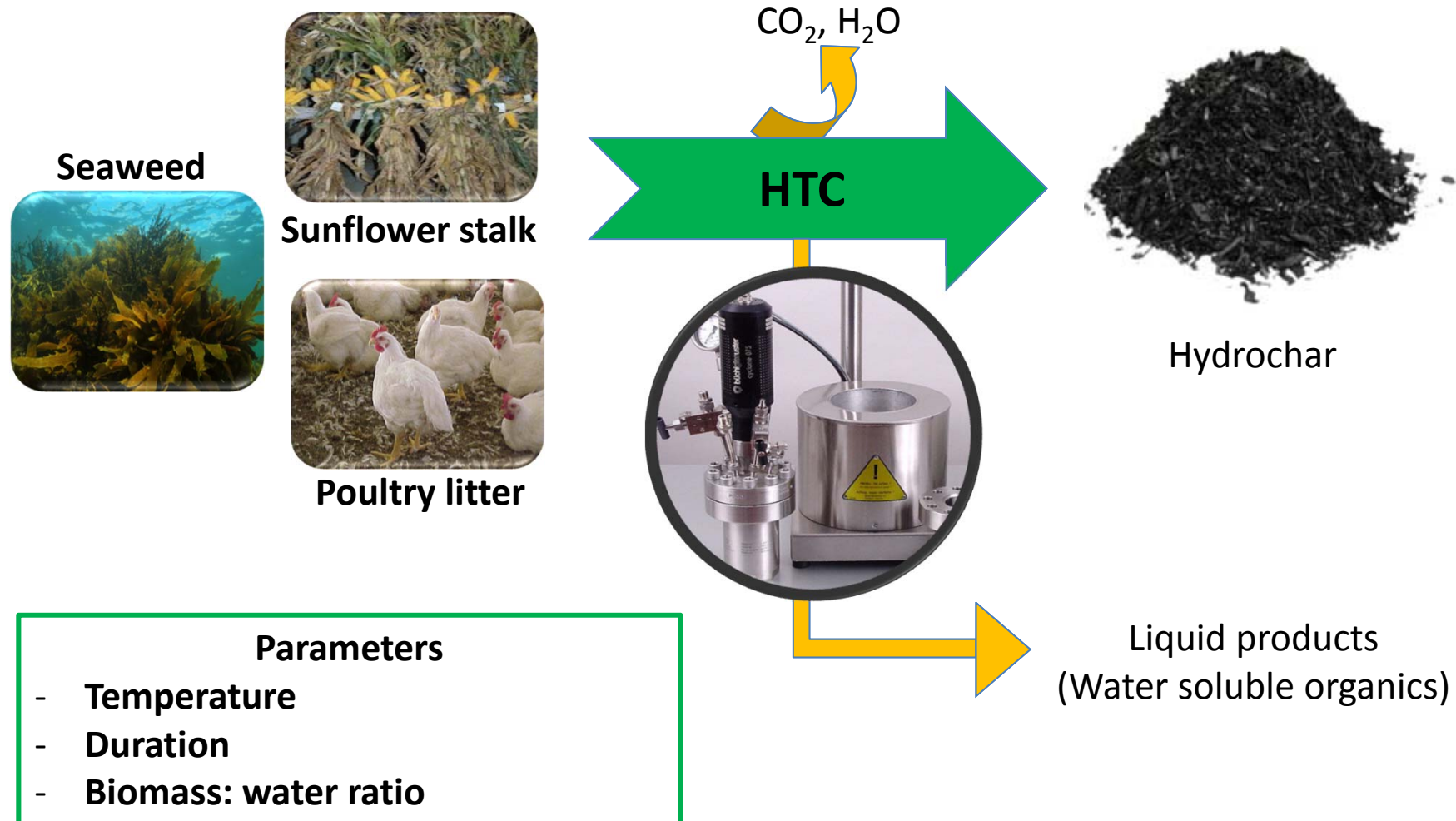
## Inorganic content of biomass, % wt.

	SS	PL	AB
Na <sub>2</sub> O	0.19	<b>0.40</b>	<b>0.83</b>
K <sub>2</sub> O	<b>0.47</b>	<b>0.63</b>	0.25
CaO	<b>4.09</b>	<b>7.83</b>	<b>4.33</b>
MgO	1.78	1.28	<b>3.16</b>
SiO <sub>2</sub>	<b>4.08</b>	1.61	0.76
Al <sub>2</sub> O <sub>3</sub>	0.06	0.52	0.90

# Methodology



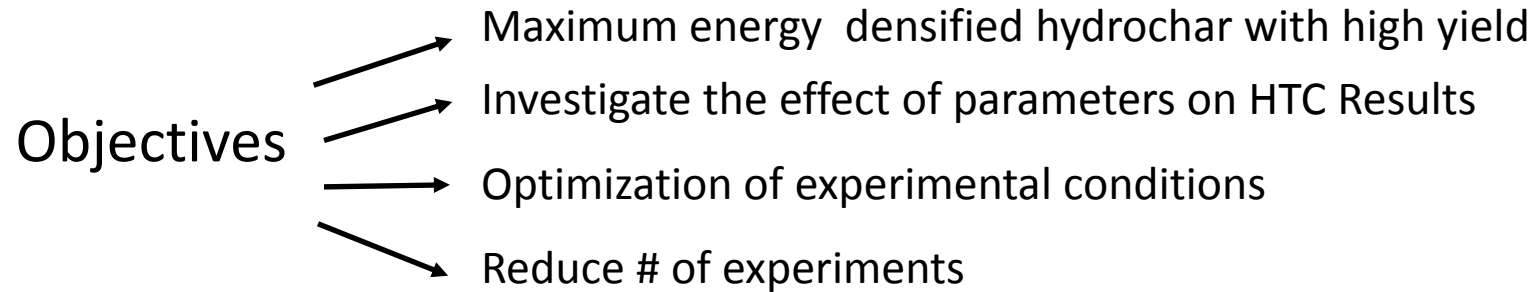
- Hydrothermal carbonization (HTC)



# Methodology



## Experimental conditions



Variables



- Temperature
- Duration
- Biomass: water ratio

Responses



- Energy density
- Mass Yield

Experimental design



Central composite design

**20 Experiments**

Evaluation/ Analysis of Response  
Optimum conditions



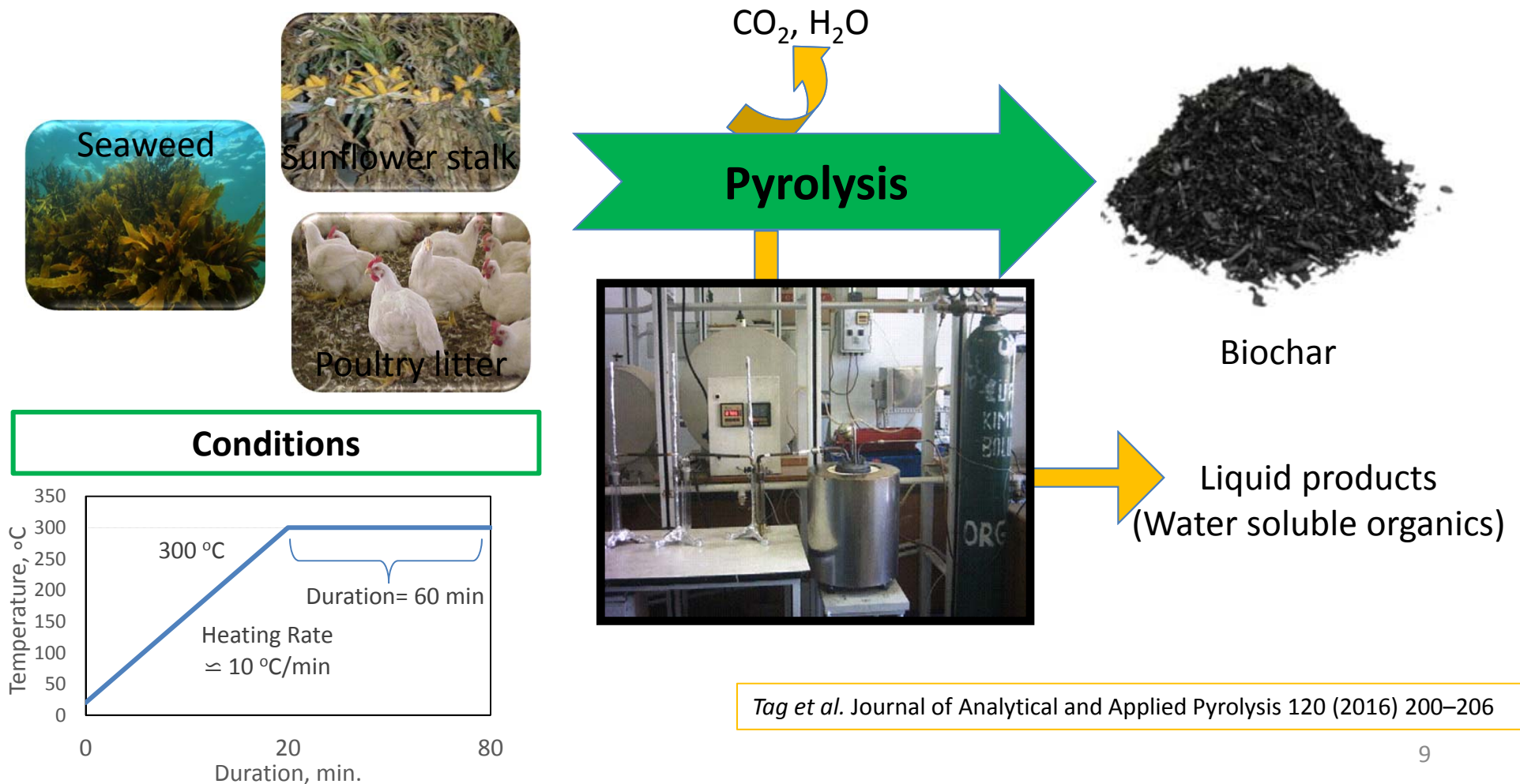
Design Expert Software 8.0  
Response Surface Methodology  
Anova test



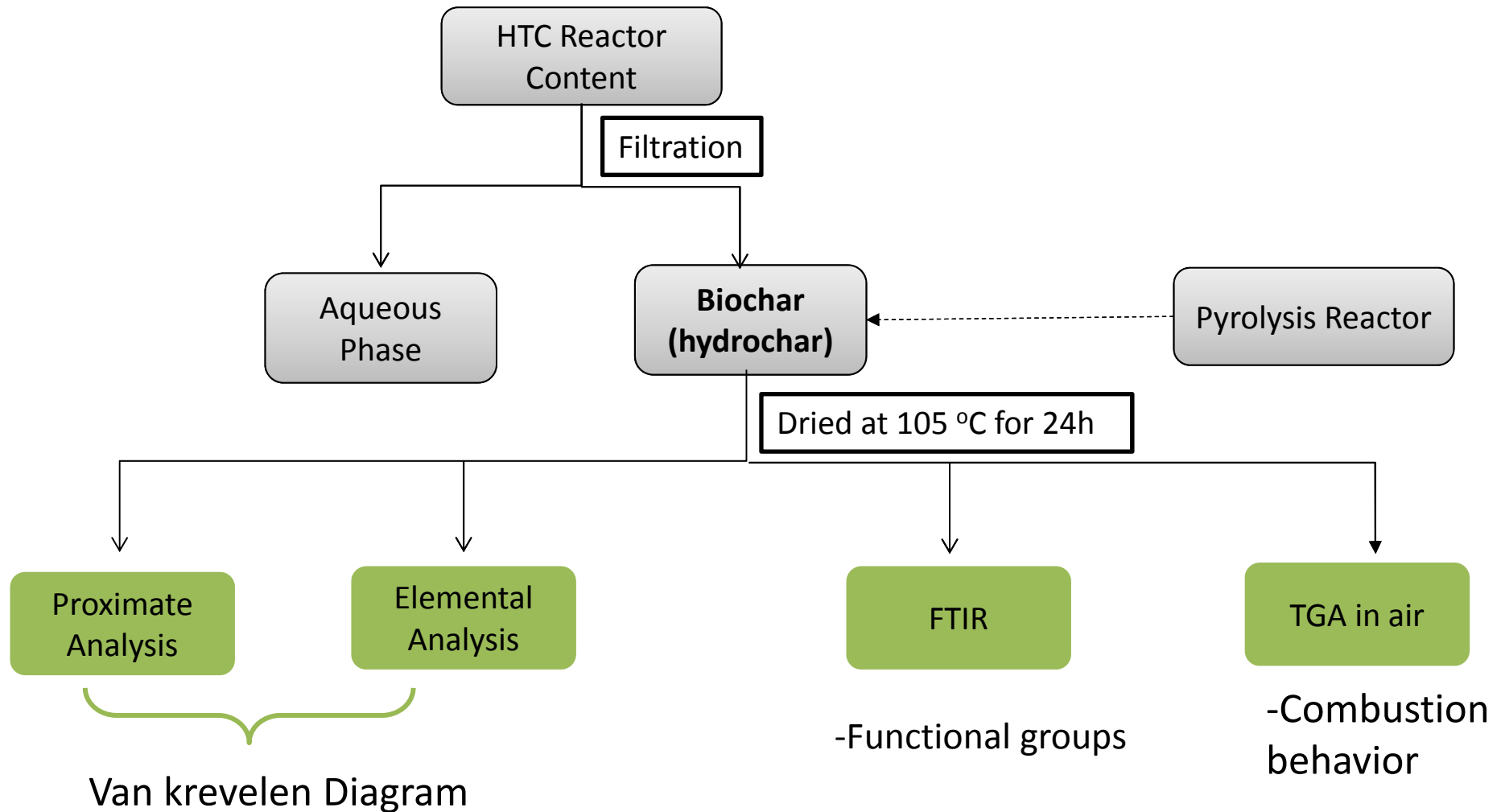
# Methodology



- Low Temperature Pyrolysis



# Biochar Analyses



HHV calculation\*  $\rightarrow$  Energy density =  $\frac{HHV_{\text{biochar}}}{HHV_{\text{biomass}}}$

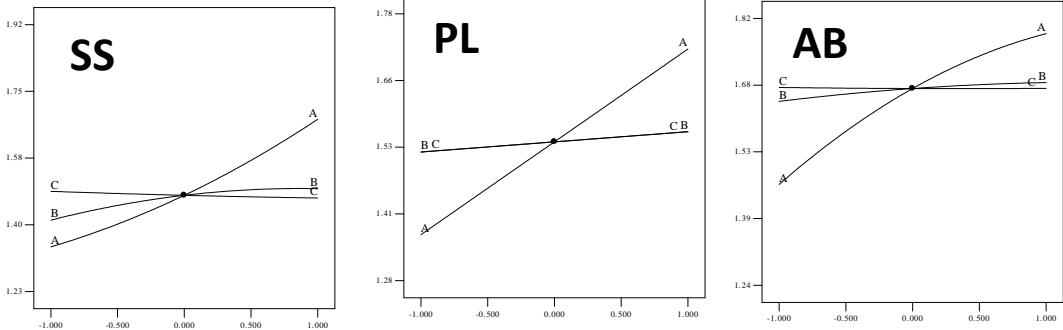
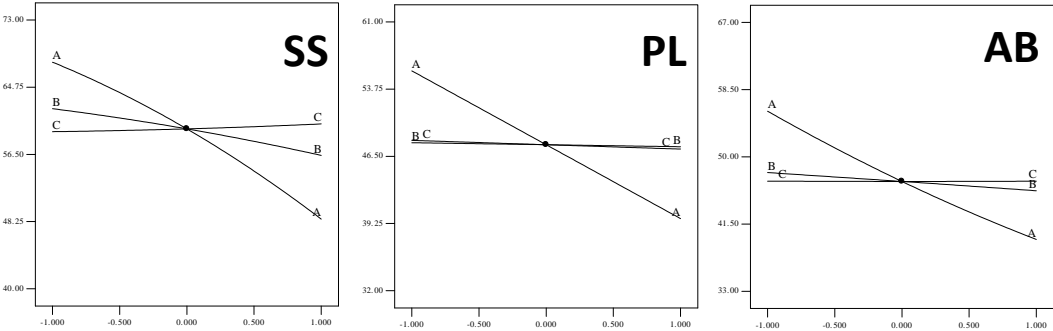
# Results & Discussion



## Yield and Energy Density

Factor	-1.68	-1	0	+1	+1.68
<b>Temperature (°C)= <math>X_1</math></b>	150	175	212	250	275
Duration (min)= $X_2$	0	60	150	240	300
Biomass:water ratio = $X_3$	0.05	0.15	0.30	0.45	0.55

Yield



Energy Density

# Results & Discussion



## Optimization conditions

Maximize energy density

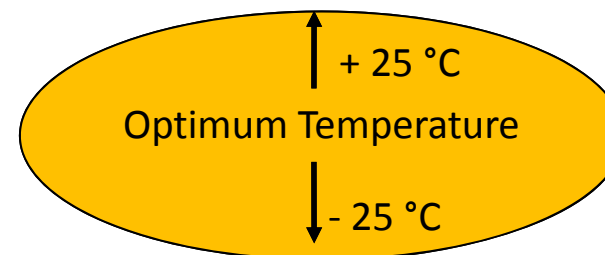
Mass yield > 40 %

	<b>SS</b>	<b>PL</b>	<b>AB</b>
Temperature, °C	250	250	225
Duration, min	150	120	120
Biomass:water ratio	0.30	0.30	0.30
Energy density	<b>1.68</b>	<b>1.76</b>	<b>1.73</b>
Mass yield, % wt.	<b>52.0</b>	<b>40.2</b>	<b>45.1</b>

# Results & Discussion



## Analyses of Biochars

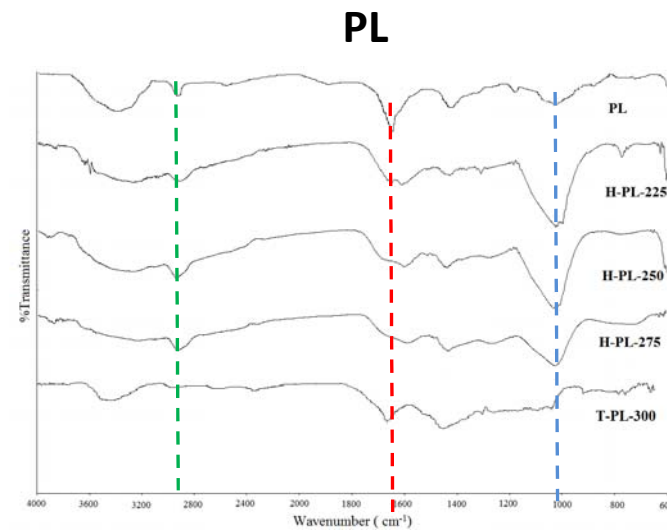
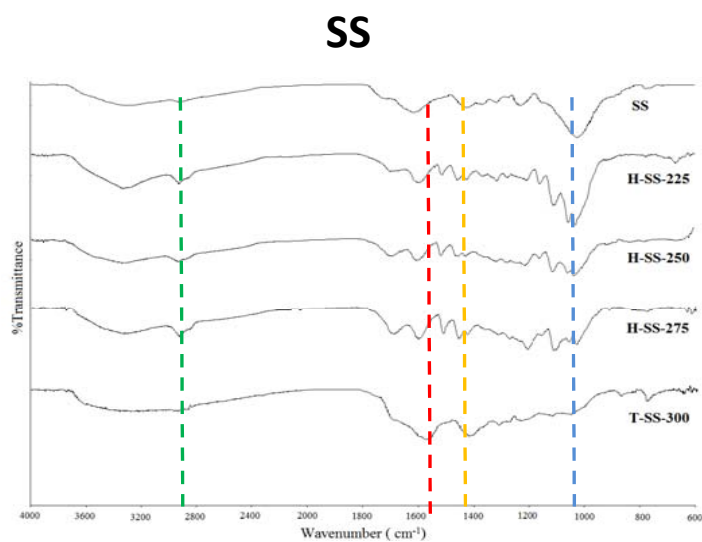


	Elemental analysis,wt %					Proximate analysis,wt %			HHV, MJ.kg <sup>-1</sup>	Yield, % wt.	Energy Density
	C	H	N	S	O	Ash	VM	FC			
<b>H-SS-225</b>	51.3	5.71	0.82	0.08	36.19	5.9	69.6	24.5	20.77	55.1	1.54
<b>H-SS-250</b>	55.07	5.94	0.94	0.09	32.96	5.0	55.4	39.6	22.71	52.0	1.68
<b>H-SS-275</b>	58.16	5.64	0.91	0.04	32.25	3.0	53.3	43.7	23.54	41.0	1.74
<b>T-SS-300</b>	50.89	4.09	1.17	0.35	31.30	12.2	47.1	40.7	19.11	65.1	1.42
<b>H-PL-225</b>	57.57	4.66	4.12	0.41	26.94	6.3	60.2	33.5	22.65	42.2	1.50
<b>H-PL-250</b>	63.87	5.45	5.36	0.37	19.05	5.9	50.1	44.0	26.58	40.2	1.76
<b>H-PL-275</b>	62.01	6.32	5.70	0.26	21.41	4.3	48.2	47.5	26.73	32.8	1.77
<b>T-PL-300</b>	53.57	3.69	5.41	0.19	24.34	12.8	44.1	43.1	20.23	53.2	1.34
<b>H-AB-200</b>	48.06	4.56	1.68	0.21	34.69	10.8	55.4	33.8	18.33	51.6	1.58
<b>H-AB-225</b>	53.26	4.01	1.52	0.28	29.03	11.9	50.2	37.9	20.07	45.1	1.73
<b>H-AB-250</b>	54.29	4.09	1.56	0.36	30.70	9.0	47.2	43.8	20.42	41.2	1.76
<b>T-AB-300</b>	41.49	3.23	1.86	0.15	24.57	28.7	45.9	25.4	15.13	63.2	1.30

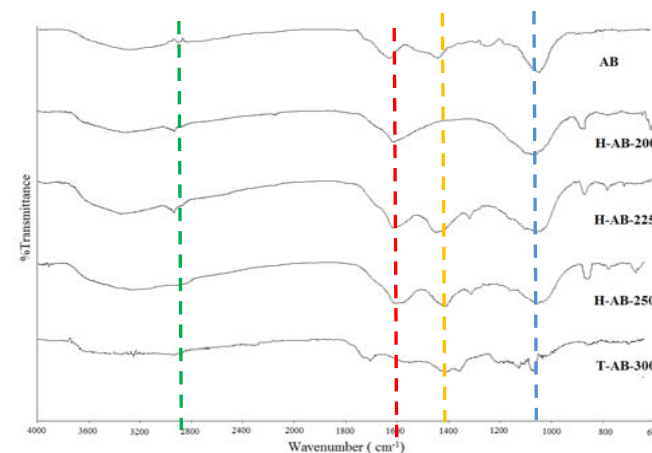
# Results & Discussion



## FTIR spectrum



- aliphatic C-H stretching vibration
- alcohol C-O stretching vibration
- aliphatic C=O stretching vibration
- aromatic ring vibration



AB

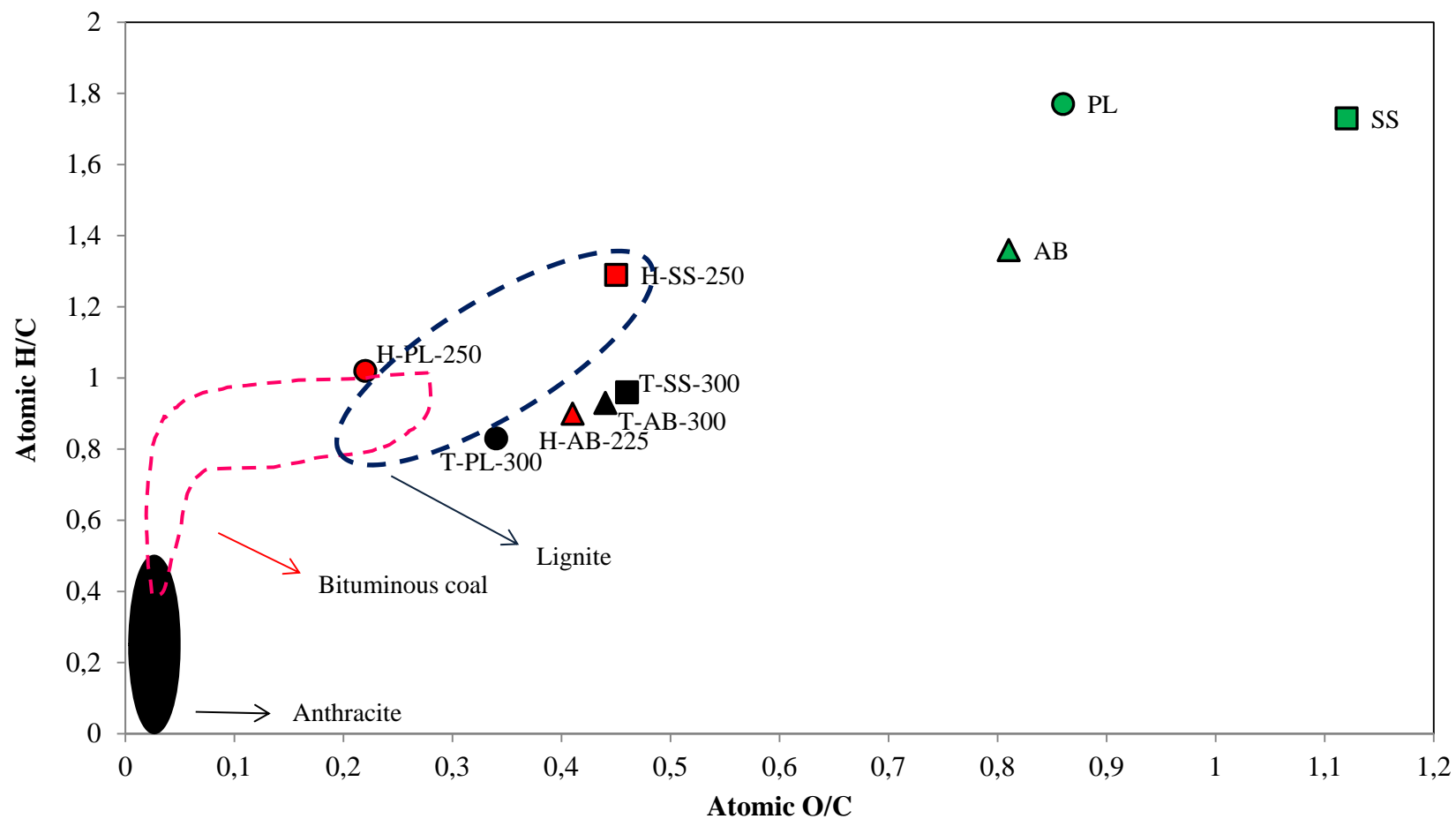
# Results & Discussion



## Van Krevelen Diagram

PL: Polultry litter  
SS: Sunflower stalk  
AB: Seaweed

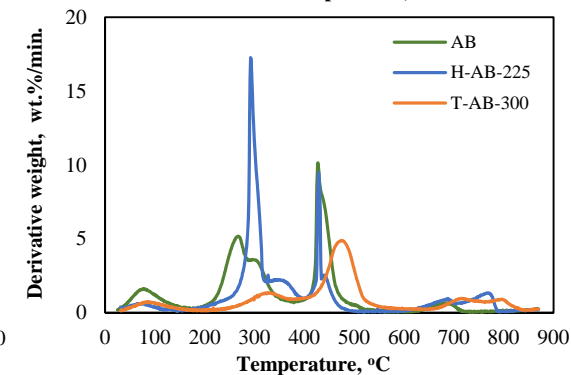
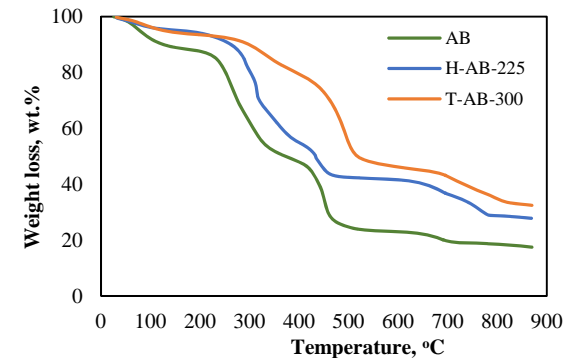
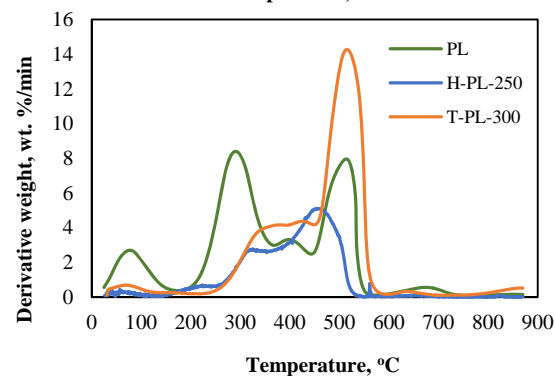
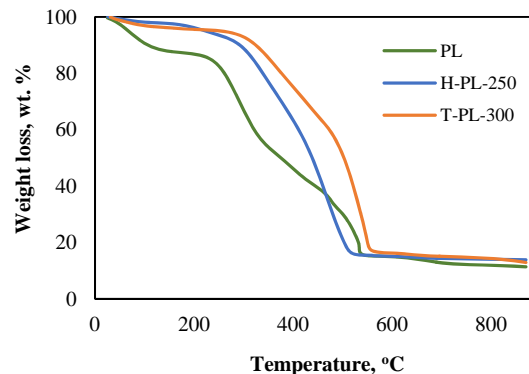
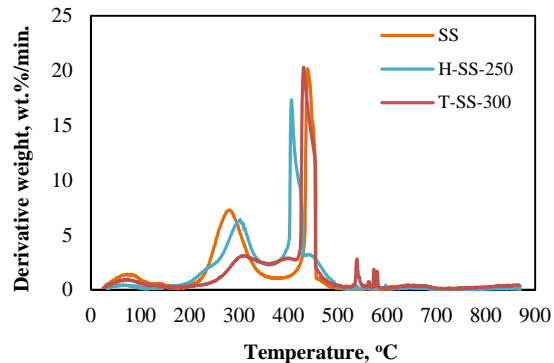
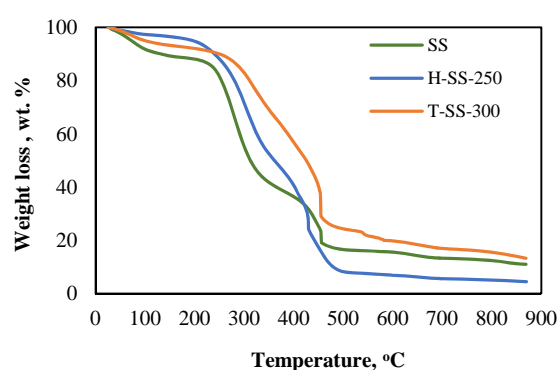
H: HTC biochar  
T: Pyrolysis biochar



# Results & Discussion



## Combustion behavior



	SS	H-SS-250	T-SS-300	PL	H-PL-250	T-PL-300	AB	H-AB-225	T-AB-300
Peak temperature, °C	281;439	310;406	431	290; 513	454	515	266; 427	292; 429	474
Combustion	7.27;20.15	3.10;17.30	20.29	8.40; 7.96	5.1	14.27	5.16; 10.13	17.25; 9.47	4.88
Reactivity, %/min.°C	3.589	2.631	4.708	2.224	1.123	2.771	2.156	4.057	1.03
Burnout, %/min	462	485	472	543	517	564	475	459	519
Ignition, °C	233	218	258	235	268	282	228	261	273



# Conclusion

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- Hydrothermal carbonization is a promising method to produce biochar with high quality.
- The temperature is the main parameter effecting the yield and energy density
- Application on wet biomass
- Lower ash content biochar
- Higher energy density than biochar obtained from pyrolysis

# Thank you for listening !

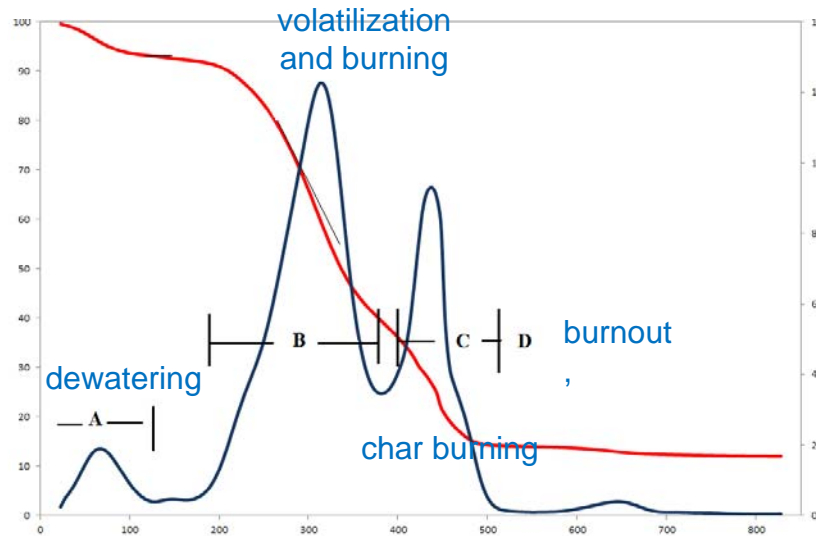


We would like to acknowledge the contribution of the COST Action TD1107 (Biochar as option for sustainable resource management)

# The experiments designed by CCD

Run	Parameter 1 Temperature(°C)	Parameter 2 Duration (min)	Parameter 3 Biomass: water ratio
1	150	150	0.30
2	175	60	0.15
3	175	60	0.45
4	175	240	0.15
5	175	240	0.45
6	212	0	0.30
7	212	150	0.05
8	212	150	0.30
9	212	150	0.30
10	212	150	0.30
11	212	150	0.30
12	212	150	0.30
13	212	150	0.30
14	212	150	0.55
15	212	300	0.30
16	250	60	0.15
17	250	60	0.45
18	250	240	0.15
19	250	240	0.45
20	275	150	0.30

# Thermogravimetric analysis



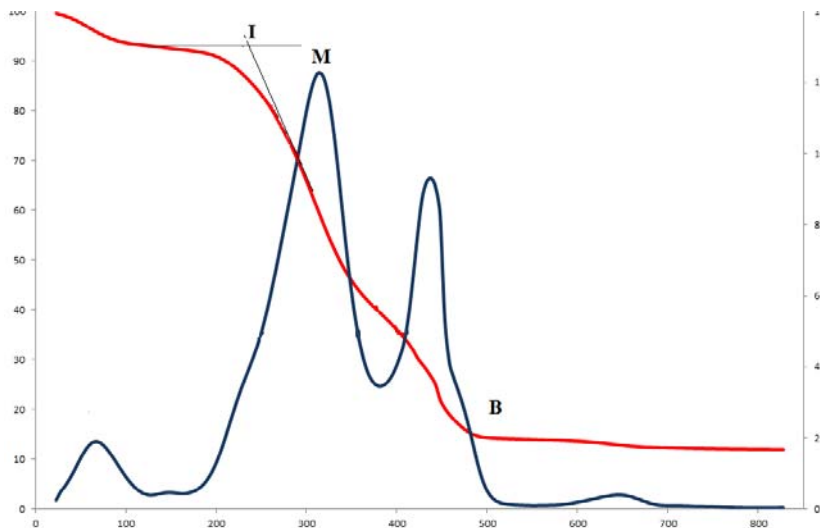
## Conditions

Heating rate: 20 °C /min

Combustion atmosphere: Air

Air flow: 100 mL / min

Sample amount: ~ 5- 10 mg



**I**, ignition temperature

**B**, burnout temperature, the rate of weight loss become <1 wt.%/ min

**M**, highest  $dm/dT$  value

**Reactivity** = 100 x maximum combustion rate / peak temperature

# Results & Discussion



## Quadratic models

$x_1$ : Temperature

$x_2$ : Duration

$x_3$ : Biomass: water

$Y_i$ : mass yield, energy yield

$$Y_i = \beta_0 + B_1 \cdot x_1 + B_2 x_2 + B_3 \cdot x_3 + B_{11} \cdot x_1^2 + B_{22} \cdot x_2^2 + B_{33} \cdot x_3^2 + B_{12} \cdot x_1 \cdot x_2 + B_{13} \cdot x_1 \cdot x_3 + B_{23} \cdot x_2 \cdot x_3$$

$Y_i$		$B_0$	$B_1$	$B_2$	$B_3$	$B_{12}$	$B_{13}$	$B_{23}$	$B_{11}$	$B_{22}$	$B_{33}$
Mass Yield	AB	+46.89	<b>-8.11</b>	-1.15	-4.191E-3	-0.66	+0.19	-0.37	+0.78	-0.027	+0.039
	PL	+46.67	<b>-7.97</b>	-0.22	-0.47	+0.050	-0.33	+0.065	+0.48	+0.44	0.66
	SS	+59.63	<b>-9.63</b>	<b>-2.87</b>	+0.47	<b>-1.95</b>	-0.14	+0.055	<b>-1.44</b>	-0.39	+0.13
Energy	AB	+1.67	<b>+0.16</b>	+0.020	-9.985E-4	-0.025	-0.015	+0.000	-0.045	-0.007445	+1.379E-3
	PL	+1.54	<b>+0.17</b>	+0.019	+0.019	+1.250E-3	+1.250E-3	-0.016	+0.012	-5.359E-3	-2.367E-4
Density	SS	+1.48	<b>+0.16</b>	+0.041	-8.587E-3	+0.011	+0.016	+3.750E-3	+0.032	-0.024	+1.600E-3