

# Agricultural wastes for wastewater treatment

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- **Introduction**
- **Goals**
- **Methodology**
- **Results and discussion**
- **Conclusion**
- **Future work**

## Agriculture and alimentary industry

### Solid wastes

### *Dried fruits and cereals*



### Portugal production

**Walnuts** > 4,000 ton/year and imported 1,000 ton.

**Peanuts**  $\approx$  10,000 ton/year of importation and 2,500 ton/year of exportation.

## Shells

### *Dried fruits and cereals*

According to INE data - 1 kg of walnuts or peanuts  $\approx$  0.27 kg of shells.

In **2013** the shells estimation is **1,150 ton for walnuts** and **2,025 ton for peanuts**.



## Industry activities

**Metal cleaning, paint, electroplating, plating baths paper and wood production, air conditions and fertilizer industries**

**Industrial wastewater** - heavy metal such as copper, cadmium, chromium, cobalt, iron, lead, nickel, and zinc.

Minimum quality of a superficial water -  $0.1 \text{ mg.L}^{-1} \text{ Cu (II)}$

Irrigation water -  $5 \text{ mg.L}^{-1} \text{ Cu (II)}$



## ***What to do with solid waste and wastewaters ?***

### **Wastewater**

- chemical precipitation,
- coagulation/flocculation,
- ion exchange,
- membrane process.

***Quite expensive***

Adsorption

### **Solid wastes - dried fruits shells**

- manufacture of animal feed
- fertilizer
- land cover

***Other option***

Adsorbents

### **Goal**

To investigate and describe the equilibrium of sorption of metals (e.g. Cu (II) and Ni (II)) on walnut and peanut shells in order to obtain the right adsorbent amount and the suitable operating conditions.

## Absorbents

**Walnut** (*Juglans regia L*) shells

**Peanut** (*Arachis hypogaea L.*) shells



natural adsorbents

**Collected from source separated domestic wastes**

## Characterization

### Granulometric analysis



### Physical analysis



## Absorbents - Treatments

### Absorbents experimental conditions tests

Treatment	Parameter
Natural	-
Washing with distilled water and drying	Temperature: 60 and 100 °C
Sieving	Different particles size: 0,5 and 1,4 mm
Carbonization	Temperature: 550°C



**Carbonization**



**Walnut shells**



**Peanut shells**



## Adsorption tests

**Batch mode** varying the absorbents dose or the metal concentrations.

Working volume of 100 to 150 mL in an orbital agitator with a mixing rate around 150 rpm



**Vacuum Filtration**

**Titration - Iodometric**

## Shells amount estimation

**Walnuts** - 0.56 kg of shells per kg

**Peanut** - 0.26 kg of shells per kg.

INE data - 1 kg of walnuts or  
peanuts  $\approx$  0.27 kg of shells.

## Granulometric analysis

### Equivalent diameter > 2 mm

94.1 % by weight of walnut shells

80.7 % by weight of peanut shells



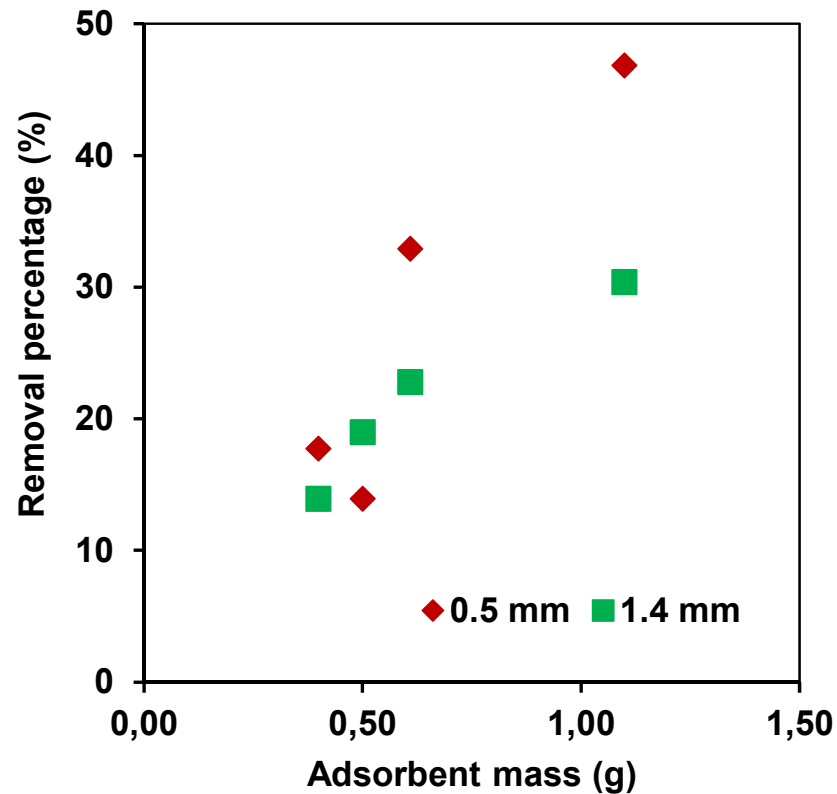
## Physical analysis

### Peanut and walnut shells characteristics

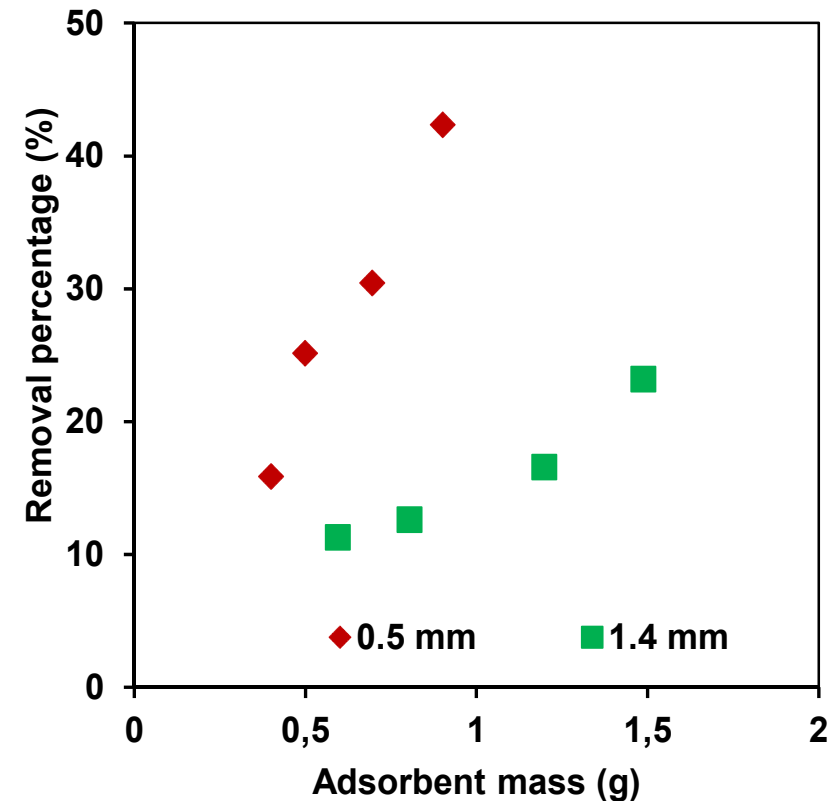
Shells	% weight		
	Moisture	Volatile matter	Ash
Peanut	5.56	94.28	5.38
walnut	10.52	99.01	0.89

## Adsorption tests

### Effect of particle size and adsorbent dose



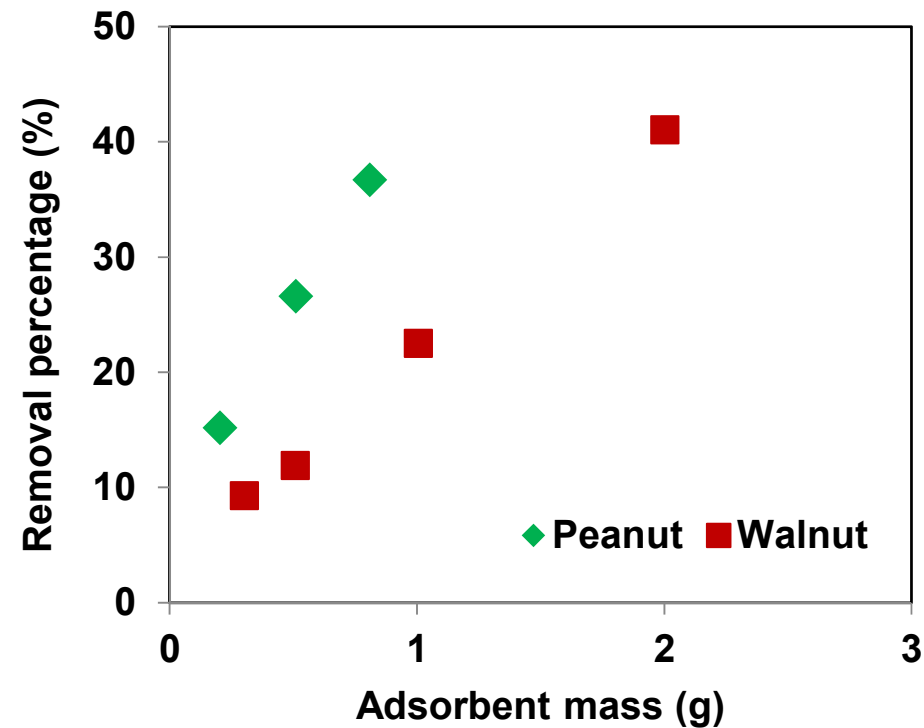
Dry peanut shells at 60 °C with a contact time = 15 min



Dry walnut shells at 60 °C with a contact time = 30 min

## Adsorption tests

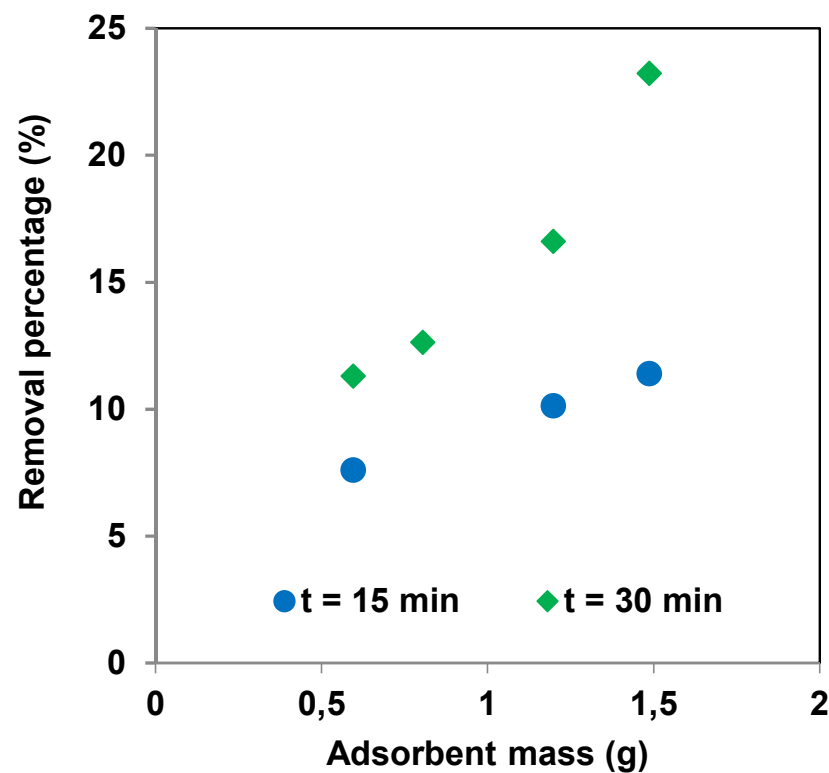
### Effect of adsorbent type



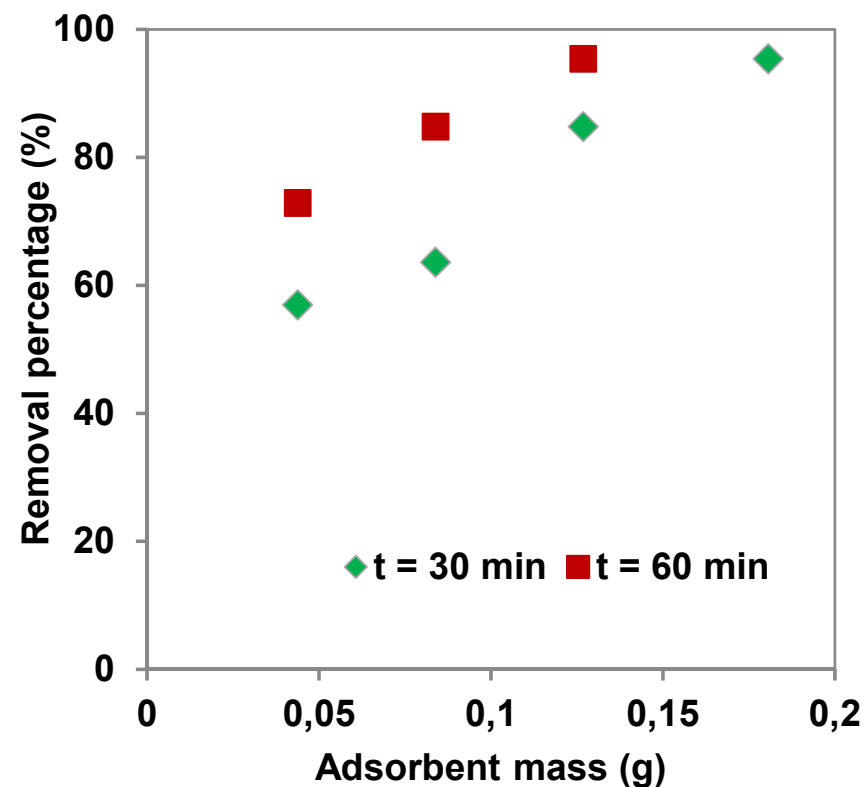
**Adsorption efficiency of Cu (II) onto dry shells at 60 °C**

## Adsorption tests

## Effect of time



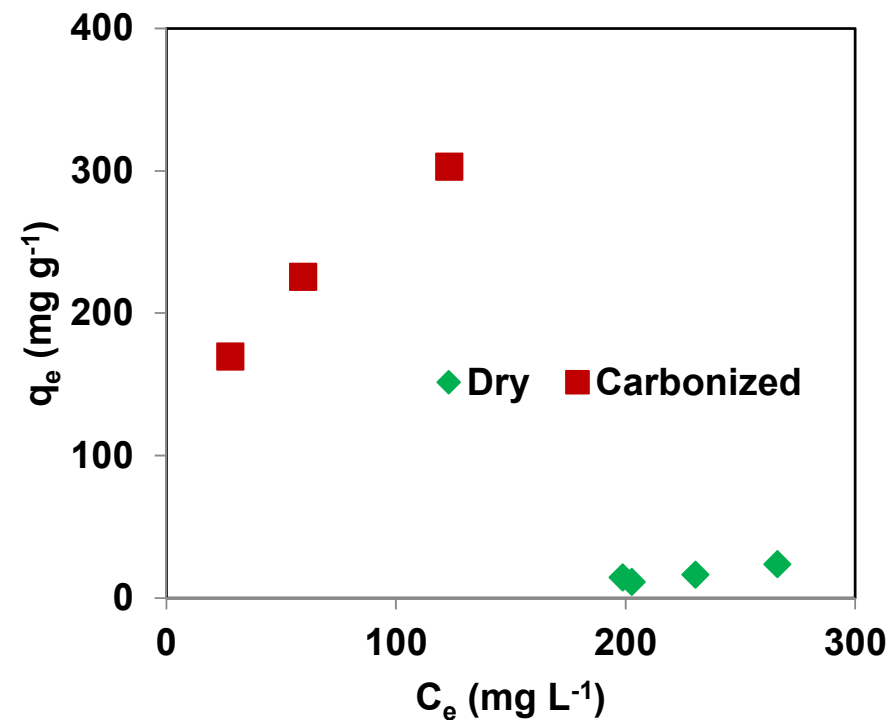
**Dry walnut shells**



**Peanut carbonized**

## Adsorption tests

## Effect of adsorbent treatment



## Carbonized and dry peanut shells

## Adsorption tests

## Isotherms

### Langmuir

- ✓ monolayer adsorption of solutes;
- ✓ surface comprised of a finite number of identical sites with homogeneous adsorption energy.

### Freundlich

- ✓ empirical expression;
- ✓ heterogeneity of the surface
- ✓ multilayer adsorption to the binding sites located on the sorbent surface.

### Linear form

$$\frac{1}{q_e} = \frac{1}{q_{max} K_L C_e} + \frac{1}{q_{max}}$$

$q_{max}$  - the maximum adsorption capacity ( $\text{mg g}^{-1}$ ),  
 $K_L$  - the affinity of binding sites and is related to the energy of sorption, ( $\text{L mg}^{-1}$ )

$$\log q_e = \frac{1}{n} \log C_e + \log K_F$$

$K_F$  ( $(\text{mg g}^{-1})(\text{L mg}^{-1})^{1/n}$ ) - capacity of adsorption  
 $n$  - intensity of adsorption,

**$n$**   
 2–10 good,  
 1–2 moderately difficult,  
 < 1 poor adsorption



## Adsorption tests

### Isotherms peanut shells

Adsorbent	Time (min)	Freundlich isotherm			Langmuir isotherm		
		$K_F$ ((mg g <sup>-1</sup> )(L mg <sup>-1</sup> ) <sup>1/n</sup> )	n	R <sup>2</sup>	$K_L$ (L mg <sup>-1</sup> )	$q_{max}$ (mg g <sup>-1</sup> )	R <sup>2</sup>
Natural (Ø = 1,4 mm)	30	0.061	0.585	0.935	-	-	-
Drying (Ø = 1,4 mm)	30	0.188	0.857	0.940	-	-	-
Carbonized	30	1.274	0.539	0.974	5.523	263.15	1
	60	1.491	0.546	0.886	0.152	303.03	0.918
Peanut shells (W+D+M +S<30 µm)		3.09	2.97	0.022	25.39	Witek-Krowiak et al., 2011	

## Adsorption tests

### Isotherms

walnut shells

Adsorbent	Time (min)	Freundlich isotherm		
		$K_F$ ((mg g <sup>-1</sup> )(L mg <sup>-1</sup> ) <sup>1/n</sup> )	n	R <sup>2</sup>
Natural (Ø = 1,4 mm)	30	0.968	2.77	0.998
Drying (Ø = 1,4 mm)	15	1.246	1.97	0.998
	30	9.985	6.79	0.895

Walnut shell (W+D 80°C + S < 1 mm)	0.256	2.27	Feizi, <i>et al.</i> , 2015
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- The **selected adsorbents remove Cu (II)** from water.
- The **highest Cu (II) removal** was obtain with **carbonized peanut shells**.
- The amount of **Cu (II) adsorbed increased** with sorbent **particle size decrease**.
- The **adsorption equilibrium** was best described by the ***Freundlich*** isotherms.

- The **pre-treatment adsorbents** increases the cost - **conditions optimization**;
- The work is still in progress with **other metals (Ni, Cr, Al or Pb)** and **shells (shrimps or eggs)**;
- Application of the **adsorbents to remove other** pollutants like dyes from wastewater.

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the wastes.**

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# Thank you for your attention

## Questions ?

