HERAKLION 2019



Two-Stage Batch Adsorber Optimisation for Malachite Green Removal Using Activated Waste Biomass

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Outline

- Introduction and Objectives
- Experimental Systems
- Modeling Theory and Models
- Results
- Conclusion

INTRODUCTION



Waste Biomass

Sources:

- Straws (wheat, rice husk...)
- Shells (coconut, pistachio, palm kernel, walnut...)
- Fruit stones (olive, dates, peaches, mango...)
- Pine, wood, bamboo, lignin....





Source: filtrasystems

Activated Carbons

- Activation: controlled • oxidation of carbon atoms in the raw material – expanding the internal surface area
- Physical and chemical activation
- Strong physical adsorption and chemical reactions
- Low density •
- High porosity: pore volume (0.2 to 0.6 cm³/g) Brunauer- Emmett- Teller (BET): surface area (500 to 1500 m²/g) •

Source:yet2.com marketplace





Dyes (Malachite Green)

- Dyes are applied to textiles, paper, leather, food, drugs, cosmetics and other products.
- products.
 More than 2000 dyes are currently used (reactive orange, congo red,
- Majory dervice mail achite greekens (increase in COD, decrease in DO, toxic, carcinogenic, mutagenic, prevent light penetration into water)

Malachite Green



 $C_{23}H_{25}ClN_2$



Source: Alibaba.c om

Adsorption



Activated Carbon

Pores

Objectives

- Characterize date stones
- Develop suitable activation methods
- Test and compare the performance of the activated date pits adsorbents on the target pollutant of Malachite Green
- Understand the adsorption mechanisms
- Design a two stage adsorption system

The waste product of the seedless date products industry is the date "pit" or date "stone" which is a sustainable and economical resource that can be used to enhance the treatment of water.

EXPERIMENTAL SYSTEMS



Experimental Systems





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Experimental Systems (Cont.)

Properties of the date

stônestone	Total volume of pore (cm ³ /g)	Mean pore diameter (nm)	BET surface area (m²/g)
NDS	0.21	2.31	85.74
PADS	0.55	2.48	908.6

Adsorption Tests

- Carried out at 20°C
- 3g of adsorbent with MG
- Shaking at 250 rpm
- Measuring initial and final concentr
- Mass balance

(amount of dye adsorbed = amount of dye removed)



Two-Stage Batch Adsorber Optimisation



MODELING THEORY AND MODELS



Isotherms

- qe :amount of contaminant adsorbed
- Ce: equilibrium concentration of the contaminant

Models:

- Langmuir
- Freundlich
- SIPS

Model information:

- Prediction
- Type of adsorption
- Molecular interaction



Errors:

SSE, chi-square statistic, gsquare statistic, relative errors, absolute errors, percentage errors, and 1 fractional errors, etc.

Isotherms (Cont.)

Langmuir isotherm

$$q_{e} = \frac{q_{m} b C_{e}}{1 + bC_{e}}$$

- •• (mg/gg/gg)gadscorption capacitycoonstant
- b (L/mag) e en er gy constant
- Assumptions:
- Ideal gas behavior of adsorbate
- Molecules do not interact among each other
 - Uniform monolayer adsorption

Freundlich isotherm $q_e = k_F C_e^{\frac{1}{n}}$

- axd sorption capacity
 constant
- m: constant (ty stanface heterogenieity)

Assumptions:

- Empirical equation
- Multilayer adsorption
- Heterogeneous system

SIPS isotherm $q_{e} = \frac{q_{m} K_{LF} C_{e}^{1/n_{LF}}}{1 + K_{LF} C_{e}^{1/n_{LF}}}$

- kLFFLEOnstant
- · :"isothernmexponent

Assumptions:

- Combination of Langmuir and Freundlich
- High concentrations ~ Langmuir

RESULTS



Isotherm Study Parameters

Isotherms		PADS	RDS
	b	0.174	0.00583
Langmuir Model	q _m	64.7	29.5
	SSE	52.4	3.53
	k _F	26.7	1.22
Freundlich Model	1/n	0.165	0.476
	SSE	404	16.8
	K _{LF}	14.8	0.203
SIPS Model	a _{LF}	0.221	0.0016
	b _{LF}	0.840	1.34
	SSE	36.2	1.30

Isotherm Study Results (Cont.)

SIPS Isotherm



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NDS

PADS



Single Stage vs Two Stage Adsorption

Amount of PADS adsorbent required

Removal %	99.50%		95%	
C _o (mg/L)	S (g)	S1+S2 (g)	S (g)	S1+S2 (g)
50	11.5	2.5	2.2	1.2
100	13.5	3.5	3.1	2.1
150	15.1	4.2	3.9	2.8
200	16.4	5.0	4.7	3.6
250	17.7	5.9	5.5	4.2
300	18.8	6.4	6.2	5.0
350	19.9	7.5	7.0	5.5
400	21.0	8.3	7.7	6.2
450	22.0	9.2	8.5	7.0
500	23.0	10.0	9.2	7.5 1

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CONCLUSION



Conclusion

- Date pits are hard lignocellulosic materials with high carbon content and low impurities, and are excellent precursors for the production of activated carbons
- Langmuir-Freundlich (SIPS) isotherm is the best fit among the studied isotherms for both adsorbents and should be used for design purposes
- The total amount of adsorbent increases with increasing initial concentration of malachite green dye, higher removal rate, and with an increase in the dye solution volume
- The two-stage system resulted in a decrease of around 33% of the total adsorbent requirement compared to the one-stage system to remove the same amount of MG
- For a commercial treatment process, the economic comparison between the adsorbent saving versus the increased cost of the two-stage adsorber over the single-stage adsorber needs to be investigated



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Thank You Any Questions?