

Synthesis of magnetic biochar for utilization in Fenton based process

Gozde Duman Tac, Jale Yanik

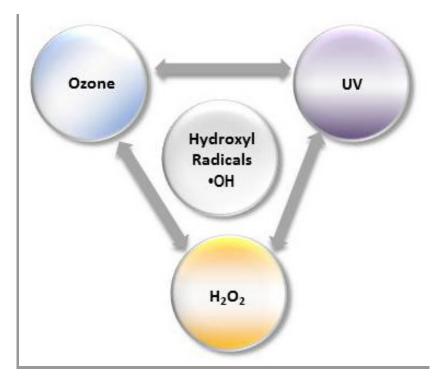
Ege University, Faculty of Science, Chemistry Department,Izmir/ TURKEY

Dye wastewater treatment

- Used in the textile, cosmetic, pharmaceutical and food industries
- High volumes of wastewater during operation
- Complex structure, resistant to biodegradation



Advanced Oxidation Process



Based on chemical oxidation by forming very reactive species such as hydroxyl radicals (·OH) Degrades organic pollutants completely to harmless chemicals, mainly CO_2 and H_2O □Feasible option for biologically persistent wastewater Widely recognized as highly efficient treatments for recalcitrant wastewater

Fenton Process

The chemical oxidation of organic compounds by H₂O₂ The chemical oxidation of organic compounds by H₂O₂ using Fe ions² using Fe ions as a catalyst

$$Fe^{2+} + H_2O_2 \rightarrow Fe^{3+} + OH^- + OH^{\bullet}$$

 $Fe^{3+} + H_2O_2 \rightarrow Fe^{2+} + H^+ + OH_2^{\bullet}$

- Particularly atteraized because of
 - •• the low cootsts
 - •• the ladko of toxity it the the rest agents
 - ·· the simplicity foll the healogology

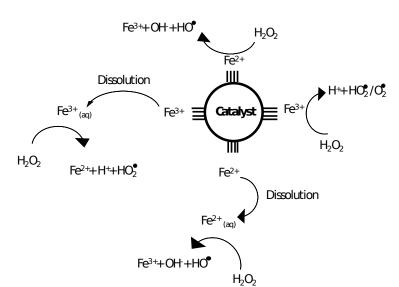
Fenton Process

Disadvantages of homogeneous catalysis

 \geq 50–80ppm of ions needed in solution

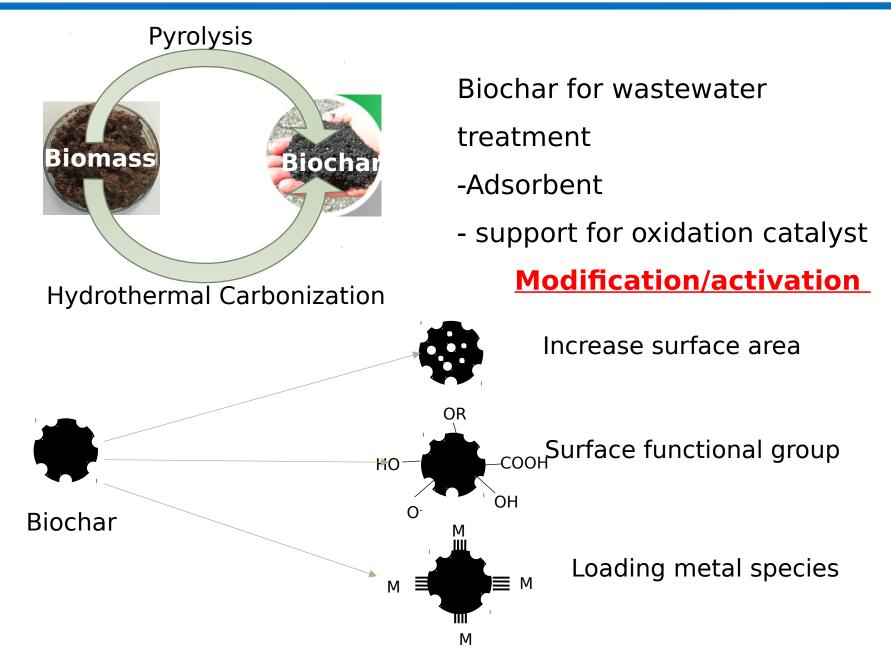
- *above* environmental regulations to dump directly into the environment => [Fe]max =2 ppm
- the removal/treatment of the sludge-containing metal ions at the end of treatment
- Not recyclable

Pure Metal oxides; poor stability, inert activity, etc.

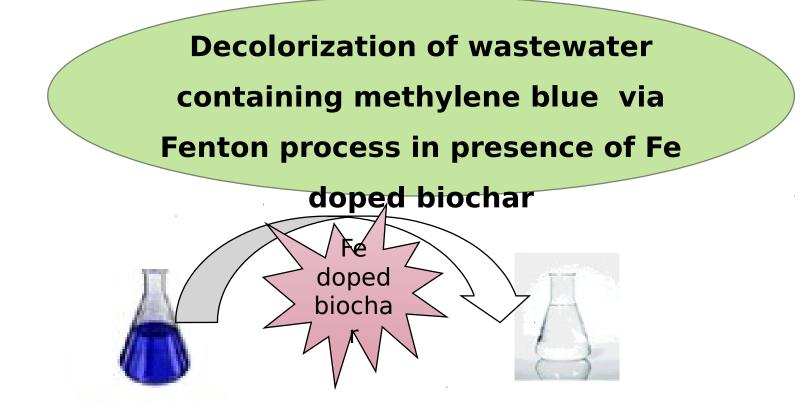


Heterogeneous catalyst

Biochar



PURPOSE



Synthesis and characterization of Fe loaded biochars

- Catalyst screening
- Parametric study on Methylene blue removal

ANALYSIS

ermination of Methylene blue (MB) removal



Performed by measuring the absorbance of the methylene blue on the transmission of the absorbance wavelength of the absorbance wavelength of the absorbance wavelength of the absorbance wavelength of the absorbance of the absorb

The wavelengths $\lambda = 664$ nm for MB, Removal efficiency (de-colorization) was calculated

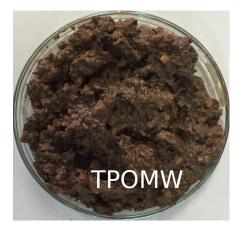
□ Bemoval efficiency (de-colorization) was

calculated by MB Removal(%) = $\frac{m_0 - m_f}{m_0} \times 100$ MB Removal

where m_0 and m_f were initial and final concentration where m_0 and m_f were initial and final of MB concentration of MB

MATERIALS AND METHODS

Biomass: Two phase olive mill waste(TP)



Fe source:

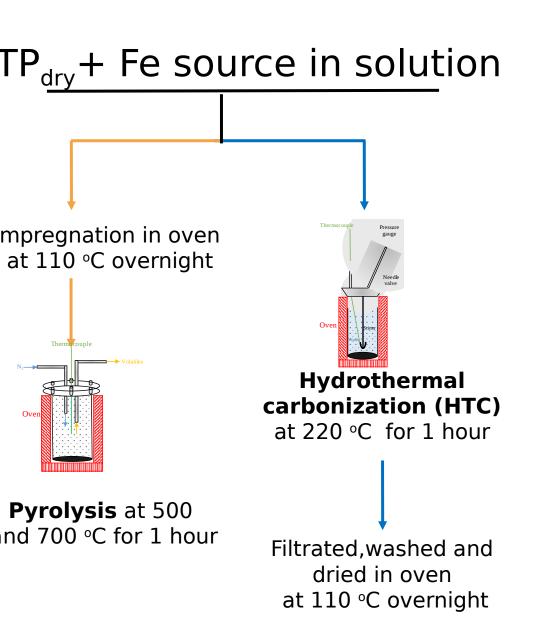
 $-FeSO_4(Fe)$,

- -Red Mud (RM): Fe rich (containing
- 38% Fe_2O_3) waste sludge from
- aluminum company
- -Acidified Red Mud (ARM): Dissolved in
- 10 % HCl solution

Properties of TPOMW, %

Moisture	66.4			
Proximate analysis, wt % (db)				
Ash	3.8			
Volatile matter	68.5			
Fixed carbon	27.7			
Ultimate analysis, wt % (db)				
С	51.47			
Н	7.02			
N	1.09			
5	0.13			
0	36.51			

MATERIALS AND METHODS



Pyrolysis	60.2
Pyrolysis	55.7
HTC	49.6
Pyrolysis	68.9
Pyrolysis	57.2
HTC	81.7
Pyrolysis	72.0
Pyrolysis	61.3

Magnetic properties



**based on initial biomass amount

MATERIALS AND METHODS

enton Reaction Experiments



Batch experiments

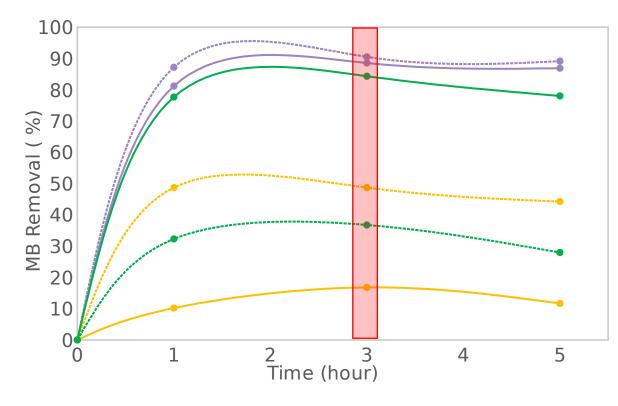
- 250 ml erlenmayer flask
- 150 rpm shaking

Tested parameters

- Catalyst type
- Day light and under dark
- > Concentration of H_2O_2
- ≻ pH
- MB concentration

RESULTS-Comparison of Fe source

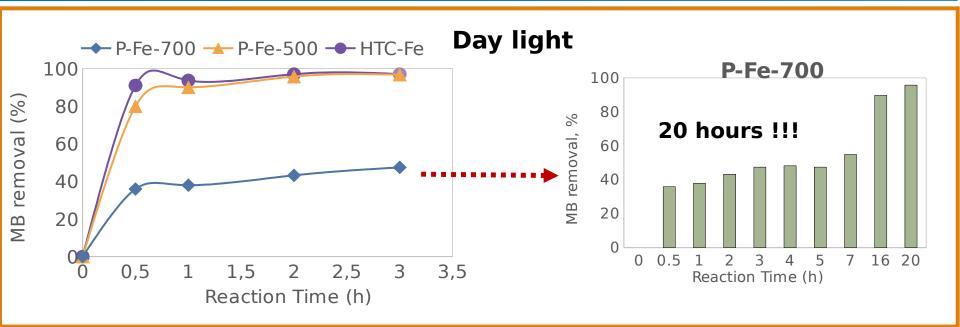
----- P-Fe-500

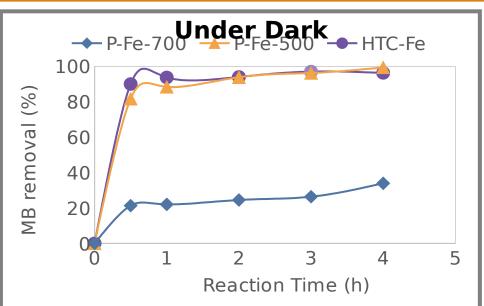


- RM based biochars had low activity.
- The use of ARM instead of RM improved the removal of MB.
- Pyrolysis temperature for
 Fe based biochars had
 significant effect.

Conditions: 100 ppm MB, 10 mM H_2O_2 , daylight, 150 rpm shaker, pH was adjusted to 3

RESULTS- FeSO₄ based catalyst

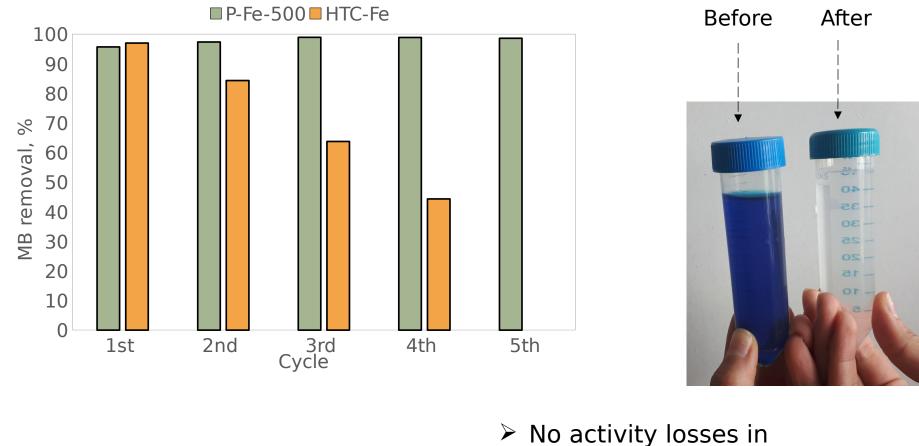




Fe content of effluent			
water, ppb			
P-Fe-500	128		
P-Fe-700	4		
HTC-Fe	357		

RESULTS- Cyclic usage of catalyst

Fenton oxidation with P-Fe-500



No activity losses in case of P-Fe-500 after 5 cycle.

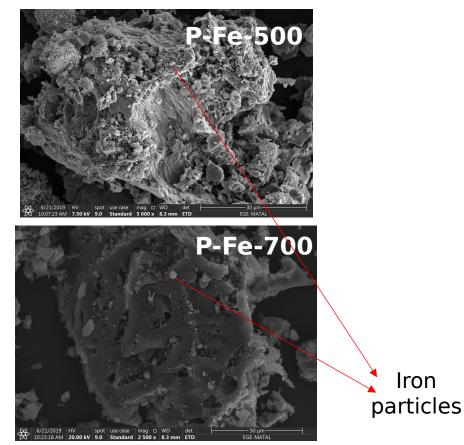
Conditions: 50 ppm MB, 10 mM H_2O_2 , daylight, 150 rpm shaker, no pH adjustment

RESULTS- FeSO₄ based catalyst

Inorganic content, %

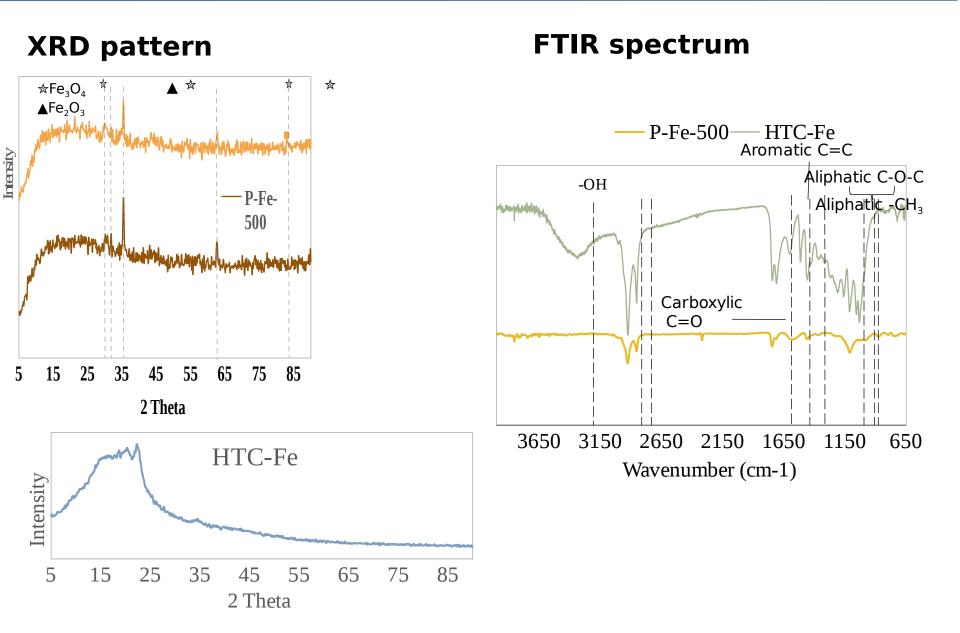
SEM images

	P-Fe-500	P-Fe-700	HTC-Fe
Fe	22.02	25.86	1.35
Al	0.06	0.07	0.07
Si	-	0.02	0.03
Mg	0.09	0.11	-
Na	0.29	0.32	0.12
Ca	0.27	0.32	0.09
Κ	3.22	4.01	0.11

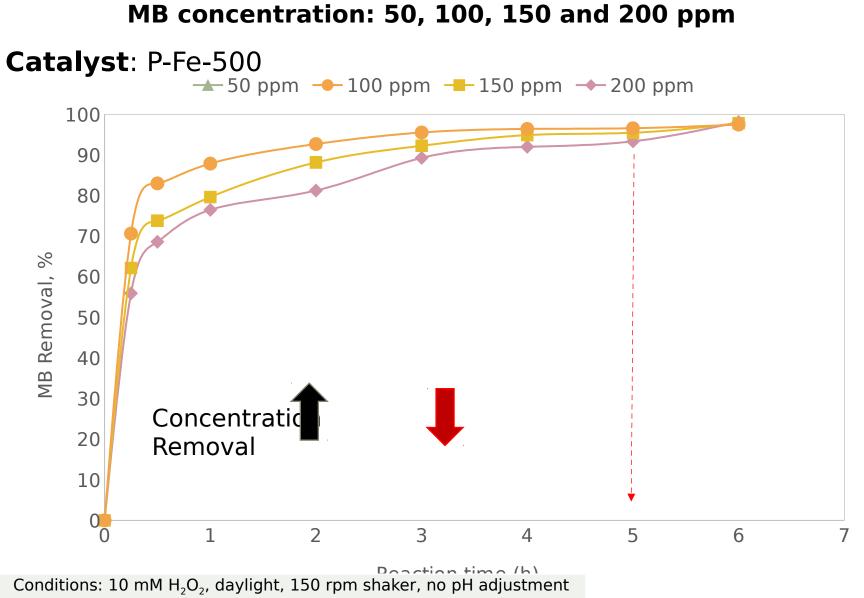


Loading of Fe failed by hydrothermal carbonization

RESULTS- FeSO₄ based catalyst



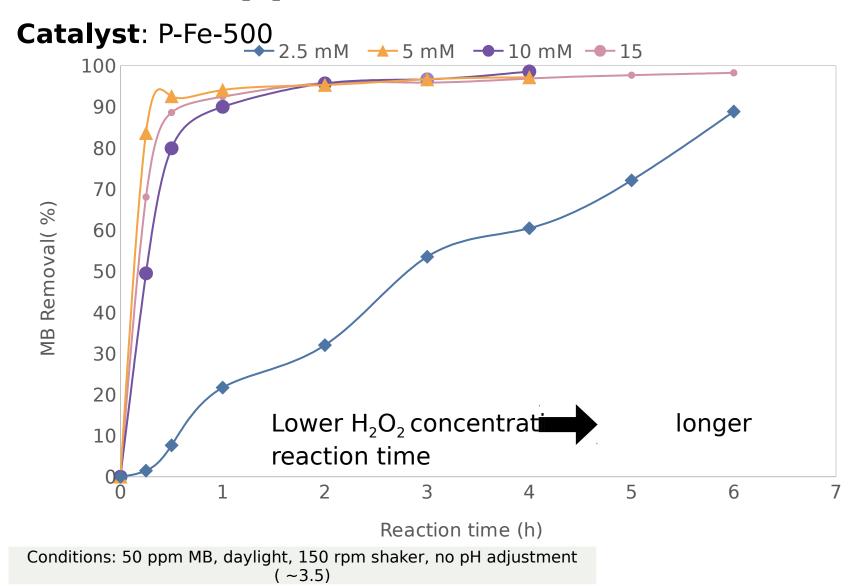
RESULTS- Parametric study



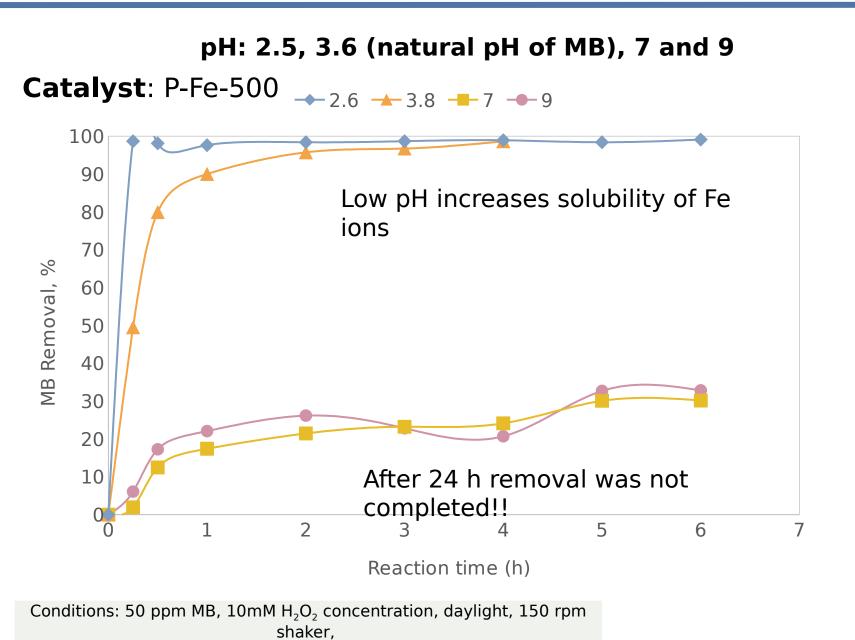
(~3.5)

RESULTS- Parametric study

Initial H₂O₂ concentration: 2.5, 5, 10 and 15 m M



RESULTS- Parametric study



Conclusion

-Fenton oxidation of MB was achieved with the catalysts prepared by TP.

-Release of Fe faciliates degradation of MB.

-P-Fe-500 had the highest activity stability in 5 cycles. Fe

concentration in effluent water is acceptable for direct dumping.

-pH is most effective parameter, which affect the solubility of Fe in wastewater.

-Biochars obtained by pyrolysis showed magnetic properties whereas magnetic biochar could not produced by HTC.

Biochar obtained from pyrolysis at lower temperature showed higher
 Ongoing studies focus on red mud to produce effective and stable activity than that at higher temperatures. catalyst,

independent from different pH.

In future work, different pollutants can be tested in their natural

pH.

THANK YOU FOR LISTENING...

- Special Thanks...
 PhD candidate Gulen Tekin
 Dr. Dogan Tac
 Dr. Raif Ilkac
 - Berkay Leskeri