



National Technical University of Athens

School of Chemical Engineering

Unit of Environmental Science & Technology

**NaOH ALKALINE
PRETREATMENT**

**FOR IMPROVEMENT OF
ENZYMATIC DIGESTIBILITY**

OF WHEAT STRAW

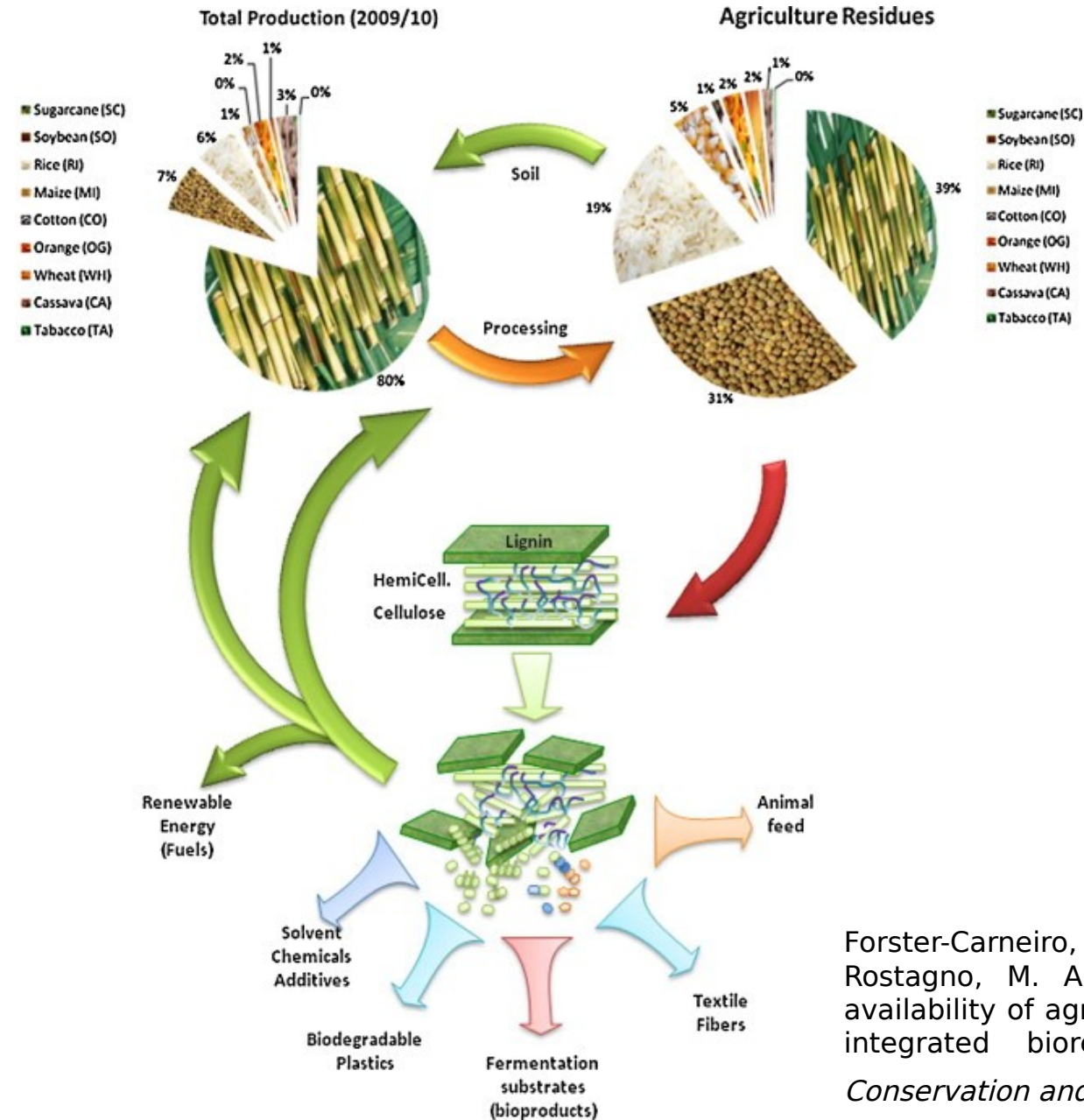
AS ALTERNATIVE SUGAR

J. Novakovic, N. Kontogianni, E.M. Barampouti, S. Mai, D.
Malamis, M. Loizidou

SOURCE



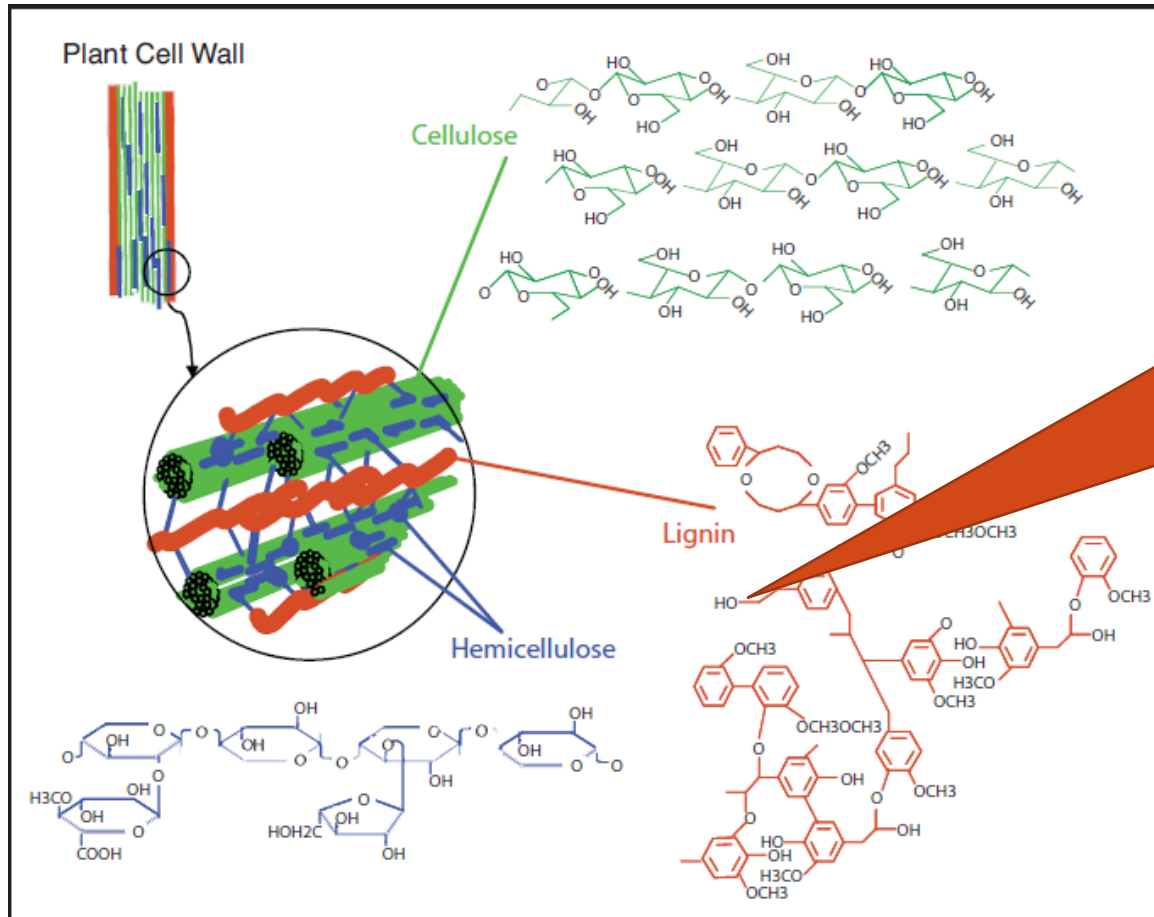
Agricultural Waste Biorefinery



Forster-Carneiro, T., Berni, M. D., Dorileo, I. L., & Rostagno, M. A. (2013). Biorefinery study of availability of agriculture residues and wastes for integrated biorefineries in brazil. *Resources, Conservation and Recycling*, 77, 78-88.



-Lignocellulosic material



<https://www.e-education.psu.edu/egee439/node/606>

The major barrier to the enzymatic hydrolysis of carbohydrates towards the production of fermentable sugars



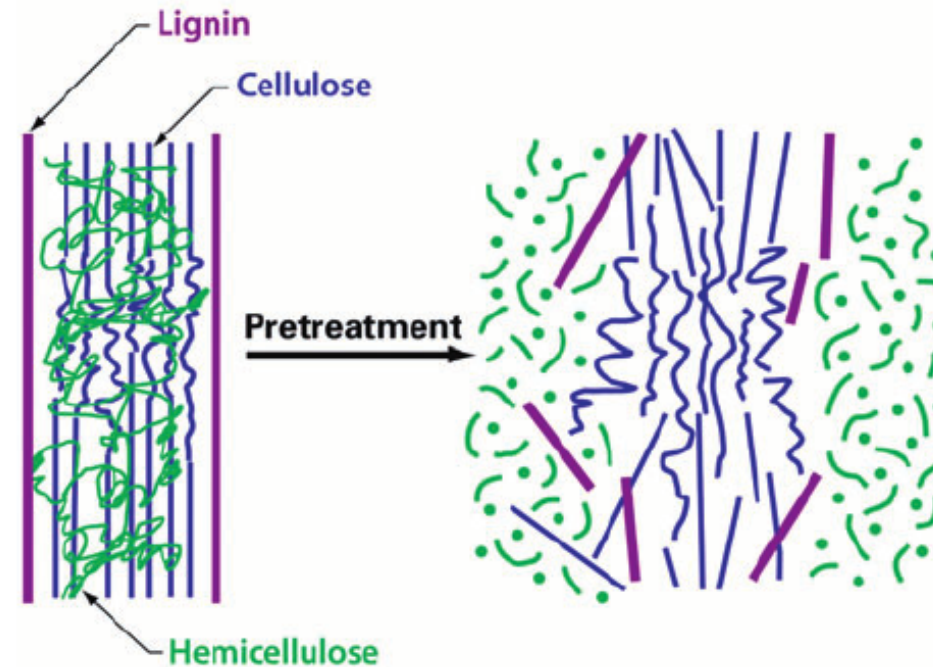
corn stover on a field credit: USDOE-NRE
<https://www.greenoptimistic.com>



7th International Conference on Sustainable Solid Waste Management, 26-29 June 2019, Heraklion, Crete Island, Greece



Pretreatments



Removal of lignin is favorable to reducing the recalcitrance of lignocellulose for enzymatic attack.

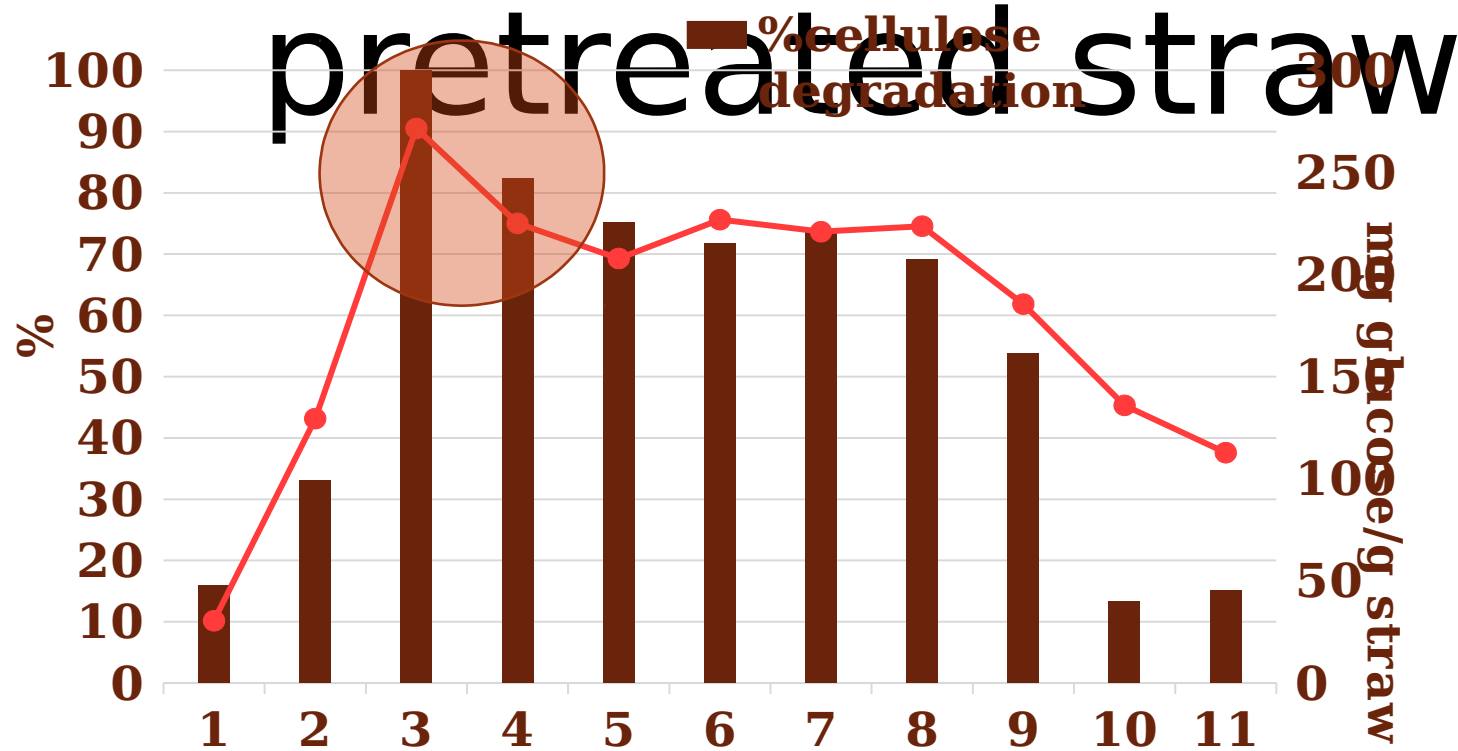


tested

A/A	Reagent	T	Solid :Liquid (w/w)	Time
i	H ₂ O ₂ (5%) NaOH (pH=11,5)	50°C	1:20	1h
ii	H ₂ O ₂ (10%) NaOH (pH=11,5)	50°C	1:20	1h
iii	NaOH 0.5M	50°C	1:10	96 h
iv	NaOH 0.5M	121°C	1:10	1h
v	CH ₅ N 25 %w/w	50°C	1:10	96 h
vi	CH ₅ N 25 %w/w	121°C	1:10	1h
vii	Na ₂ CO ₃ 0.5M	50°C	1:10	96 h
viii	Na ₂ CO ₃ 0.5M	121°C	1:10	1h
ix	NH ₃ 25 %w/w	50°C	1:10	96 h
x	NH ₃ 25 %w/w	121°C	1:10	1h



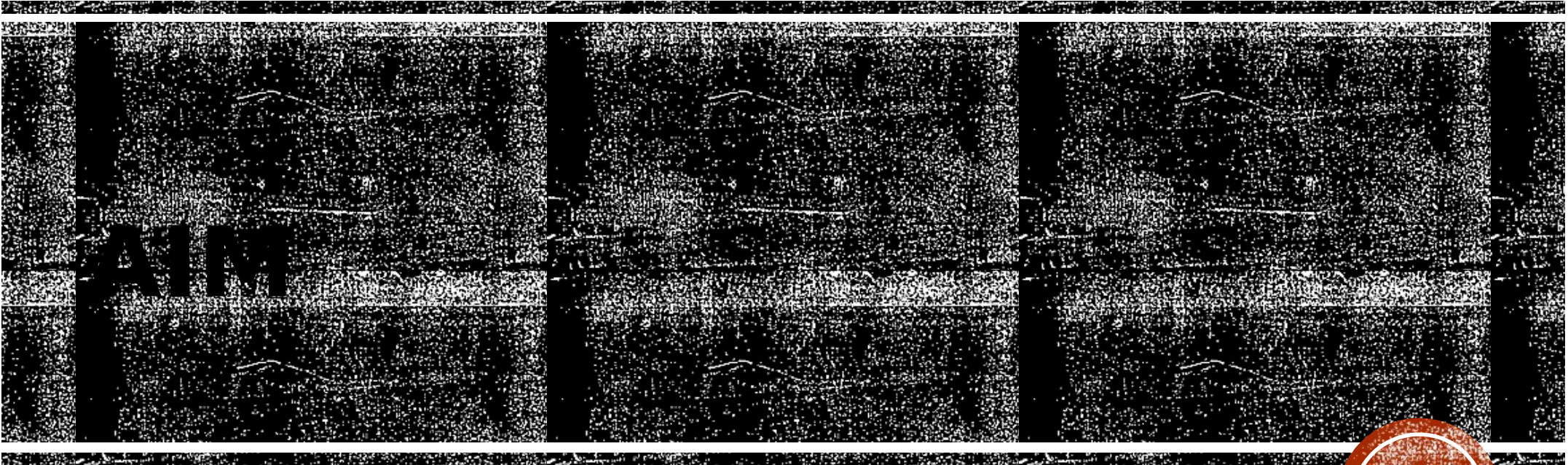
Saccharification of alkaline pretreated straw



Pretreatment methods

(i) alkaline peroxide 5%, **(ii) alkaline peroxide 10%**, **(iii) NaOH 0.5M**, (iv) NaOH 0.5M autoclaving, (v) methylamine 25 %w/w, (vi) methylamine 25 %w/w autoclaving, (vii) Na₂CO₃ 0.5M, (viii) Na₂CO₃ 0.5M autoclaving, (ix) ammonia 25 %w/w, (x) ammonia 25 %w/w autoclaving.





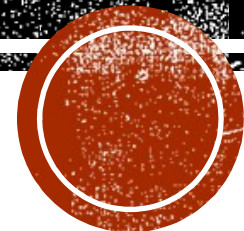
Optimisation of the NaOH pretreatment process along with the enzymatic hydrolysis in order to obtain more fermentable sugars and glucose recovery

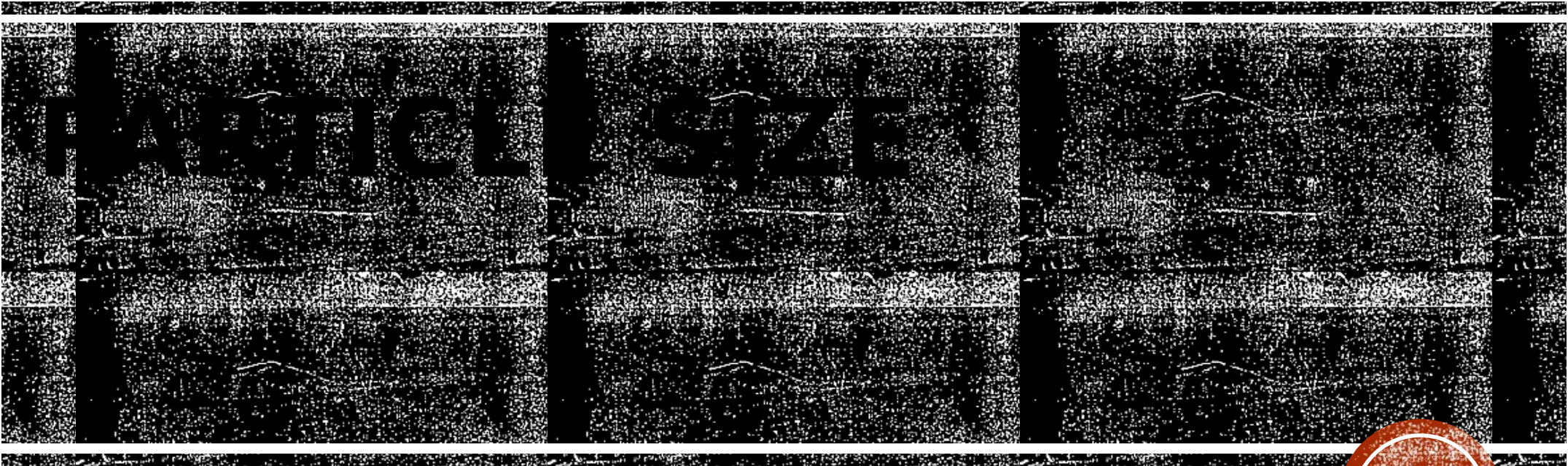
Raw material - Wheat straw

Origin: From Aspropyrgos province, Greece

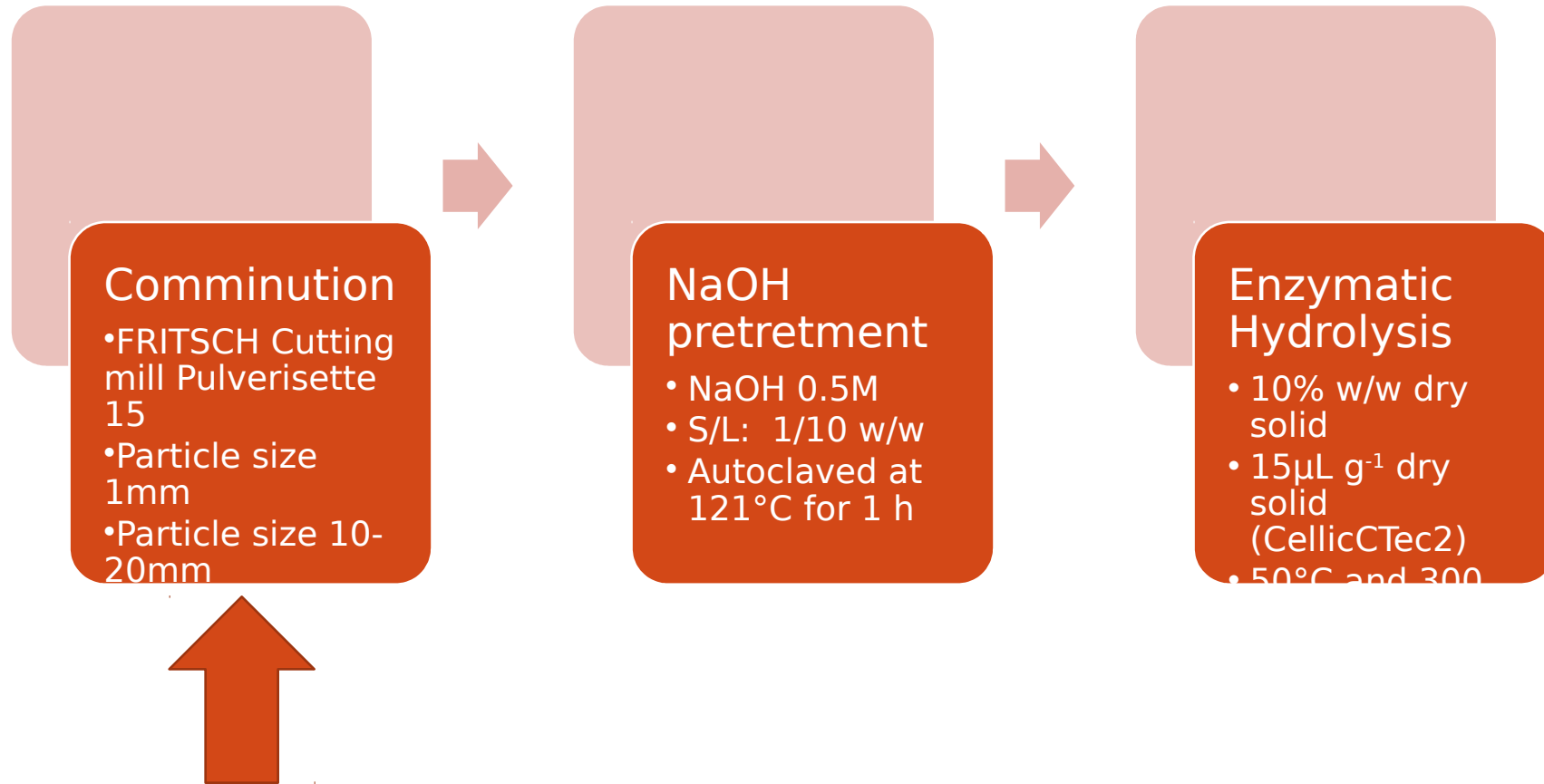
Parameter		Value (% w/w)
Cellulose		33.8
Hemicellulose		45.1
Lignin		16.4
	Klason lignin	15.4
	Acid-soluble lignin	1.0
Ash		4.7



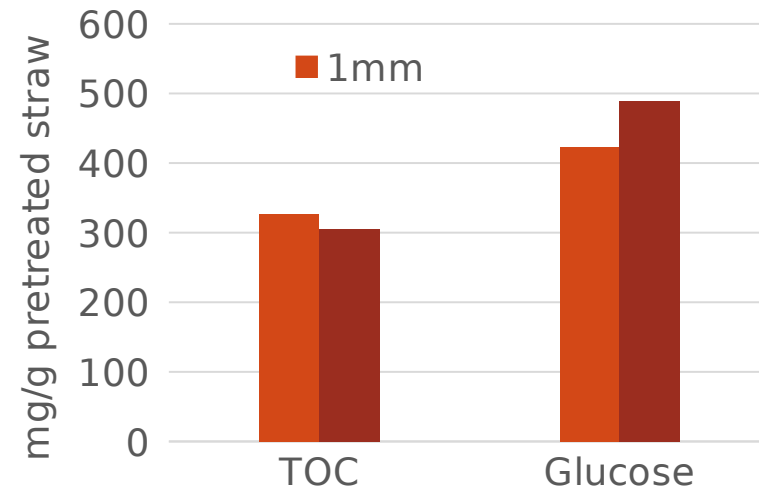
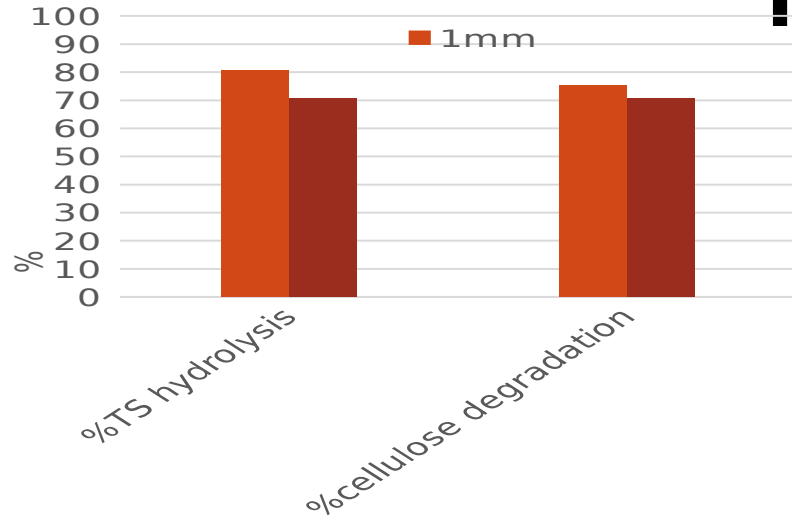




Particle Size- Experimental procedure



Particle Size



Conclusion

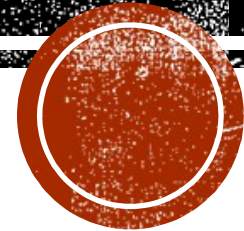
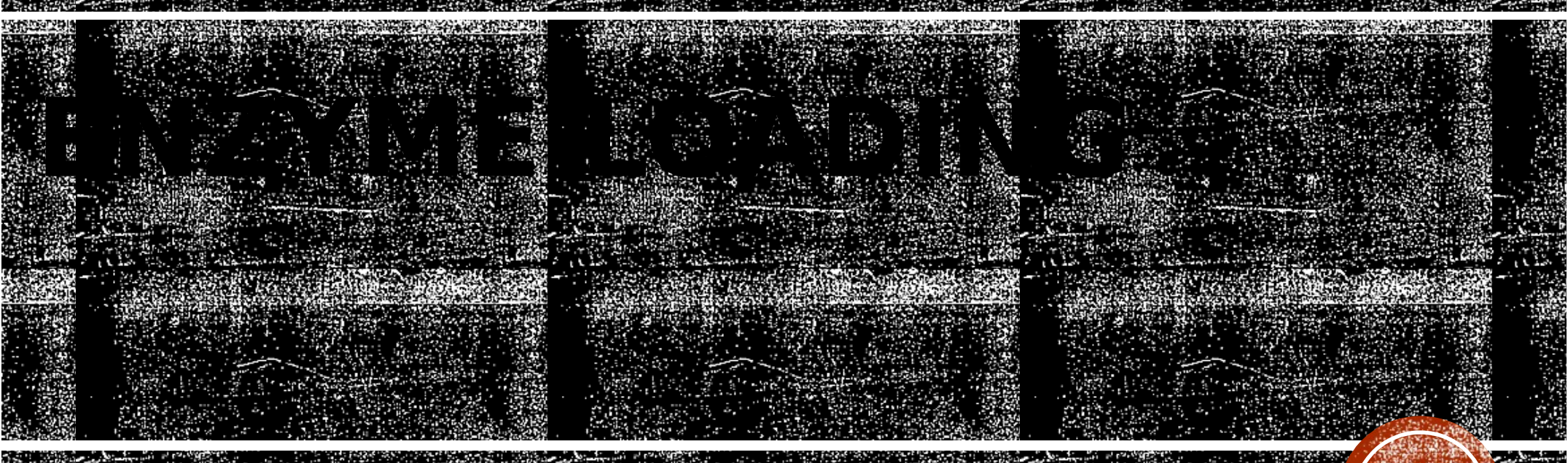
The particle size in the range of 1 to 20mm didn't affect significantly the performance of the pretreatment scheme

Effect of particle size on enzymatic hydrolysis of pretreated straw

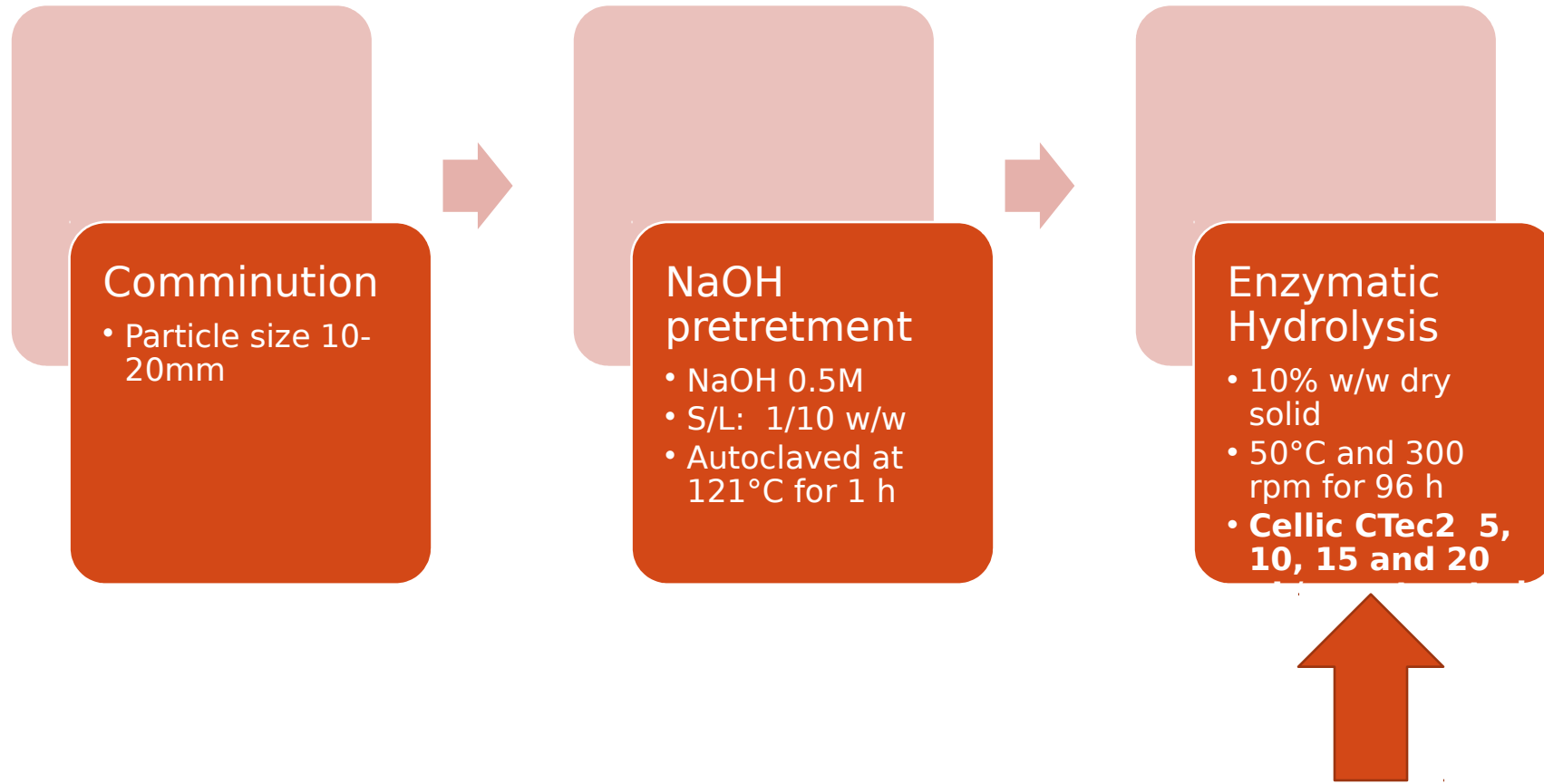


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Enzyme Loading- Experimental procedure



Enzyme Loading

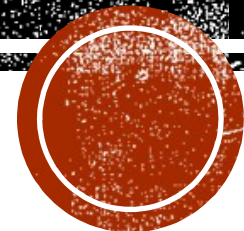
Conclusion

15 $\mu\text{L/g}$ pretreated straw was selected as the optimum cellulase dosage

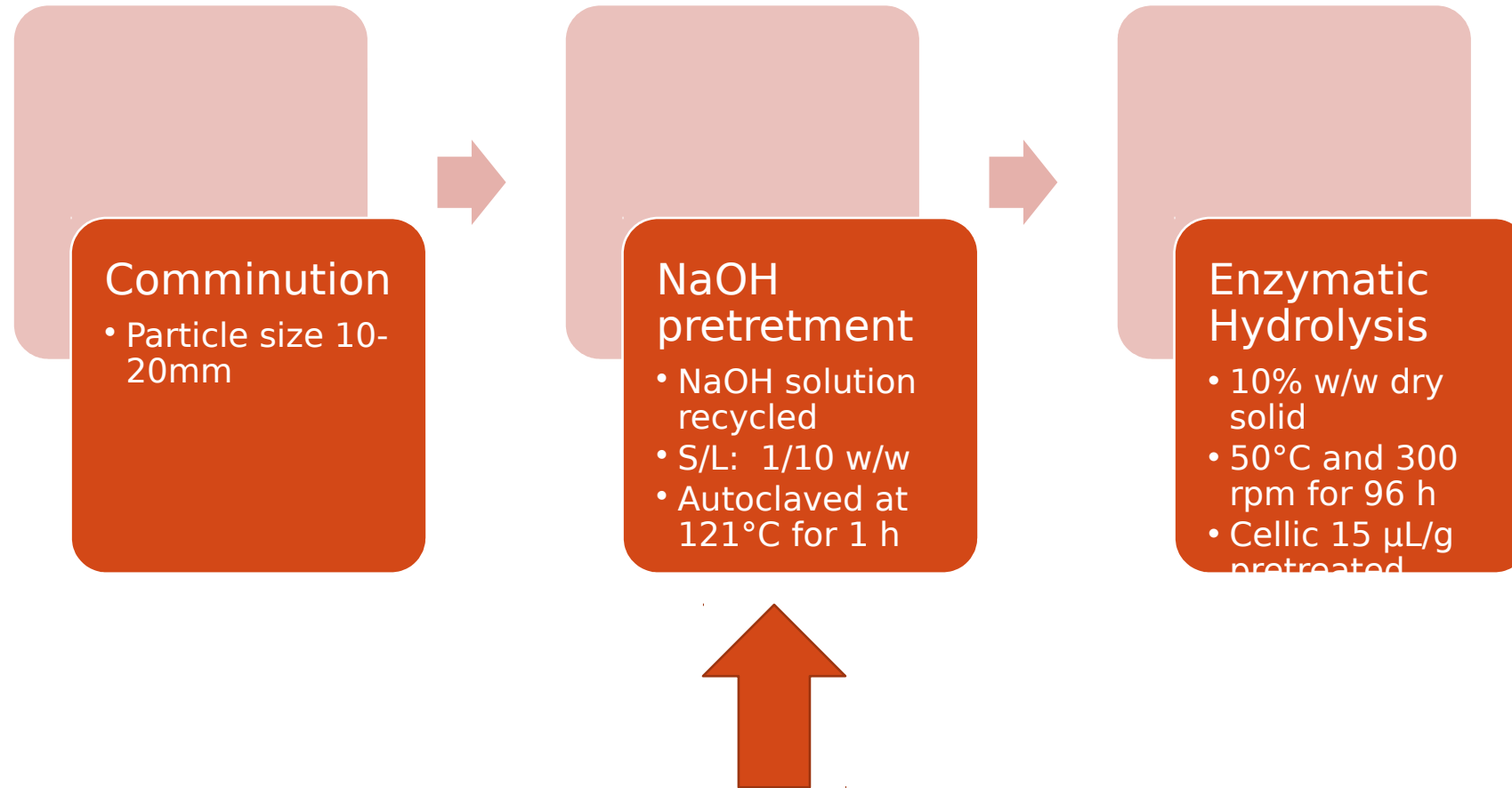
Effect of enzyme loading on the straw solubilization and cellulose degradation during enzymatic hydrolysis



ALKALINE SOLUTION RECYCLING



Alkaline solution Recycling- Experimental procedure



Alkaline solution Recycling

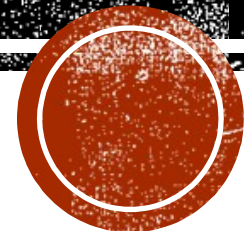
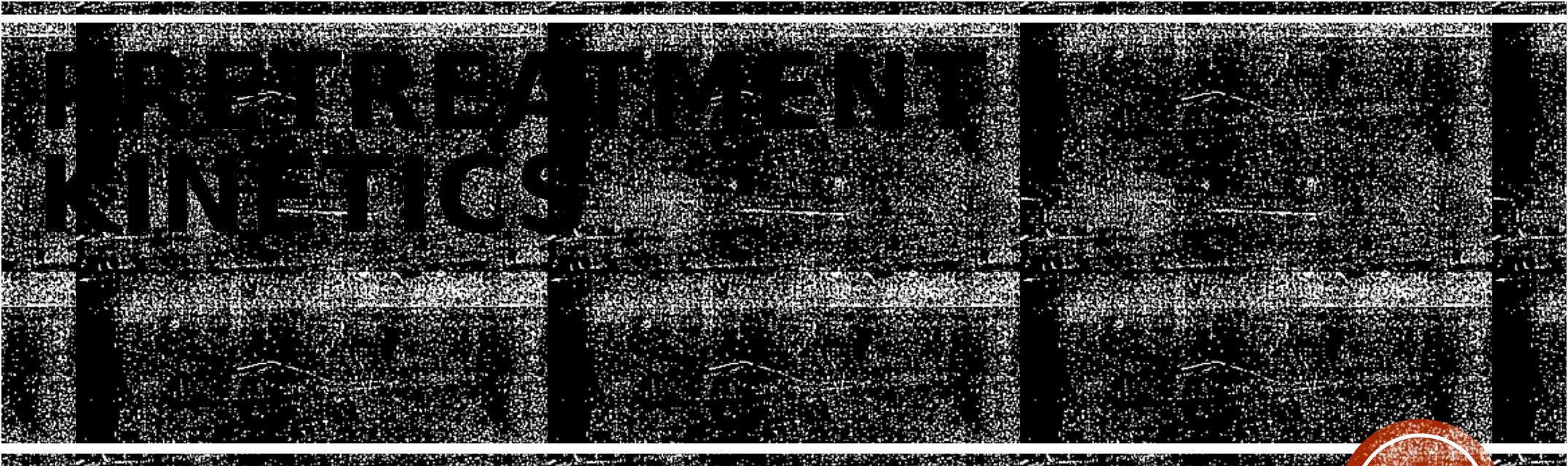
Cycle No	%TS hydrolysis			%cellulose degradation			%AIL degradation			%ASL degradation			%hemicellulose degradation		
1	36.6 1	±	0.1 2	2.74	±	0.26	86.36	±	2.1 6	99.5 4	±	2.84	51.7 1	±	2.59
2	30.1 6	±	0.2 1	4.12	±	1.47	79.51	±	3.5 8	99.4 8	±	2.93	26.3 4	±	2.31
3	26.8 0	±	0.3 2	7.34	±	1.61	72.21	±	5.2 3	99.4 1	±	3.65	15.6 7	±	3.26
4	30.0 8	±	0.7 8	8.50	±	2.44	76.47	±	2.4 5	99.4 1	±	5.62	44.0 2	±	6.19
5	14.0 3	±	0.1 3	5.05	±	2.63	65.96	±	1.3 6	99.3 8	±	3.18	23.6 5	±	4.36

Conclusion

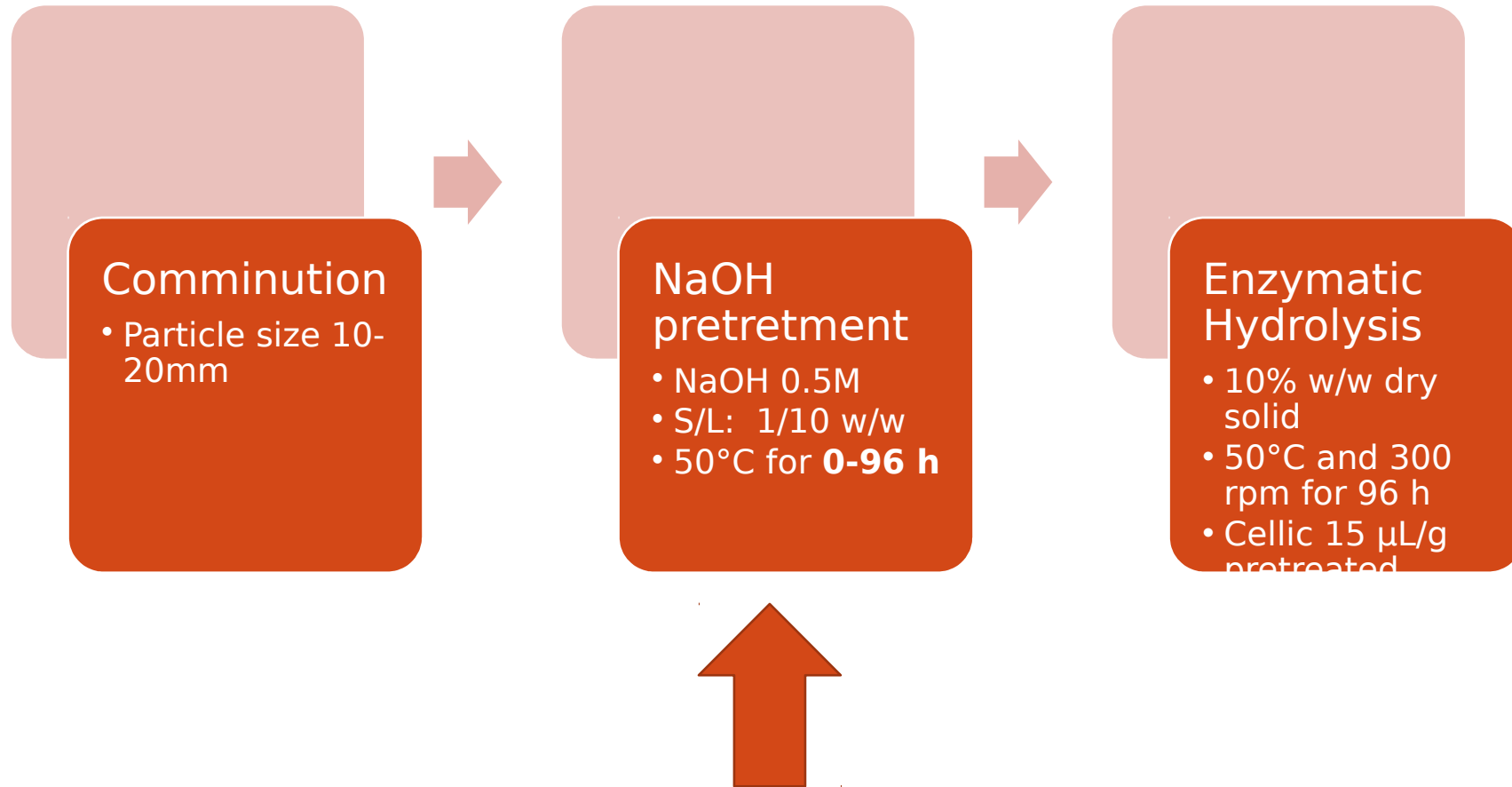
The alkaline solution could be recirculated at least 4 times before being “saturated” although after each experiment it needed to be supplemented with some fresh solution.

Solid fractions' degradation after the different cycles of pretreatment of wheat straw.

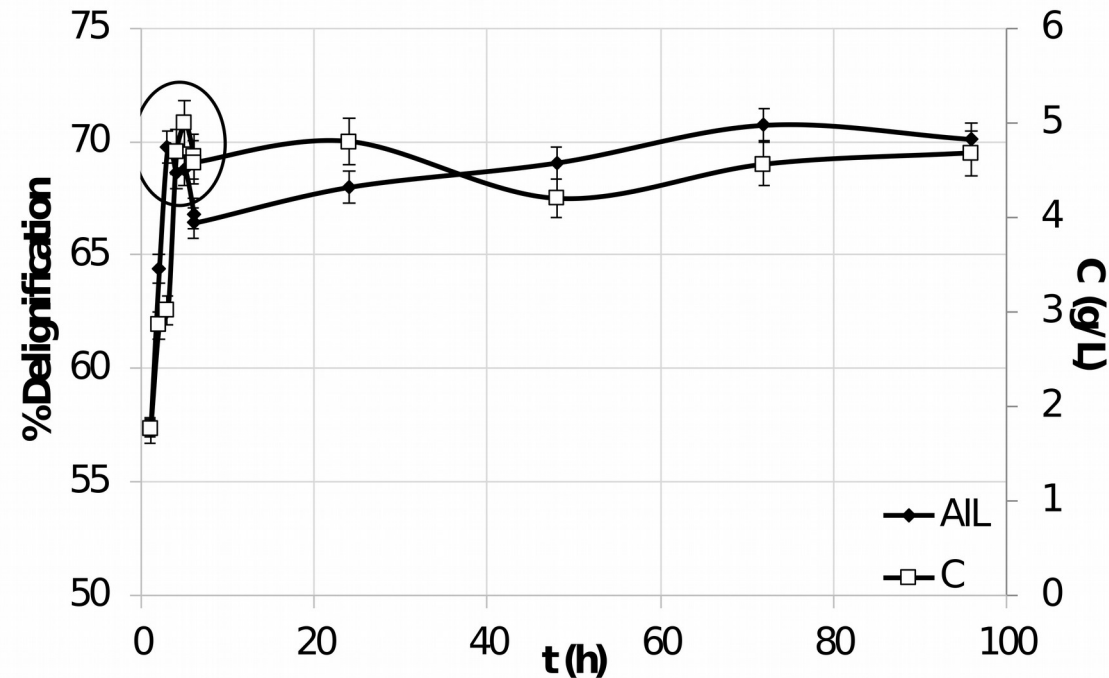




Pretreatment Kinetics - Experimental procedure



Pretreatment Kinetics

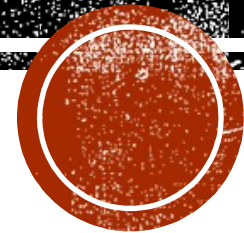
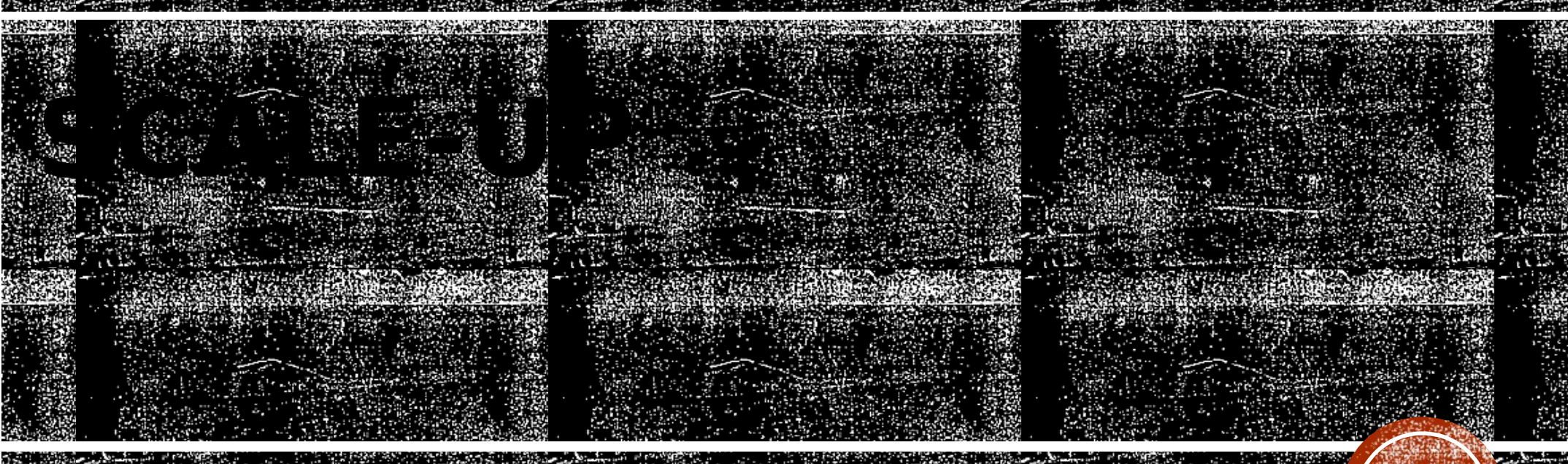


Conclusion

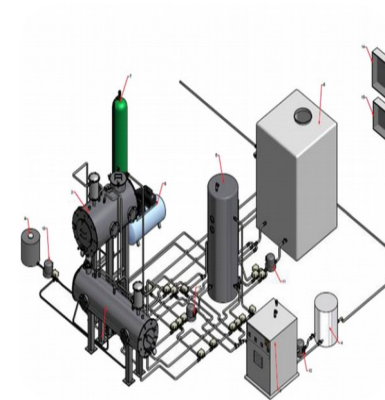
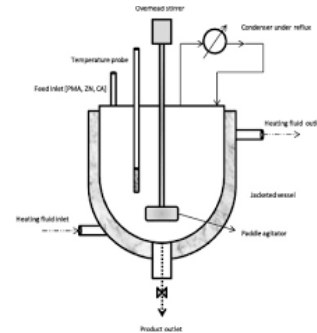
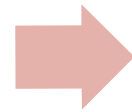
In the time interval of 3-5h of pretreatment, the delignification efficiency reached its maximum and remained statistically constant the rest 90h.

Timeline of total organic carbon (g/L) and delignification efficiency (%) during NaOH 0.5M pretreatment at 50°C





Scaling-up - Experimental procedure



5g/batch
 $V_{\text{reactor}} = 250\text{mL}$

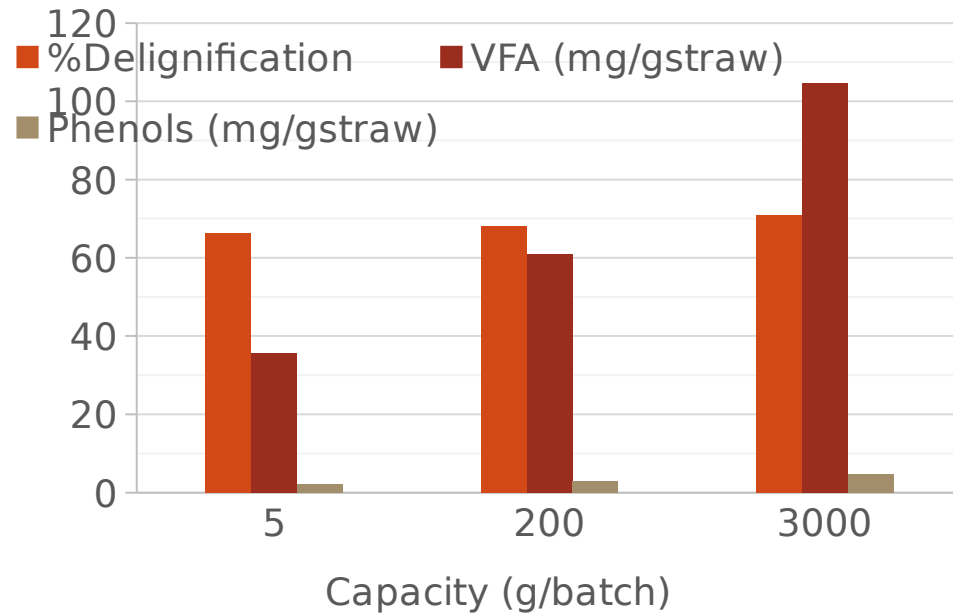
200g/batch
 $V_{\text{reactor}} = 4\text{L}$

3000g/batch
 $V_{\text{reactor}} = 200\text{L}$

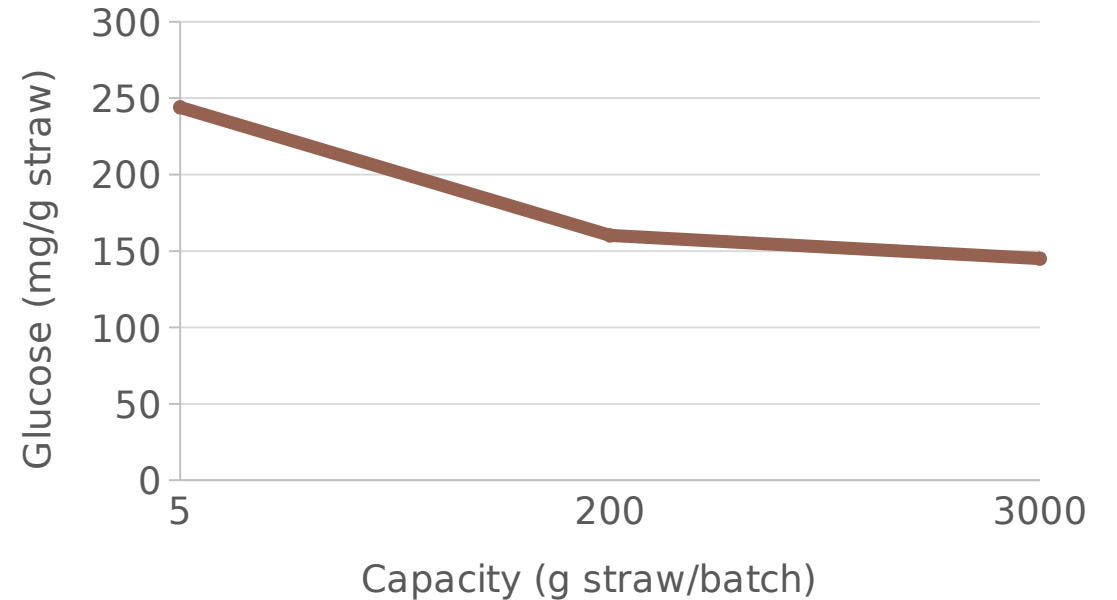


Scaling-up

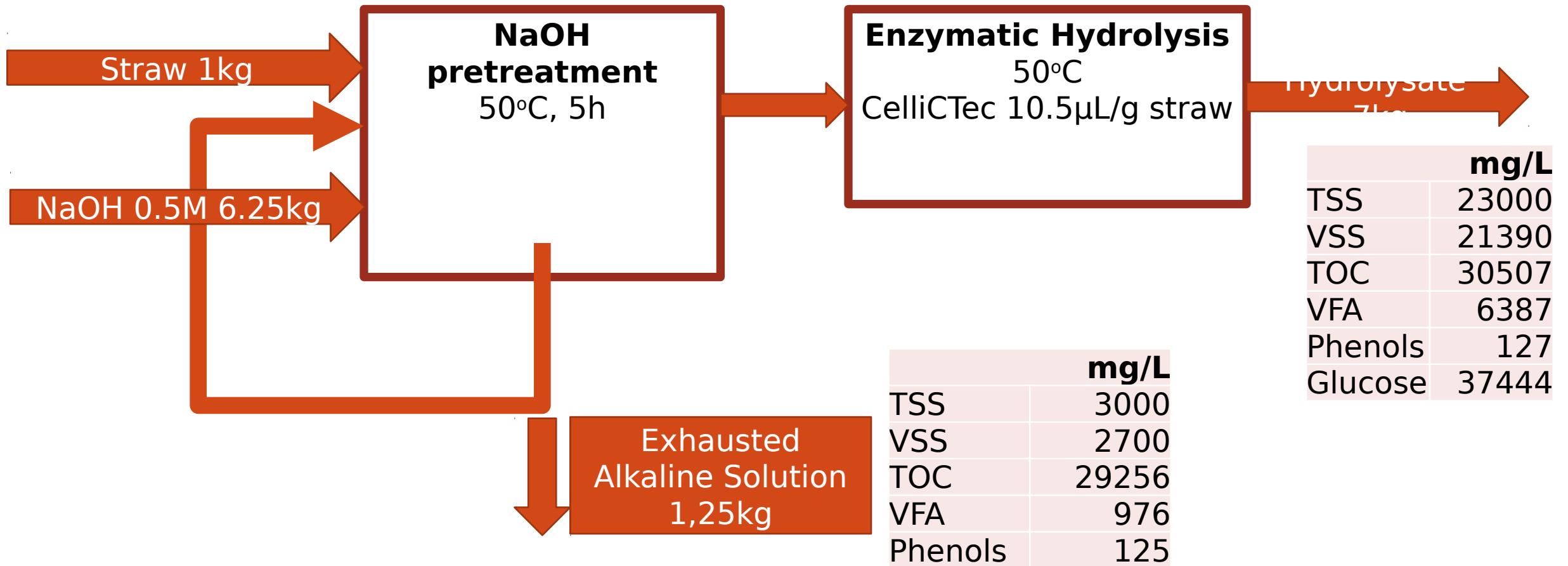
NaOH pretreatment step



Saccharification step



CONCLUSIONS



Acknowledgements

The authors acknowledge funding through European Horizon 2020 NoAW (No Agro Waste, Grant no. 688338) project for supporting this work.

**THANK YOU
FOR YOUR
ATTENTION**

