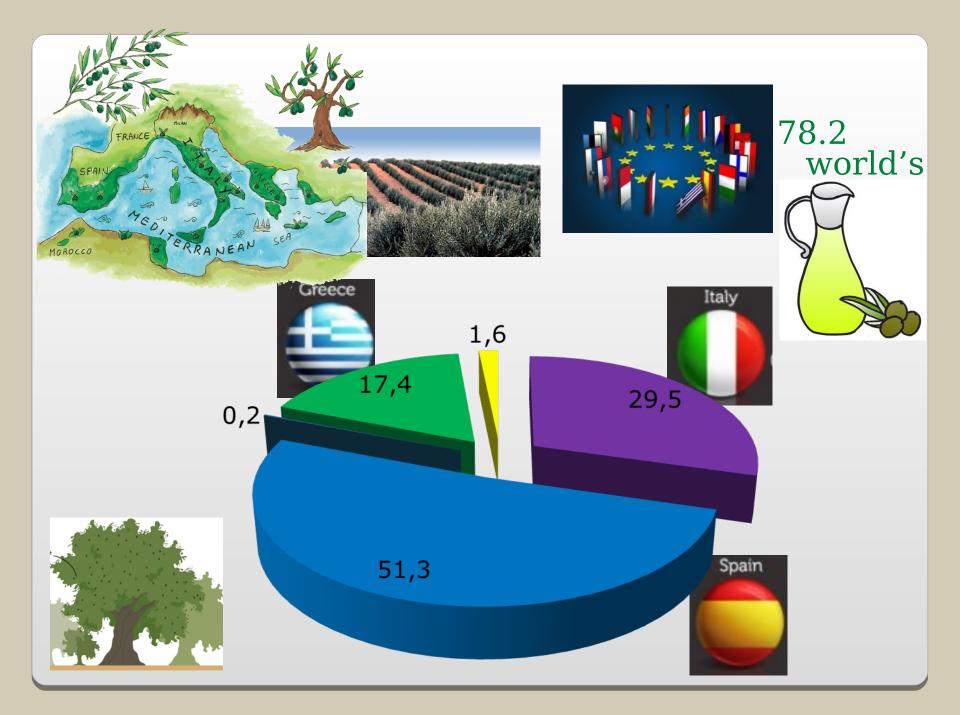
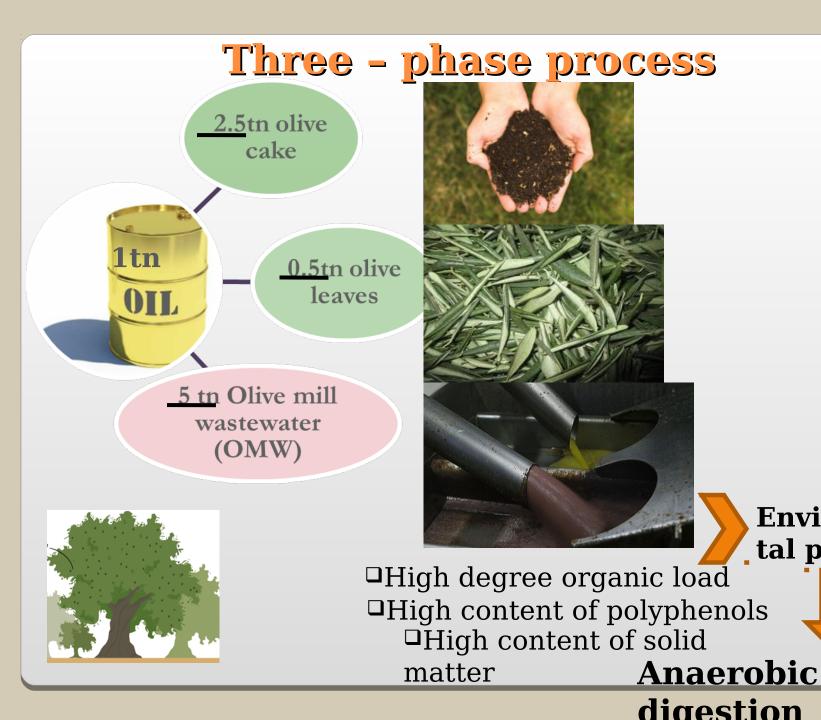
HERAKLION 2019iction in pilot digesters olid Waste Management wastewater ble and agro-industrial by-products D. Thanos, A. Maragkaki, M. Fountoulakis, T.

Manios

Laboratory of Natural Resources, Management & Agricultural Engineering Hellenic Mediterraneon University, Greece







Environmen tal problem

Aim

Examine on a pilot scale, the effect of different waste mixtures available in Crete on methane production for bioenergy generation and to find environmental friendly and economically feasible solutions to re-use and valorize the majority of agricultural waste and by-products in Crete, Greece

Specific aim: Investigate biogas production for raw OMW mixed with varying amounts of Poultry Manure and different liquid feedstocks

The approach and results could facilitate the development of biogas production in other Mediterranean regions with similar sources of

Raw Materials



Afte







Raw Materials

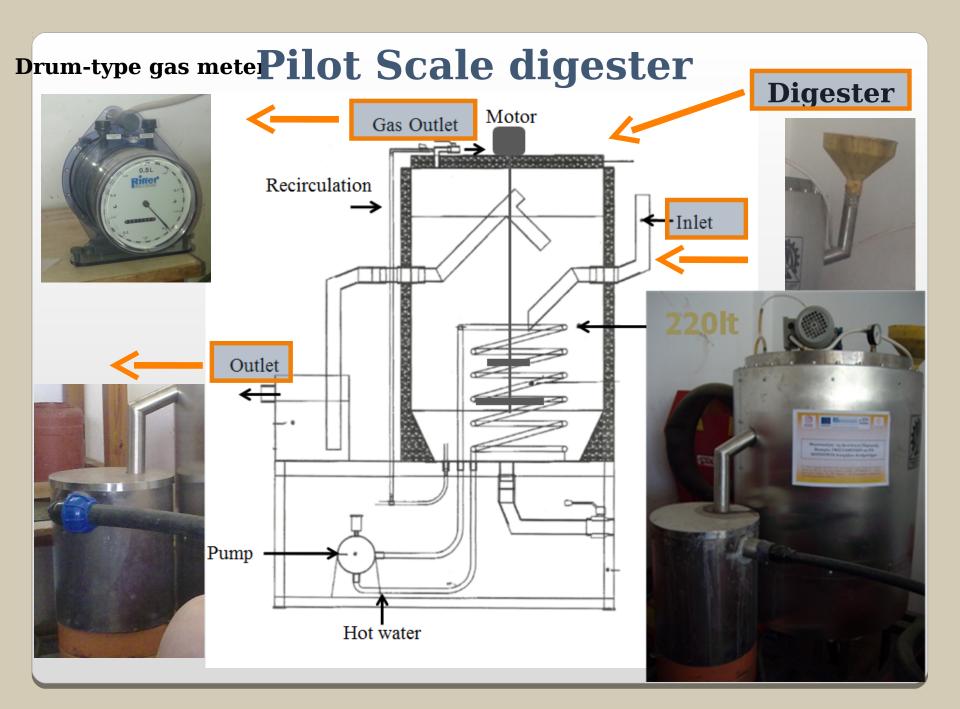
Composition of Liquid Pig Manure (LPM), Olive Mill Waste Water (OMW), Cheese Whey (CW) and Poultry Manure (PM)

Paramet ers	LPM	OMW _A	OMW_B	CW	PM_A	PM_{B}
pH	7.7 ±	$4.9 \pm$	5.7 ±	$4.5 \pm -$	<u>8.9. ±</u>	8.8 ±
	0.1	0.0	1.6	0.1	0.0	0.1
TS (g/l)	$9.5 \pm$	94.9	38.9	73.9	268.2	283.9
	9.6	± 2.5	±	± 1.1	± 3.2	±
			21.4			52.5
VS (g/l)	$5.9 \pm$	83.2	32.6	59.9	180.2	186.9
	6.9	± 2.4	<u>+</u>	± 1.9	± 1.6	±
			17.4			19.8
t-COD	12.9	195.6	71.4	80.7	$7.7 \pm$	7.7 ±
(g/l)	± 9.2	± 15.3	±	± 3.2	3.3	3.3
			$)) \chi$			

Experimental procedure

- ✓ 2 type of feedstock:
- * Sub A: 30 % v/v OMW & 70 % PM & LPM TS ratio ~ 10%
- * Sub B: 40 % v/v OMW & 60 % PM & CW - TS ratio ~ 10% 2
- * Mesophilic AD, 35° C, HRT = 30° day
- ✓ Influent & effluent samples analyzed TS, VS, pH, TCOD, d-COD and methene

Operational parameters - Reactor characteristics							
Reactor no	Digeste r working volume (L)	HRT (days)	Time (days) _e	Feedstock	OLR (kgVSm ⁻ ³ d ⁻¹)		
1 – Sub A	180	30	1 - 66	30 % OMW & 70 % PM & LPM	2.2		
	180	30		40 % OMW	۷.۷		

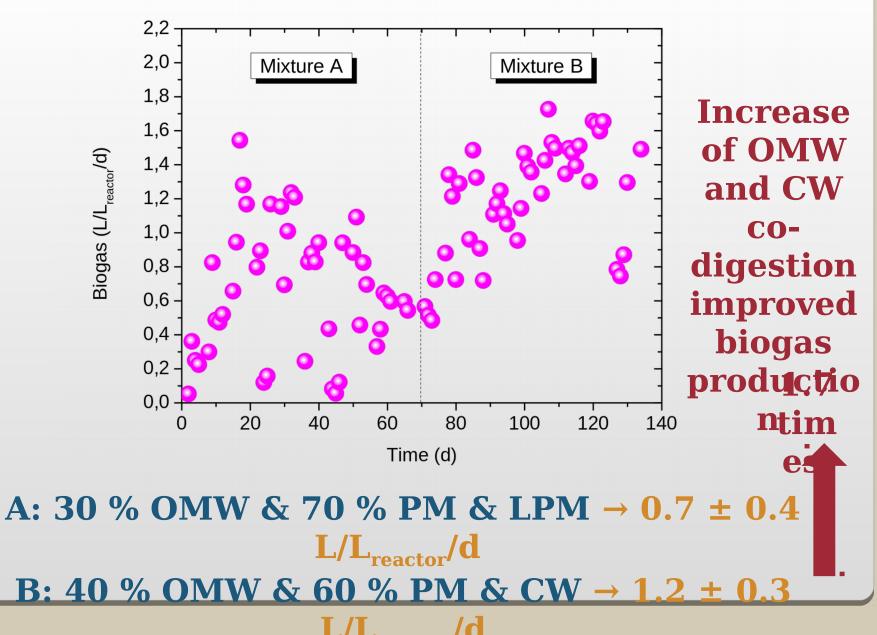


Feedstock Results

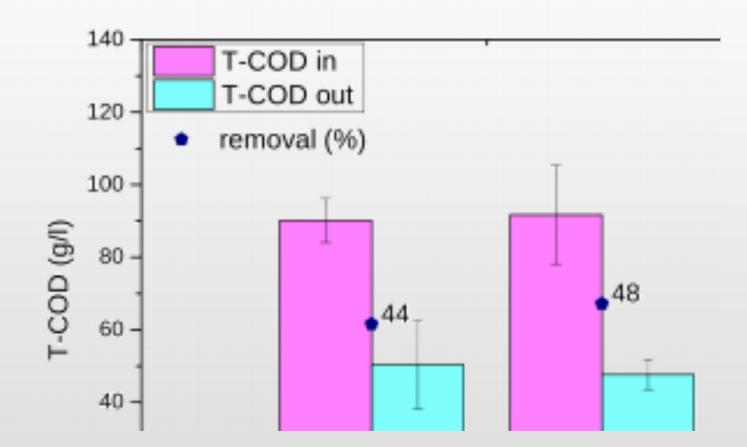
Characteristics of experimental materials as feedstock

Parameters	o-substrate A	Co-substrate B
pH OMW _A was reduced because	6.9 ± 0.1	6.1 ± 0.4 ом
TS (g/l) of OMW 'dilution' with LPM	84.6 ± 9.1	$85.9 \pm 10.9^{W \&}_{PM}$
VS (g/l) OMW	59.8±5.9	62.1 ± 8.4
t-COD (g/l) & PM &	<u>90.1 + 7.5</u>	<u>90.3 ± 13.0</u>
d-COD (g/l) LPM	423 + 27	50.9 + 15.9
N (g/l)	65 + 05	44 + 0.6
P (mg/l)	471 ± 92	437 ± 86
$L_{biogas}/L_{reactor}/day$	0.7 ± 0.4	1.2 ± 0.3
$%CH_4$	60 ± 4.7	61 ± 3.4

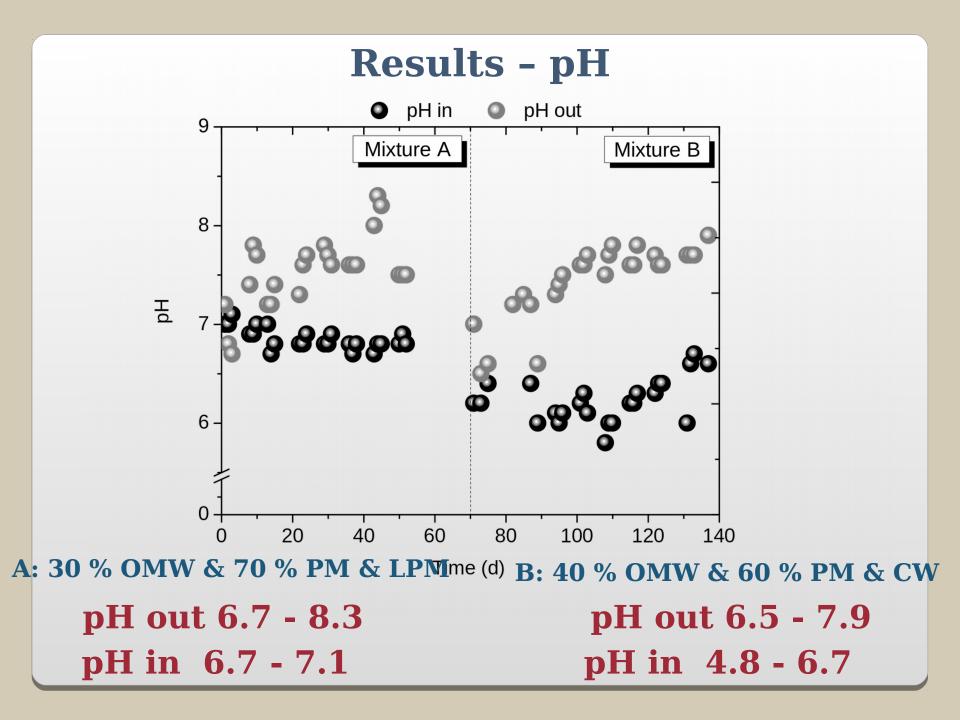
Results

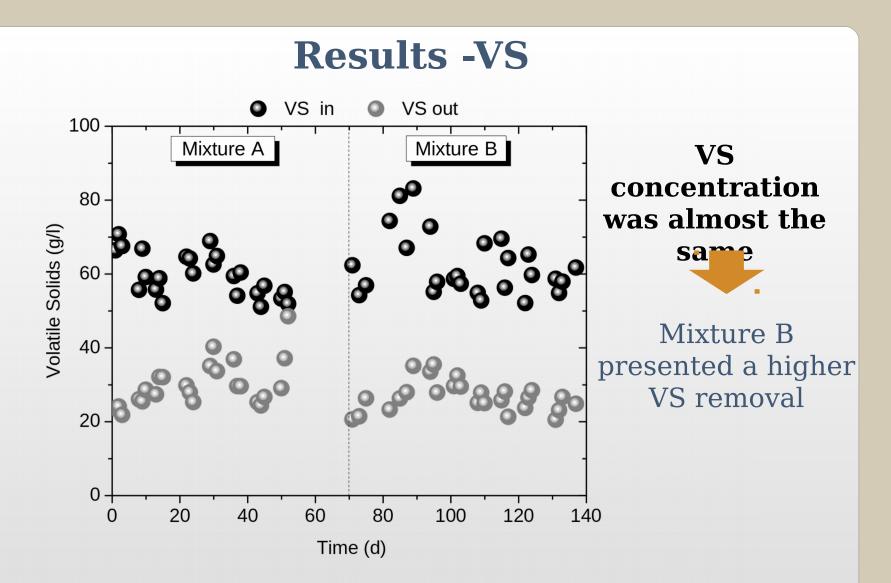


Results - T - COD



A: 30 % OMW & 70 % PM & LPM \rightarrow 44% B: 40 % OMW & 60 % PM & CW \rightarrow 48%





A: 30 % OMW & 70 % PM & LPM \rightarrow 50% B: 40 % OMW & 60 % PM & CW \rightarrow 57%

Conclusions

✓ Co-digestion of OMW, PM and CW is an attractive treatment option for these wastes, because manure improves the buffer capacity of the mixture and a high methane yield can be achieved

✓ Co-digestion of 40 % v/v OMW and 60 % PM and CW increased biogas production from 0.7 ± 0.4 L/L_{reactor}/d to 1.2 ± 0.3 $L/L_{reactor}/d$

 \rightarrow meaning that the increase of OMW and CW co-digestion improved biogas production by 1.7 times

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