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# Volatile Fatty Acids production as PHAs precursors from candy manufacturing wastewater

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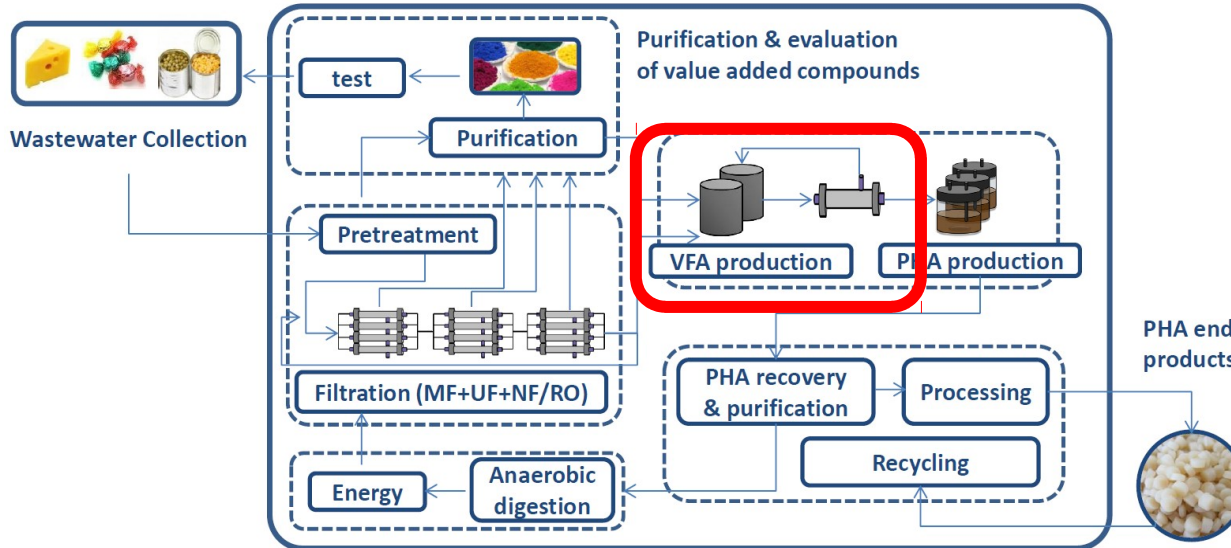
AFTERLIFE has received funding from the Bio-Based Industries Joint Undertaking under the European Union's Horizon 2020 research and innovation program under grant agreement No. 745737 .

# Outline

- Food/Sweet & beverage industries consume around 4.9 m<sup>3</sup>/inhabitant-year of water (Eurostat, average from 2003 to 2011);
- Around 3700 Million m<sup>3</sup>/year of wastewater are generated;
- Typically treated in-situ and/or in a municipal wastewater treatment plant (MWWTP)
  - > Treatment Cost/Disposal: up to 10 €/m<sup>3</sup>
- High concentration of organic compounds (mainly soluble) and very biodegradable, not properly valorized yet;

# Advanced Filtration Technologies for the Recovery and Later conversion of relevant Fractions from wastewater (AFTERLIFE)

AFTERLIFE process



**14 Partners**

-10 SME

-4 Research Organizations

**3 food/sweet industries:**

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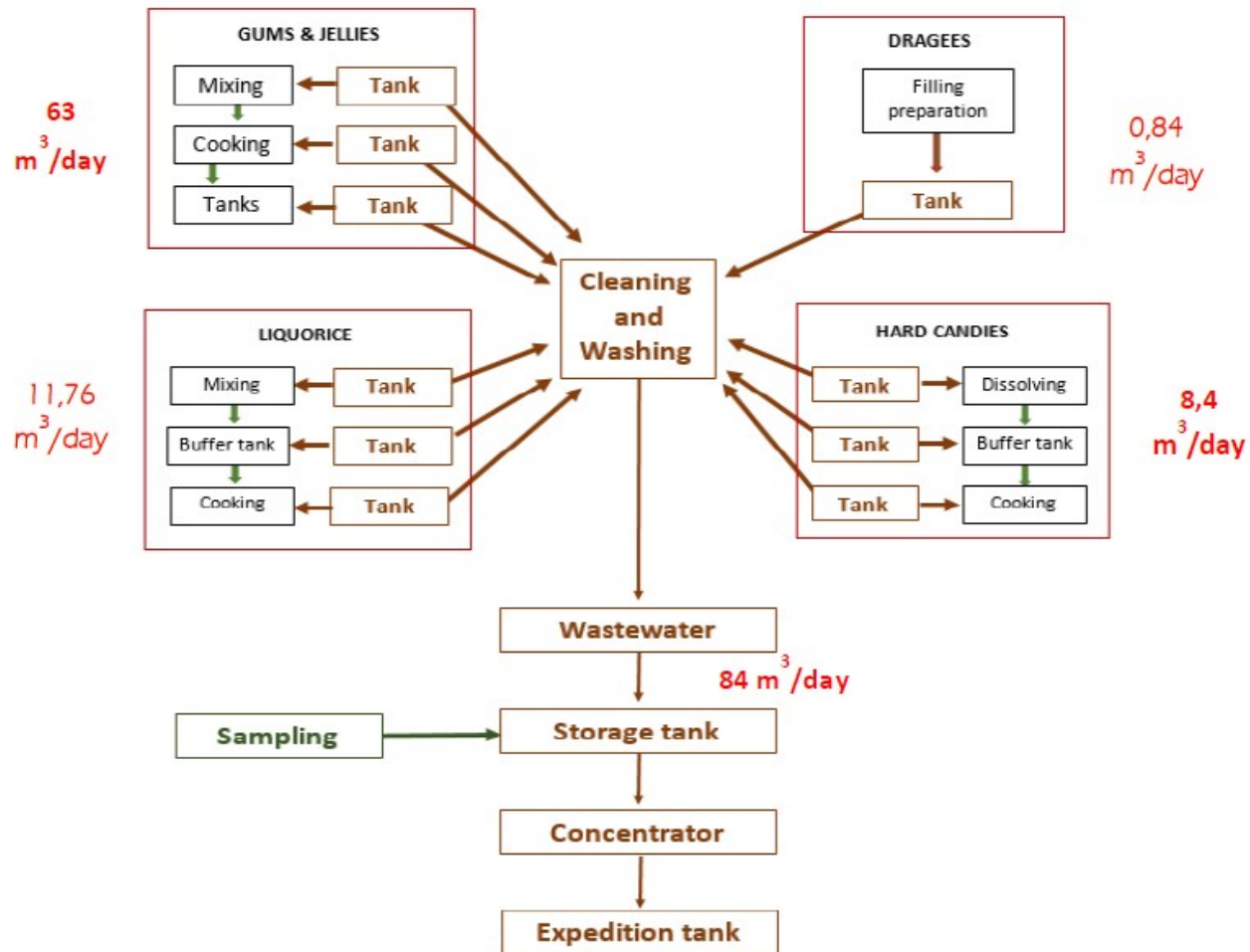
- Candies;
- Cheese;
- Lemon and essential oil

**Total budget around 4 M€**

## Impact for the society

- Recovery and valorization of nutrients and organic matter from wastewater;
- Reduction of CO<sub>2</sub> equivalent per unit of bioplastic produced (< 3 ton/ton);
- Recovery of pure water > 70% of the initial WW volume;
- Increased EU competitiveness: expected PHA final price < 3 €/kg.

# Production of candy manufacturing wastewater



# Objectives

- To study the effect of pH and type of inoculum on the VFAs productivity under batch conditions;
- To assess the best performances in terms of VFAs productivity and yields in a Sequencing Batch Fermentation Reactor;
- To evaluate the final VFAs compositions

# Characteristics of the Candy WW

Parameter	Unit	Average	Min	Max
TS	gTS/kg	82	57	123
TVS	gTS/kg	79	52	120
COD	g/L	81,6	53,5	126
sCOD	g/L	74,3	51,6	104
TKN	mgN/L	582	404	874
PO <sub>4</sub> -P	mgP/L	121	84	182

Relatively high content of Total Solids (>95%TVS), although is «wastewater»;

The COD is mostly in soluble form (around 90%);

High COD/N and COD/P ratio favour the PHA production

# Experimental Setup

Batch tests	Batch Conditions	
pH	5.5; 7.0; 3.5 (not controlled)	
	Buffered	Not buffered
Substrate/ Inoculum ratio	1:1 (COD based)	
Type of inoculum	Activated sludge from municipal WWTP Anaerobic digestate from biogas plant (treating agro-waste materials)	

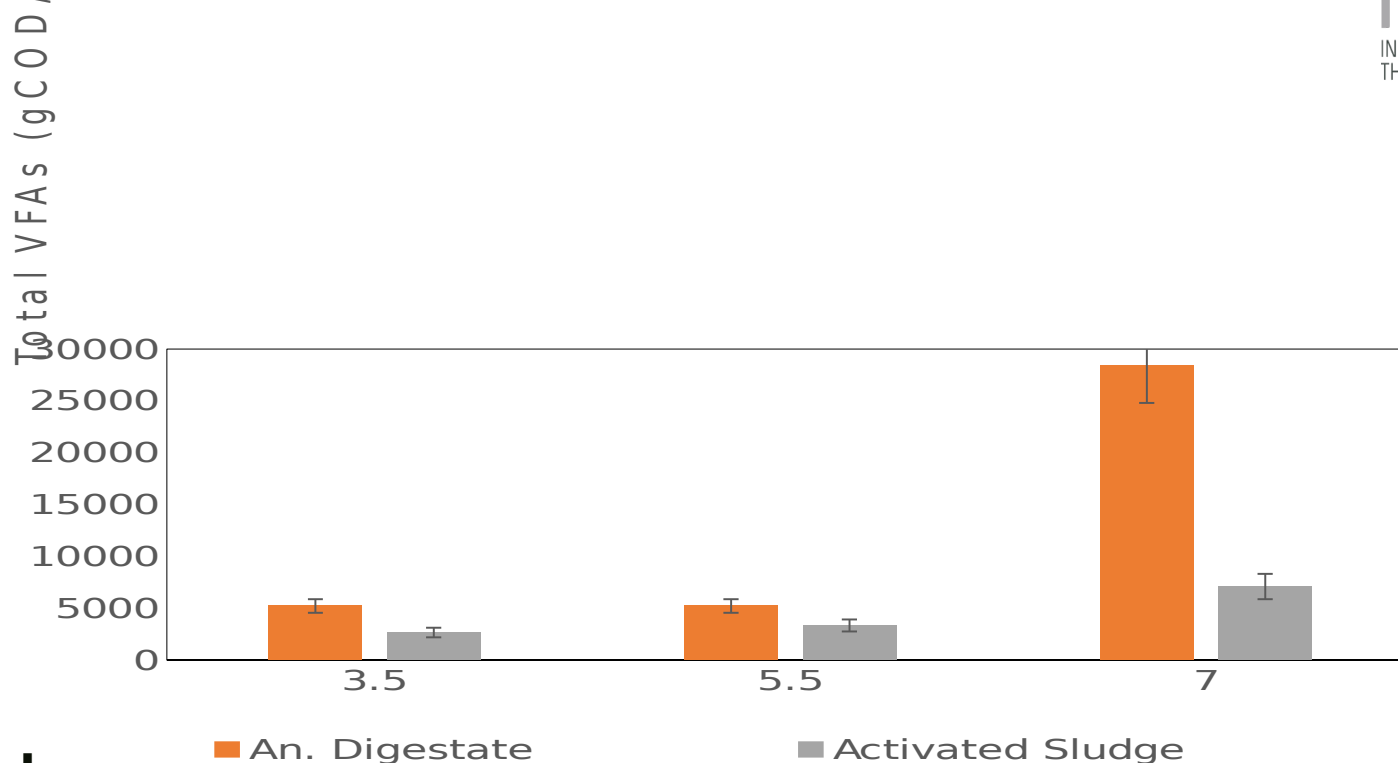
Batch temperature: 37°C

Duration: 7 days

Biogas production was monitored and recorded



# Effect of the type of inoculum and initial pH

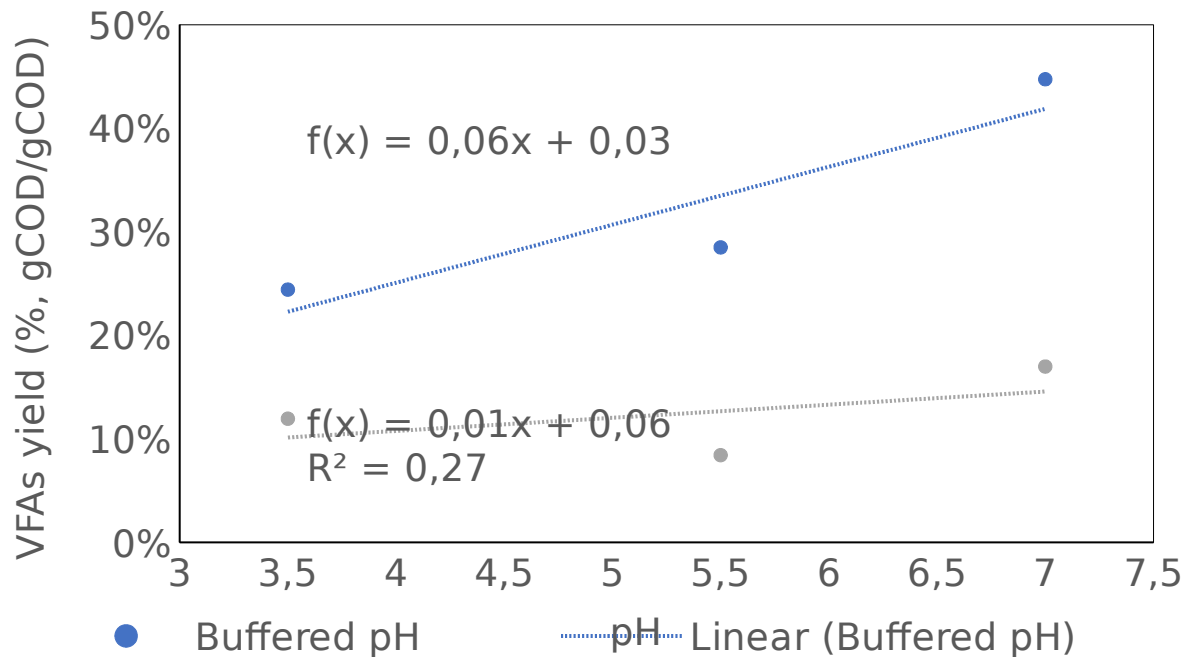


## Take home:

- The pH influence the production of VFAs;
- Type of inoculum play an important role during the start-up of the fermentation reactor;



# Effect of the pH control on VFAs production

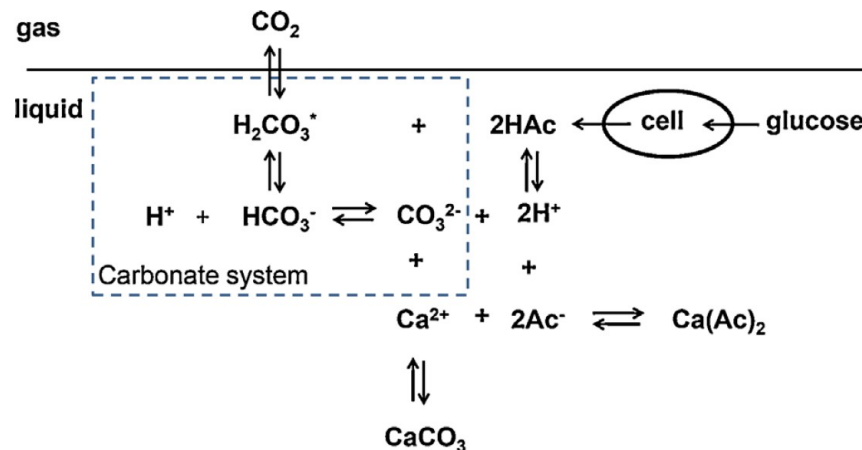


Maximal VFAs concentration were achieved after **4-5 days** of fermentation

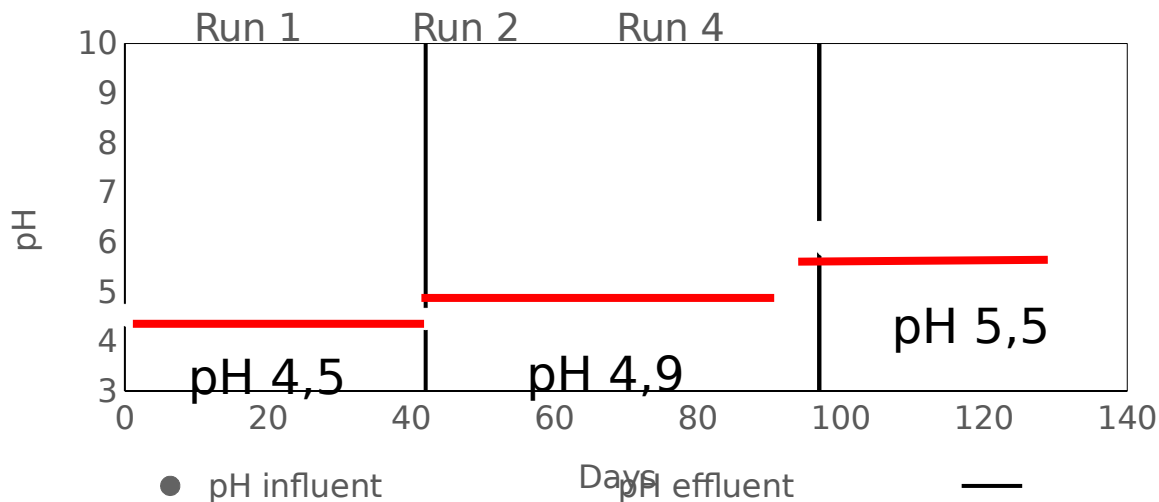
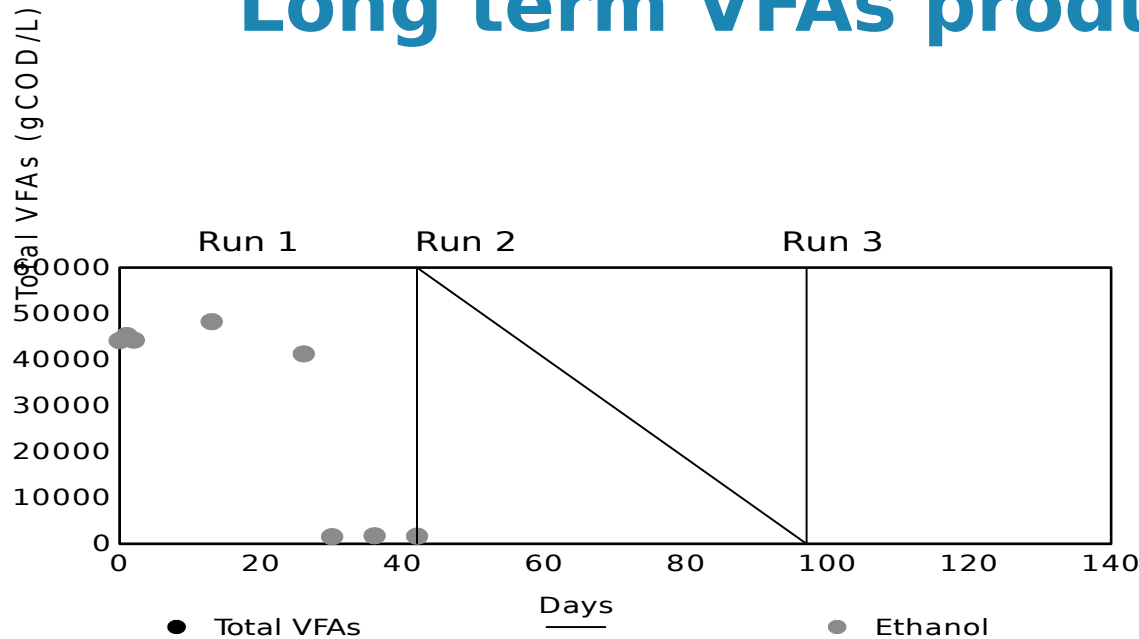
# Operating conditions of the Sequencing Batch Fermentation Reactor

Working volume: 5 liters

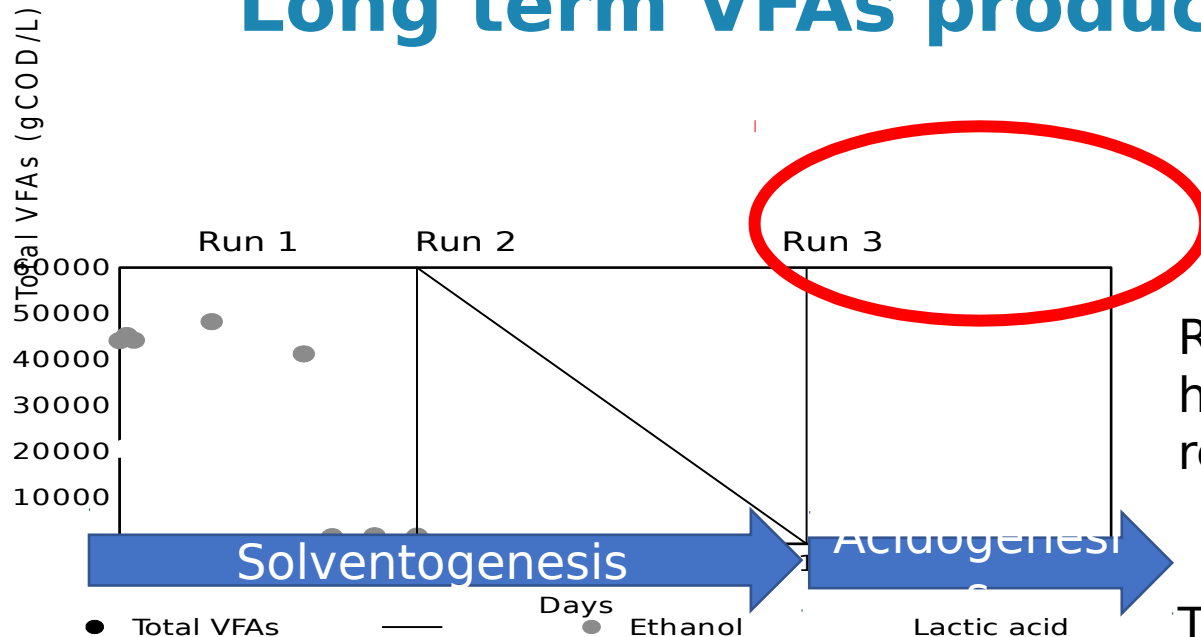
Parameter	Unit	Run 1 (0-42)	Run 2 (43-97)	Run 3 (98-140)
HRT	day	2	2	4
Temperature	°C	37±1	37±1	37±1
vOLR	kgCOD/m <sup>3</sup> day	43±5	38±6	26±2
Alkaline Source	-	-	CaCO <sub>3</sub>	CaCO <sub>3</sub>



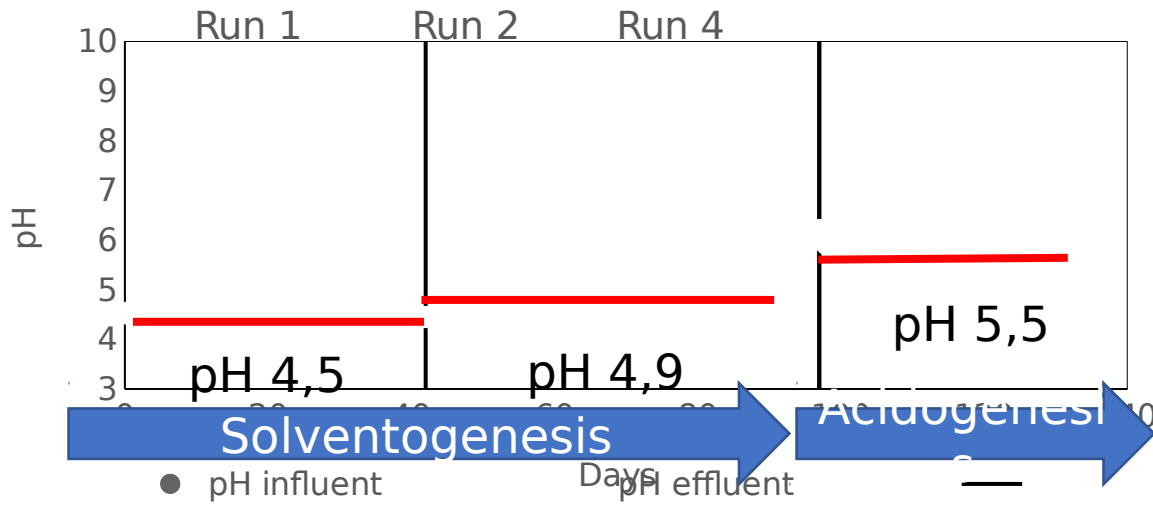
# Long term VFAs production



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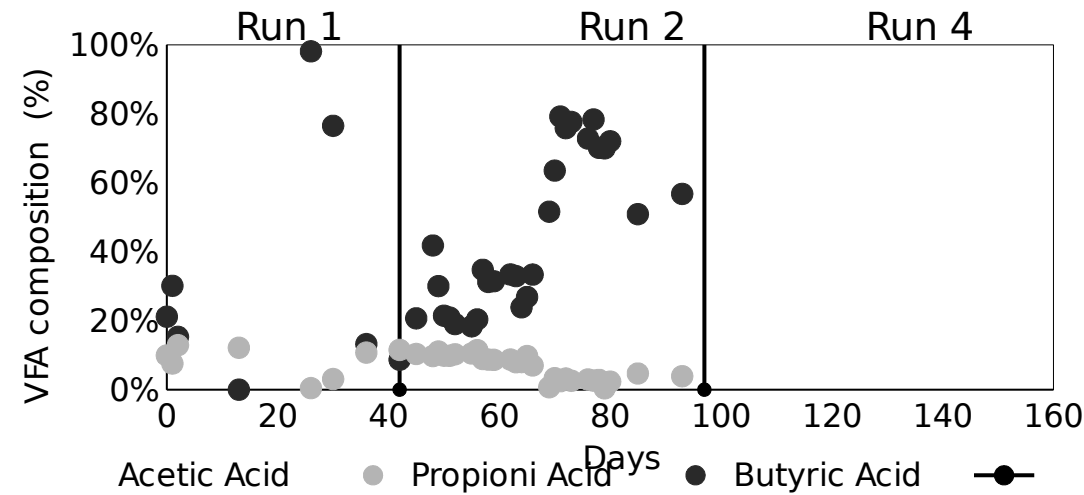
Run 3 (HRT = 4 days), higher alkalinity is retained in the reactor



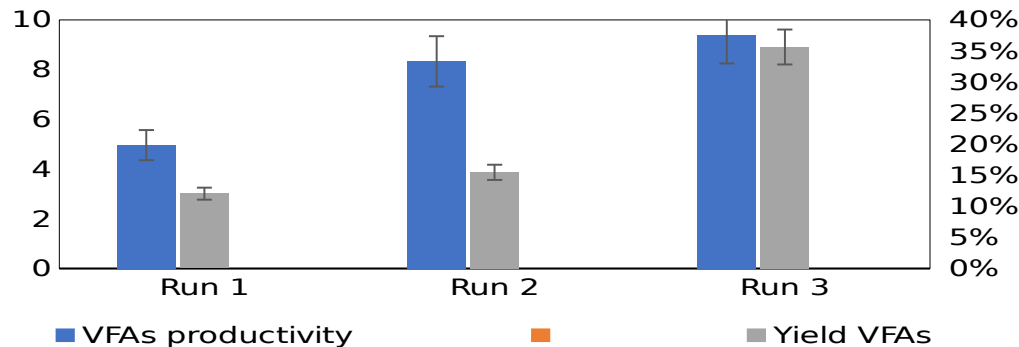
The pH-induced metabolic shift from solventogenesis to acidogenesis

For pH higher than 5,2-5,5, the VFAs concentration increased up to 40-50 gCOD/L

# Long term VFAs production



VFAs productivity  
(kg COD<sub>VFA</sub>/m<sup>3</sup> d.)



- Butyrate was the main type of acid produced (up to 80%)
- In run 4, the observed VFAs productivity was around 10 kgCOD<sub>VFA</sub>/m<sup>3</sup> reactor day;

In run 4, around 36-40% of the COD influent was converted to VFAs

# Conclusions

- The BBI - AFTERLIFE project aims at the valorization of wastewater from food processing through the recovery of added value compounds (e.g., PHAs)
- Wastewater from candy manufacturing represents a relevant source of biodegradable carbon for biorefinery purposes;
- pH was fundamental to shift the metabolism from solventogenesis to acidogenesis
- Around 36-40% of the COD could be converted to VFAs, mainly as butyric acid (80%)
- The VFAs productivity were around 10 kgCOD/m<sup>3</sup> day, operating at HRT of 4 days



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# Thank you for your attention

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