

Utilization of organosolv pretreated lignocellulosic biomass for the production of omega-3 fatty acids by the marine microalgae *Crypthecodinium cohnii* and lactic acid by *Lactobacillus delbrueckii* A. Karnaouri<sup>+</sup>, P. Kostopoulos<sup>+</sup>, A. Chaima<sup>+</sup>, G. Asimakopoulou<sup>1</sup>, D. Perraki<sup>1</sup>, K. Kalogiannis<sup>2</sup>, A. Lappas<sup>2</sup>, E. Topakas <sup>1</sup>

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# Valorization of lignocellulosic biomass on the forefront of sustainability and circular

### economy



- ✓ Greece has a developed *agricultural sector* that supports a big part of the economy.
- ✓ EU mandates about CO₂ emissions and sustainability of all production processes have given a significant boost to the *biorefinery concept*.
- For biorefineries to be economically viable, they need to produce *high added value products* with <u>close to</u> <u>zero wastes</u>, satisfying niche markets such as the food and pharmaceutical ones.



"Novel Conversion Technologies of Waste Biomass to Food additives and Fine Chemicals", funded by Hellenic Foundation for Research & Innovation





## The overall scheme of NoWasteBioTech



## **Biomass pretreatment and efficient fractionation**



# Omega-3 fatty acids as important nutraceuticals

## Functional products and Nutraceuticals:

- Nutraceuticals are standardized grade of food sources derived from food sources, which contain one or more bioactive compounds
- extra benefits in addition to basic nutritional value found in food (prevention or treatment of various diseases).
- addition of small amount of nutraceuticals in foods (1-5%) adds *higher value to the final products*.
- the demand for functional foods and beverages, especially for *omega-3 fatty acid fortified products*, has increased significantly in the past few years, due to the increase in the cost





# Production of $\Omega$ -3 fatty acids from marine microalgae

- Production of Ω-3 polyunsaturated fatty acids (PUFAs), especially those with with long chain (LC-PUFAs)
- microalgae oil is rich in EPA (20:5n-3) and DHA (22:6n-3) [] recognized as bioactive compounds of pivotal importance
- microalgae oil is an attractive alternative to fish oil (its sustainable supply has been challenged due to the reduction of fish resources worldwide
- marine heterotrophic microalgae that belong to Dinoflagellata







## The heterotrophic dinoflagellate Crypthecodenium

- Crypthecodinium cohnii, a flagellated marine microalga, is considered as a prolific DHA producer.
- ✓ The strain ATCC 30772 is able to grow utilizing a variety of different carbon sources, such as short chain fatty acids (acetic, propionic, butyric acid), ethanol, sugars (glucose, galactose, lactose)
- ✓ The accumulation of lipids reaches up to 45-50% of dry cell weight, with DHA to comprise up to 60% of total fatty acids
- ✓ GRN 41; "DHASCO (docosahexaenoic acid-rich single-cell oil) from *Crypthecodinium cohnii* for use in infant formula" (USA, 2001)



Κύτταρα του μικροφύκους C. cohnii x40 (a) και x100 (b)



# Efficient production of omega-3 fatty acids from *C. cohnii*

#### Cultivation strategy

- ✓ Cultivation on shake flasks, 120h
- ✓ Nitrogen source: yeast extract 2 g/lt
- ✓ Sea salts 25 g/lt
- Carbon source: pure sugars, enzymatically hydrolyzed lignocellulosic biomass-derived sugars

(SHF process)

#### Analysis of ω-3 fatty acids

- Harvesting the microalgae cells Freeze drying
- Determination of dry cell weight gravimetrically
- Extraction of fatty acids with modified Folch method (CHCl<sub>3</sub>/MeOH)

2:1(v/v)

Trans-esterification and analysis of FAMEs with GC-MS



# Pure sugars as carbon sources for *C. cohnii*

|           | Biomass         | Biomass (mg/g |       | TFA    |        | DHA    |                         |
|-----------|-----------------|---------------|-------|--------|--------|--------|-------------------------|
| Sugar     | g/lt            | consumed)     | % TFA | (g/lt) | % DHA  | (g/lt) |                         |
| Glucose   | 9.67            | 306           | 43.03 | 4.16   | 29.98  | 1.25   |                         |
| Xylose    | 1.40            | 312           | 37.32 | 0.52   | 5.66   | 0.03   |                         |
| Mannos    |                 |               |       |        |        |        |                         |
| e         | <u>(1.23-</u> ) | 187           | 45.40 | -0.56- | 17.78- | -0.10  | Incubation time (hours) |
| arabinos  | JJ              |               | l     |        |        | j      |                         |
| e         | 1.18            | 126           | 46.57 | 0.55   | 18.55  | 0.10   |                         |
| Glc/ligni |                 |               |       |        |        |        |                         |
| n 50.50   | 10.86           | 354           | 47.90 | 5.20   | 27.14  | 1.41   |                         |
| Glc/HMF   | 7.08            | 320           | 35.24 | 2.50   | 22.95  | 0.57   |                         |
| Glc/Xyl*  | 4.27            | 296           | 40.04 | 1.71   | 31.47  | 0.54   |                         |

Microalgae biomass

*C. connii* prefers glucose as a carbon source over other sugars present in biomass

 $\checkmark$  No catabolic repression by the simultaneous presence of hexose and pentose (gluc

- Presence of lignin can possibly affect positively the microalgae metabolism for enhanced DHA production
- ✓ Presence of furans inhibit cell growth and lipid accumulation





# Enzymatic hydrolysis and Saccharification



- Hydrolysis with Cellic Ctec2<sup>®</sup>, enzyme loading 15mg/g substra
- 50°C, MES bufffer 80mM pH 5.5, 160rpm agitation, 48 hours

|                  |  |           |             |        |               | /~ <u>`</u> |
|------------------|--|-----------|-------------|--------|---------------|-------------|
|                  |  |           | %           |        | %             |             |
|                  |  | %         | hemicellulo | %      | solubilizatio | % cellulose |
| bee              | Pretreatment conditions                                      | cellulose | se          | lignin | n             | conversion  |
| °chv             | H <sub>2</sub> O/THF (50/50%), O <sub>2</sub> 12 bar, 175°C, |           |             |        |               |             |
| <b>VOO</b>       | 120min   | 80.11     | 11.39       | 5.77   | 56.39         | 78.28       |
| <u>م</u><br>nino | H <sub>2</sub> O/ACO (50/50%), O <sub>2</sub> 25 bar, 175°C, |           |             |        |               |             |
| pine             | 120min   | 80.28     | 12.26       | 1.58   | 67.05         | 68.52       |
|                  | H <sub>2</sub> O/ACO (50/50%), O <sub>2</sub> 12 bar, 175°C, |           |             |        |               | *           |
|                  | C O ma i m   |           | 10.21       |        |               | 74.70       |

### **Biomass-derived sugars for the sustainable production** of $\omega$ -3 fatty acids

|            |   | Biomass        | biomass (mg/g |                 |            |           |            |
|------------|---|----------------|---------------|-----------------|------------|-----------|------------|
|            | Pretreatment conditions                                       | g/lt           | consumed)     | % <b>TFA</b>    | TFA (g/lt) | % DHA     | DHA (g/lt) |
|            | H <sub>2</sub> O/THF (50/50%), O <sub>2</sub> 12 bar, 175°C,  |                |               |                 |            |           |            |
| σ          | 120min  | 7.39           | 320           | 44.18           | 3.27       | 23.89     | 0.78       |
| eec –      | H <sub>2</sub> O/ACO (50/50%), O <sub>2</sub> 25 bar, 175°C,  |                |               |                 |            |           |            |
| hw         | 120min  | 7.71           | 312           | 38.22           | 2.95       | 23.15     | 0.68       |
| ood        | H <sub>2</sub> O/ACO (50/50%), O <sub>2</sub> 12 bar, 175°C,  |                |               |                 |            |           |            |
| _<br>pine_ | 60min   | 7.76           | 304           | 33.45           | 2.60       | 27.14     | 0.70       |
|            | Glucose   | 9.67           | 306           | 43.03           | 4.16       | 29.98     | 1.25       |
|            | 60min   | 8.72           | 325           | 39.06           | 3.41       | 26.85     | 0.91       |
|            | H <sub>2</sub> O/THF (50/50%), O <sub>2</sub> 12 bar, 175°C,  |                |               |                 |            | -         |            |
|            | 60min   | 7,98           | 328tty ac     | <b>id5</b> 5.71 |            | -         | 0.75       |
|            | H <sub>2</sub> O/EtOH (50/50%), O <sub>2</sub> 16 bar, 175°C, |                | composit      | ion             |            |           |            |
|            | 60min   | 1esize<br>5.47 | 294 C16       | 38.66           |            | DHA       | .49        |
|            | omega-3 fatty actus   |                | C18:0         |                 |            | <i>th</i> | C EPA Z    |
|            |   |                | C18:1         |                 |            |           |            |
|            |   |                | C22:0 (DH     | IA)             |            |           | <b> </b>   |
|            |   |                |               |                 |            |           | Bio le     |

ste

## Lactic Acid

- a valuable chemical platform that has extensive applications: food, cosmetics, textiles, pharmaceutical, and chemical industries
- The raw substrate materials for LA production constitute 40–70% of the total production cost, which is a challenge for cost- effective LA fermentation
- there has been a growing interest in the use of lignocellulosic was Feedstock from Non-Edible Renewable Resources
  rials are abundant,

rene



Agricultural wastes,

Agricultural wastes, forestry products/wastes, and other lignocellulosic waste materials



gar content without

Through Lactic Acid Bacteria



## Sustainable production of Lactic Acid from biomass





## Lactic acid production by Lactobacillus delbrueckii

- Lactobacillus delbrueckii was able to utilize glucose, mannose and galactose to achieve high production yields of lactic acid
- During bioconversion, LA accumulation acidifies the fermentation broth, causing inhibition to bacteria metabolism and thus limiting the process efficiency and yield; addition of CaCO<sub>3</sub> can *efficiently alleviate the adverse effects of low pH* and boost the production of lactic acid.

|              | <u>mg lactic/ g sugar</u> |  |  |  |  |
|--------------|---------------------------|--|--|--|--|
| <u>sugar</u> | <u>(168h)</u>             |  |  |  |  |
| glucose      | 939 ± 19                  |  |  |  |  |
| mannose      | 855 ± 2                   |  |  |  |  |
| arabinose    | -                         |  |  |  |  |
| galactose    | 903 ± 26                  |  |  |  |  |
| xylose       | -                         |  |  |  |  |

Lactic acid yields produced by utilizing pure sugars (6% w/v) as carbon source

![](_page_13_Picture_6.jpeg)

### Lactic acid production by utilizing lignocellulosic biomass

LA production from *L. delbrueckii* and SSF using organosolv pretreated biomass at 45°C, 9% initial dry matter, with an enzyme loading of 9mg/ g of biomass, after 168h of fermentation. (*ACO: acetone, EtOH: ethanol, THF: tetrahydrofuran*)

|  | <b>Biomass pretreatment</b>  | Cellulose<br>% | Hemicellulose<br>% | Lactic<br>acid (g/lt) | mg lactic<br>acid/g<br>biomass | %<br>theoretical<br>yield |  |
|--|--|----------------|--------------------|-----------------------|--------------------------------|---------------------------|--|
|  | H <sub>2</sub> O/ACO (50/50%), O <sub>2</sub> 8 bar, 160°C, 120min   | 66.77          | 18,36              | 77.11                 | 756                            | 79.60 ± 8.16              |  |
|  | H <sub>2</sub> O/ACO (50/50%), O <sub>2</sub> 16 bar, 160°C, 120min  | 76.63          | 13.32              | 61.07                 | 678                            | 67.67 ± 2.32              |  |
|  | H <sub>2</sub> O/ACO (50/50%), O <sub>2</sub> 8 bar, 175°C, 120min   | 82.3           | 13.9               | 50.5                  | 561                            | 52.36 ± 1.01              |  |
|  | H <sub>2</sub> O/ACO (50/50%), O <sub>2</sub> 16 bar, 175°C, 30min   | 79.74          | 15.69              | 64.56                 | 717                            | 67.43 ± 2.87              |  |
|  | H <sub>2</sub> O/EtOH (50/50%), O <sub>2</sub> 16 bar, 160°C, 120min | 72.96          | 16.03              | 52.5                  | 583                            | 58.72 ± 4.98              |  |
|  | H <sub>2</sub> O/EtOH (50/50%), O <sub>2</sub> 16 bar, 175°C, 60min  | 81.28          | 13.99              | 67.1                  | 745                            | 70.21 ± 0.91              |  |
|  | H <sub>2</sub> O/THF (50/50%), O <sub>2</sub> 16 bar, 150°C, 120min  | 73.09          | 13.3               | 78.93                 | 837                            | 86.97 ± 6.7               |  |
|  | H <sub>2</sub> O/ THF (50/50%), O <sub>2</sub> 16 bar, 160°C, 120min | 79.13          | 12.1               | 85.7                  | 912                            | 89.78 ± 10.1              |  |
|  | H <sub>2</sub> O/THF (50/50%), O <sub>2</sub> 16 bar, 160°C, 60min   | 68.99          | 15.55              | 72.96                 | 785                            | 83.29 ± 1.14              |  |
|  | H <sub>2</sub> O/ THF (50/50%), O <sub>2</sub> 16 bar, 175°C, 60min  | 85.28          | 10.82              | 53.23                 | 591                            | 55.25 ± 0.42              |  |

![](_page_14_Picture_3.jpeg)

## Conclusions – Future work

- Lignocellulosic biomass can be used for the production of value-added products, such as omega-3 fatty acids and lactic acid, through *environmentally friendly bioconversion processes*.
- Wet oxidation in presence of organic solvents is an efficient pretreatment method for the fractionation of lignocellulosic biomass.
- Fermentation of microalgae needs to be optimized to maximize the accumulation of fatty acids and boost the mechanism of DHA synthesis (fermentation strategy, effect of C/N ratio ect.)
- Utilization of pretreatment liquid fraction in order to achieve a zero-waste, holistic approach for the valorization of lignocellulosic biomass waste streams.

![](_page_15_Picture_5.jpeg)

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![](_page_16_Picture_5.jpeg)

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![](_page_16_Picture_7.jpeg)

![](_page_16_Picture_8.jpeg)

Thank you for your attention!

![](_page_16_Picture_10.jpeg)

![](_page_16_Picture_11.jpeg)

![](_page_16_Picture_12.jpeg)

![](_page_16_Picture_13.jpeg)