Biofuels and biomaterials from primary and activated sludge.

L.N.B. Menezes1, João V.S. Manzoni1, Nadia S. Parachin2, P.A.Z. Suarez1

¹Chemistry Institute, University of Brasília, Brasília, Federal District, P.O. Box 4478, Brazil ²Department of Molecular Biology, University of Brasília, Brasília, Federal District, P.O.Box 70.790-900, Brazil.

> Keywords: Sewage sludge, pyrolysis, biofuels, bio-oil, biochar Presenting author email: psuarez@unb.br

ABSTRACT

Sewage sludge has become an environmental challenge because it is produced in a large scale and still has an uncertain final destination. The process of pyrolysis is a sustainable and innovative way of managing this residue mainly because turn a waste into useful bilo-oil and a sterile carbon char. The products formed in the reaction depend on a myriad of factors, such as the diversity of metals present in the *in natura* sludge; the contents of carbon, hydrogen, nitrogen and oxygen; the temperature, heating rate; and the residence time; among other factors. This study proposes the pyrolysis of primary and secondary sludge at 450 °C and the analysis of formed biochars and bio-oils oils. The complex crystallographic profile, absent of potentially toxic metals and the increase of superficial area of biochars grant the use as a biomaterial. The bio-oil analysis shows the displacement of carbonyl groups probably related to the degradation of the fatty acids during the reaction, also seen in NMR spectra, which can lead them to be used as biofuels.

Introduction

The wastewater treatment occurs through physical and biological processes², which will inevitably produce large amounts of sludge. For instance, about 30 million tons of sludge are produced in China every year ⁶, while in Brazil, about 372,000 tons are generated⁷ and leans to increase as much as universalisation of sanitation occurs. The primary sludge arises from the removal of suspended solids, organic matter, oils and greases. The secondary sludge arises from the removal of organic matter and macronutrients such as N and P by microorganisms³. The current final disposal of the sludge is mostly done by landfilling, land spreading, or incineration⁴. Those methods are potentially hazardous to the environment and not economically optimized since the cost of managing the sludge represent up to 50% of the total cost of treatment of the effluent itself⁸.

There are many challenges regarding bringing the traditional sludge management techniques up to date with modern stands of sustainability and effiency. The pyrolysis, a thermochemical treatment carried out in the absence of oxygen at moderate to high temperatures (300-700 °C)¹³, of the sludge is a technological solution to this problem, since it presents the main advantages of the incineration (the destruction of pathogens, the recovering of mineral resources and the reduction in volume¹¹) and has substantial energy and environmental advantages,¹² like the reduction of Greenhouse Gases (GHG) and the recovery of energy. The resulting products achieved in this process are a solid called biochar and a liquid product known as bio-oil¹⁴, which has properties analogous to petroleum diesel. The reaction conditions and the characteristics of the feedstock sludge determine the physicochemical properties of both the formed biochar and the bio-oil, such as composition, particle size, distribution and also regularity of the internal structure of micro, meso and macropores¹⁵.

In this work we have studied the pyrolysis of a primary and a secondary sludge collected from Norte Sewage Treatment Station in Brasilia, Brazil. After the pyrolysis it was obtained a biochar and a bio-oil, which were characterized in order to identify potential uses for them.

Materials and Methods

The primary and secondary sludge were collected from Norte Sewage Treatment Station in Brasilia, Brazil, dried at 105 °C and their total content of fat, oil and grease (FOG) was measured by *n*-hexane extraction with the aid of a Soxhlet apparatus using standard methods¹⁶. The solvent mixture with the lipidic material was then subjected to filtration, evaporation and drying under vacuum. The pyrolysis reaction was carried out with 10 g of dry sample in alumina crucible in a stainless steel horizontal tubular furnace, from room temperature to 450 °C, with a heating rate of 10 °C/min, residence time of 90 min under inert atmosphere- N₂ (g). The bio-oil formed was collected from the outlet of the furnace and was solubilized in dichloromethane, which was later evaporated at 40 °C. The dried sludge feedstock and the biochars were analyzed through Scanning Electron Microscopy with Dispersive Energy Spectroscopy (SEM-EDX) on a Jeol 840a microscope, with a tungsten capillary filament and electric potential difference of 0.2 to 40 kV with a take-off angle of 49.57° and voltage of 15,000kV acceleration. The elementary analysis of Carbon, Hydrogen, Nitrogen (CHNO) were made in Perkin Elmer EA 2400 Series II equipment, with thermal conductivity detector. The X-ray diffraction (XRD) analysis were made on a RIGAKU model ULTIMA-IV, operating with a copper tube and nickel filter, under a voltage of 35 kV and a current of 15 mA, the scan speed was

0.05 °/min and 2 θ angle ranged from 2 to 80°. The Analysis of the pore volume was performed on a Quanta Chrome Nova Win apparatus at -195,85 °C.

The oils extracted and bio-oils ¹H and ¹³C spectra were obtained from 20 mg of sample dissolved in 0.5 mL of deuterated chloroform (CDCl₃) and with TMS (tetramethylsilane) as internal standard, using a Mercury Plus 7.05T spectrometer (300 MHz), with a 5 mm diameter probe. The infrared spectra (FTIR) were acquired on a Shimadzu IR Prestige 21 spectrometer, with an attenuated total reflectance (ATR) cell. The spectra were acquired after the accumulation of 32 interferograms, covering the region between 400 and 4000 cm⁻¹. The acidity essay of the oils were made according to American Society for Testing and Materials¹⁷.

Results and Discussion

The of reaction yield analysis (Figure 1) indicates a bigger volatilization of the organic fraction present in the Primary Sludge (PS). The Elemental analysis of hydrogen, oxygen and carbon of the sludges (Figures 2 and 3) shows there is carbon and nitrogen fixation after the thermal process in the Primary Sludge (PS) and Primary Sludge Biochar (PSB) and losses of hydrogen (probably in the gas fraction). Regarding the Secondary Sludge (SS) and Secondary Sludge biochar (PSB), it was possible to observe a high fixation of oxygen in the produced char. The nitrogen percentage of this sludge feedstock (compared to PS) is much higher due to the presence of nitrogen compounds in the biological flake. The H/C and O/C ratios show low aromaticity and high content of oxygenated functional groups.





Figure 1- Yield of Pyrolysis Reaction of PS and SS

Figure 2- Analysis CHNO of PS (Primary Sludge), PSB (Primary Sluge Biochar), SS (secondary Sludge), SSB (Secondary Sludge Biochar)



Figure 3- Ratio H/C and O/C of PS , PSB , SS and SSB

The analysis of the images generated by the scanning electron microscope (SEM) (Figure 4) indicates both dried *in natura* sludges have a very irregular structure, with asymmetric cavities and a surface full of granules but the SS image also shows the presence of flakes, arising from the activated sludge. After the thermal process, both biochars seems to be have a more simetric structure, with a continuous network, also seen in EDX and XRD analysis.



Figure 4- SEM microscopy a) PS (300X), b) PSB (2000X), c) SS (300X), d) SSB(2000X)

The PS samples have higher crystallinity and a greater number of peaks, as seen in the the X-Ray diffractogram (Figure 5). The intense peak at 26° is related to the crystallographic plane of SiO₂ in the form of quartz (c) the peak near 35° (peak d) is relative to calcite (CaCO₃), at 21° associated to kaolinite- Si₂Al₂O₅ (OH)₄ (peak a), which is clearer after the reaction. In the SS samples the a large band between an intense signal of SiO₂ in the form of quartz in 26° (c signal) and a broad band in 22° (peak b) is relative to cellulose type I, which is decomposed in thermal process. The detailed profile of metals is seen in the analysis of X-ray fluorescence (EDX) data (Table 1) which reveals the absence of potentially toxic metals and a higher percentage of aluminum, iron, silicon and calcium in the SI samples. In contrast, the SS samples present high phosphorus content (removed from the effluent and precipitated in the sludge). BET analysis indicates irregular internal mesoporous and an increase of surface area after heat treatment, mainly on PSB, consistenly to sludge biochars.



Table 1- EDX of PSB and SSB

Element	PSB		SSB	
	Mass	atomic	Mass	atomic
	%	%	%	%
Oxygen	38,17	56,81	33,6	51,18
Magnesium	0	0	3,88	3,89
Aluminum	14,95	13,19	10,51	9,49
Silicon	14,56	12,35	8,67	7,52
Phosphorus	5,03	3,87	17,45	13,73
Potassium	2,69	1,64	8,56	5,33
Calcium	9,93	5,9	7,54	4,58
Iron	14,67	6,25	<mark>9,79</mark>	4,27
Total	100	100	100	100

Commented [c1]: Paulo, eu mantenho as 2 colunas? Percentual em massa ou percentual aotmico?

a)kaolinite, b)cellulose type I, c) quartz and d) calcite. Table 2- Specific Superficial Area and Porus Volume

Sample	Specific Superficial Area (m ² g ⁻¹)				Porus Volume (cm ³ .g ⁻¹)		
	BET ^a	Microporous ^b	External	$V_{0,98}^{c}$	Microporous ^b	Mesoporous	
PS	0	0	0	3,4	0	3,4	
PSB	18,89	9,89	9,00	13,08	6,3	6,78	
SS	0,55	0	0,55	3,08	0	3,08	
SSB	2,59	0	2,59	3,9	0	3,9	

^{a-} BET Method (Brunauer, Emme and Teller). ^b t-plot method, ^cadsorbed volume at p/p₀=0,98

Characterization of liquids

The fatty, oils and grease (FOG) extracted from the primary sludge has a disagreeable smell and dark color, whereas the one from the secondary sludge has a more yellowish tone which shows different levels of oxidation. The FOG from the PS presents acidity of 107.69 mg KOH/g while the one from the PS has 80.57 mgKOH/g. The carboxylic acid and triacylglyceride profile shown by the infrared and nuclear magnetic resonance analyzes are quite similar. In the ¹³C NMR spectrum of both oils (Fig 10 and Fig 11) there is a small band around 180 ppm relative to C=O carbonyl (of carboxylic acid or ester) and a reduced signal at 130 ppm relative to C=C. Relative bands between 16 and 37 ppm relative to sp³ carbon and the multiplet between 22 ppm and 34 ppm refers to sp² carbon. The spectra of ¹H indicate the presence in all samples of peaks related to aliphatic hydrogens (2.48 ppm, singlet, 2.30 ppm, 0.98 ppm), terminal CH₃ hydrogens (triplet at 80 ppm) and CH₂ (intense singlet at 1.3 ppm) but did not present H associated with acid groups and no triacylglyceride related hydrogens (multiplet at 4.5 ppm). ¹H spectra indicate the presence in all samples of peaks related to terminal CH₃ hydrogens (triplet at 0.80 ppm) and CH₂ (intense singlet at 1.3 ppm). The modifications on carbon and hydrogen structure before and after the thermal process are also seen in Table 3 and 4, demonstrating the increase of alkanes and short aliphatic products after the thermal process of PSO while the SSO lead to form long and branched aliphatics and olefins. To better understand the formation of acid groups, the analysis of Infrared Spectra because the influence of the solvent CDCl₃ affect the chemical shift of carbonyl groups on 13C NMR spectra and OH from carboxylic acids on ¹H NMR spectra.









Table 3- Chemical shift on¹³C NMR spectra.

δ (ppm)	Carbon assignments	PSO	SSO	PSB	SSB
0-28	Short aliphatics	7,14%	59,26%	21,43%	21,05%
28-55	long and branched aliphatics	92,86%	22,22%	71,43%	63,16%
55-95	alcohols, ethers, phenolic- methoxys, sugars, carbohydrates	0,00%	3,70%	0,00%	0,00%

95-165	aromatics, olefins	0,00%	7,41%	0,00%	10,53%
165-180	esters, carboxylic acids	0,00%	3,70%	7,14%	5,26%

Table 4- Chemical shift on ¹H NMR spectra

δ (ppm)	Proton Assignment	PSO	SSO	PSB	SSB
0,5-1,5	alkanes	16,67%	45,45%	37,50%	20,00%
1,5-3,0	aliphatics α -to heteroatom or insaturation	41,67%	36,36%	50,00%	40,00%
3,0-4,4	alcohols, methylene-dibenzene	16,67%	9,09%	0,00%	20,00%
4,4-6,0	methoxyl, carbohydrates	8,33%	9,09%	12,50%	20,00%

Infrared spectra of the two oils (Fig 14 and Fig 15) presented a broad band between 2500 and 3500 cm⁻¹ relative to the presence of O-H of acid groups. The infrared spectra of the two oils show the widening of the bands between 2500 and 3500 cm⁻¹ relative to the presence of acid groups. The C = O draw of carboxylic acids appears less displaced than the C = O groups of esters (1710 cm⁻¹ and 1740 cm⁻¹, respectively). In the sample, along the C = O stretch, the C-O-H bond deformation appears around 1800 cm⁻¹. At 1420 cm⁻¹, there is presence of the band referring to the angular deformation O-H and axial stretching O-C-C.



Figure 14- Infrared spectra of Primary Sludge Oil (PSO), Secondary Sludge Oil (SSO), Primary Sludge Bio-oil (PSB) and Secondary Sludge Bio-oil (SSB)

Figure 15- Infrared spectra of Primary Sludge Oil (PSO), Secondary Sludge Oil (SSO), Primary Sludge Bio-oil (PSB) and Secondary Sludge Bio-oil (SSB)

Conclusion

In this study primary and secondary sludge were pyrolyzed at 450 °C and the analysis of formed biochars and biooils oils. The sludge generated in the Primary treatment presents peaks related to a regular and diversified crystalline network, with the presence of silicates. In the SS samples the a large band between an intense signal of SiO₂ in the form of quartz in 26 ° and a broad band in 22°, related to cellulose type I is decomposed in thermal process. Scanning Electron Microscopy (SEM) and BET analysis denote the presence of irregular internal mesopore and an increase of surface area after heat treatment, mainly on PSB, consistenly to sludge biochars. There is also the increase of alkanes and short aliphatic products after the thermal process of PSO while the SSO lead to form long and branched aliphatics and olefins. In summary, the pyrolysis seems to be an excellent alternative for managing sludges. We are currently studying potentials uses for the bio-oil and the biochar obtained in the process.

Acknowledgments

The authors are in debt with CAESB, CNPq, CAPES and FAPDF for financial support of this work.

References:

- Kan, T., Strezov, V. & Evans, T. Effect of the Heating Rate on the Thermochemical Behavior and Biofuel Properties of Sewage Sludge Pyrolysis. *Energy and Fuels* **30**, 1564–1570 (2016).
- Tchobanoglous, G. Wastewater engineering: Treatment and reuse. American Water Works Association. Journal 95, (2003).
- Sheik, A. R., Muller, E. E. L. & Wilmes, P. A hundred years of activated sludge: Time for a rethink. Front. Microbiol. 5, 1–7 (2014).
- Kijo-Kleczkowska, A., Środa, K., Kosowska-Golachowska, M., Musiał, T. & Wolski, K. Mechanisms and kinetics of granulated sewage sludge combustion. *Waste Manag.* 46, 459–471 (2015).
- Zhang, Q. H. *et al.* Current status of urban wastewater treatment plants in China. *Environ. Int.* 92–93, 11–22 (2016).
- Feng, L., Luo, J. & Chen, Y. Dilemma of sewage sludge treatment and disposal in china. *Environ. Sci. Technol.* 49, 4781–4782 (2015).
- Drechsel, P., Qadir, M. & Wichelns, D. Wastewater: Economic asset in an urbanizing world. Wastewater Econ. Asset an Urban. World 1–282 (2015). doi:10.1007/978-94-017-9545-6
- 8. Kacprzak, M. *et al.* Sewage sludge disposal strategies for sustainable development. *Environ. Res.* **156**, 39–46 (2017).
- Batista, L. F. Lodos Gerados Nas Estações De Tratamento De Esgotos No Distrito Federal: Um Estudo De Sua Aptidão Para O Condicionamento, Utilização E Disposição Final. Univ. Brasília. Fac. Tecnol. Dep. Eng. Civ. e Ambient. 197 (2015).
- Luiza, A. :, Salazar, C. & Negreiros, C. DISTÂNCIA E CUSTO DE TRANSPORTE DO LODO DE ESGOTO PRODUZIDO NO DISTRITO FEDERAL CONSIDERANDO DUAS OPÇÕES LOCACIONAIS DE PELETIZAÇÃO.
- Mills, N., Pearce, P., Farrow, J., Thorpe, R. B. & Kirkby, N. F. Environmental & economic life cycle assessment of current & future sewage sludge to energy technologies. *Waste Manag.* (2014). doi:10.1016/j.wasman.2013.08.024
- 12. M.C. Samolada, A. . Z. Comparative assessment of municipal sewage sludge incineration, gasification and pyrolysis for a sustainable sludge-to-energy management. *Waste Manag.* **34**, 411–420 (2014).
- Syed-Hassan, S. S. A., Wang, Y., Hu, S., Su, S. & Xiang, J. Thermochemical processing of sewage sludge to energy and fuel: Fundamentals, challenges and considerations. *Renew. Sustain. Energy Rev.* 80, 888–913 (2017).
- 14. Fonts, I. *et al.* Assessment of the Production of Value-Added Chemical Compounds from Sewage Sludge Pyrolysis Liquids. *Energy Technol.* **5**, 151–171 (2017).
- Kołodyńska, D. *et al.* Kinetic and adsorptive characterization of biochar in metal ions removal. *Chem. Eng. J.* 197, 295–305 (2012).
- AOCS Official Method Aa 4-38. Available at: https://aocs.personifycloud.com/PersonifyEBusiness/Default.aspx?TabID=251&productId=111412. (Accessed: 20th January 2019)
- 17. ASTM D664 18e2 Standard Test Method for Acid Number of Petroleum Products by Potentiometric Titration.