



Institut de Science
des Matériaux de Mulhouse



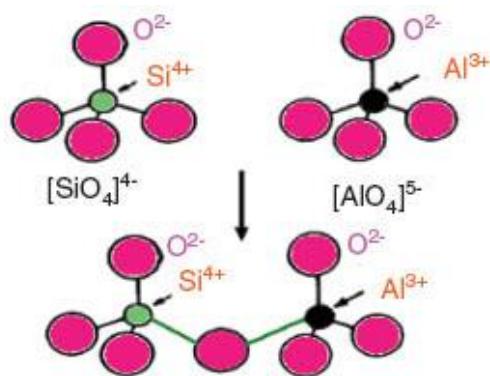
Valorization of agricultural by-products with zeolites

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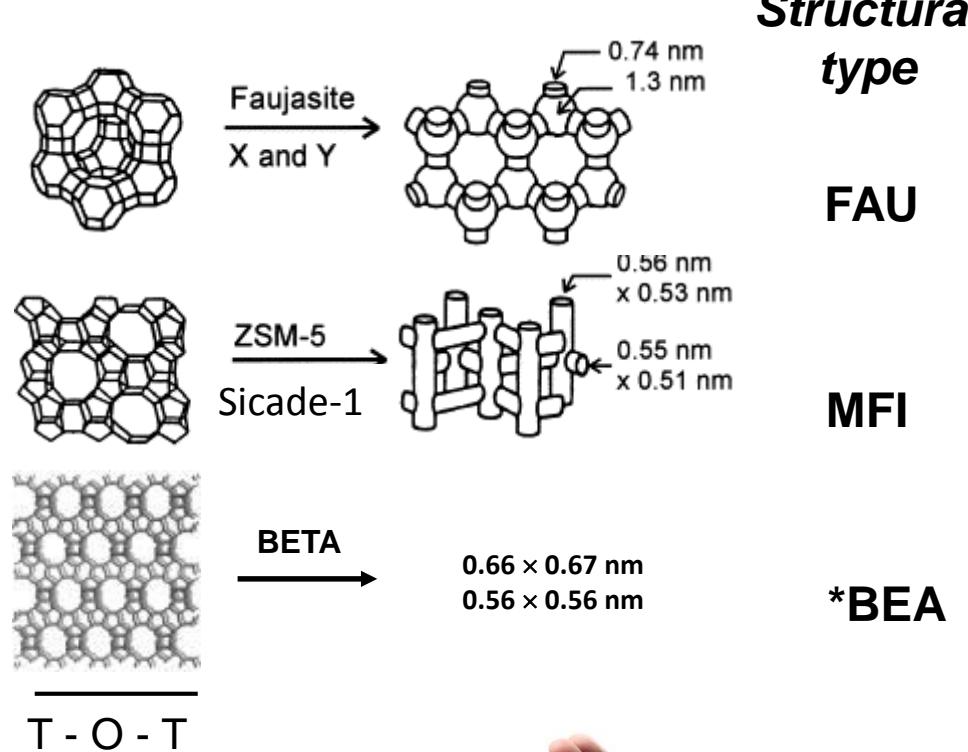


Zeolites

(alumino)silicates



T = Si, Al



Properties :

- Adsorption (molecular sieves, size and shape selectivities)
- Intrinsic acidity (Brönsted, Lewis)
- Ions exchange



Valorization of agricultural by-products with zeolite

Raw material as T source
(Ex. : rice husk/straw for Si)



Zeolite synthesis

Precursor of molecules
(Ex. : pyrolysis of red pepper stems to obtain aliphatic and aromatic hydrocarbons)



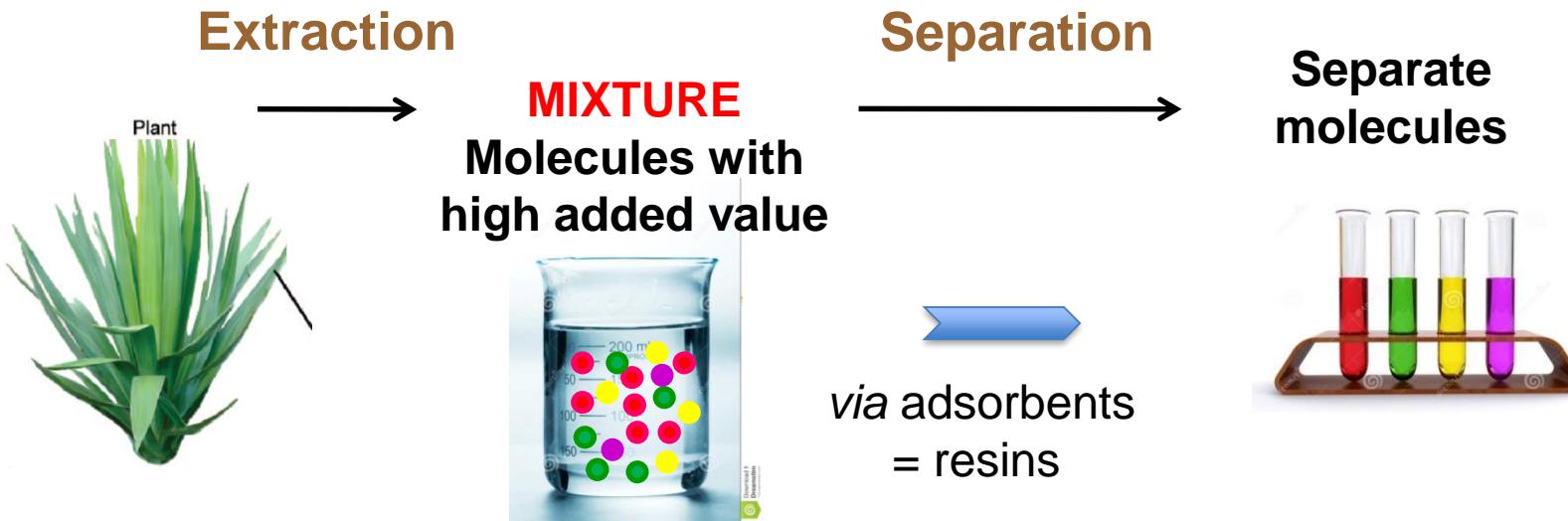
Zeolite = acid catalyst

Biomass as **sources of molecules with high added value**

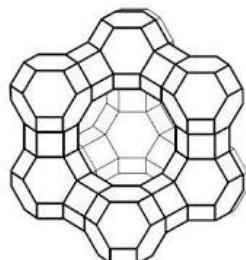


Zeolite = adsorbent

Recovery of molecules with high added value from vegetables



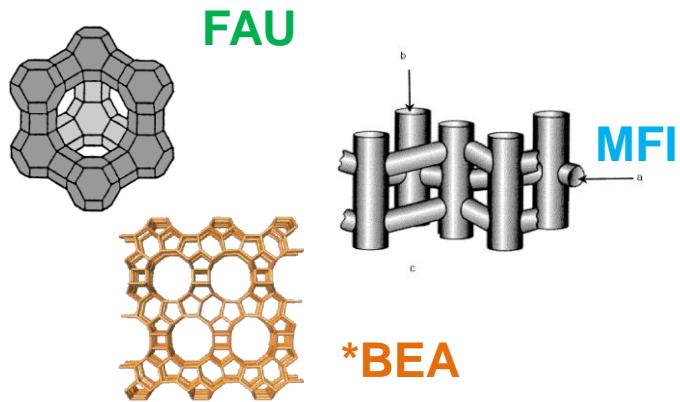
→ Problem: lack of adsorbents with high adsorption and desorption performance
→ Our work : **zeolites as adsorbents**



- Micropores (channels, cavities) with molecular dimensions, calibrated porosity ($\phi < 2 \text{ nm}$)
- High surface area
- High thermal stability
- Ease of regeneration

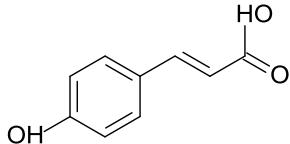
Materials and methods

Zeolites

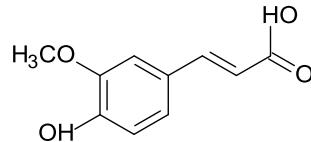


Adsorbent	Molar ratio Si/Al	BET surface (m^2/g)	Pore size (nm)
USY30	14.5	749	0.74
Sicade-1	∞	400	0.51×0.55 0.53×0.56
BETA	88	659	0.66×0.67 0.56×0.56
XAD16	-	≥ 800	n.d.

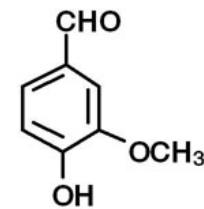
Molecules with high added value



p-coumaric acid 1.0×0.5 nm



ferulic acid 1.0×0.5 nm



vanillin 0.71×0.69 nm

Adsorption

Aqueous synthetic solutions at $21-24^\circ\text{C} \pm 2$.

10-200 mg adsorbent (dried at 140°C , 6h) + 10 mL solution ($C_i = 10$ to 500 mg.L^{-1})

Kinetic adsorption curves

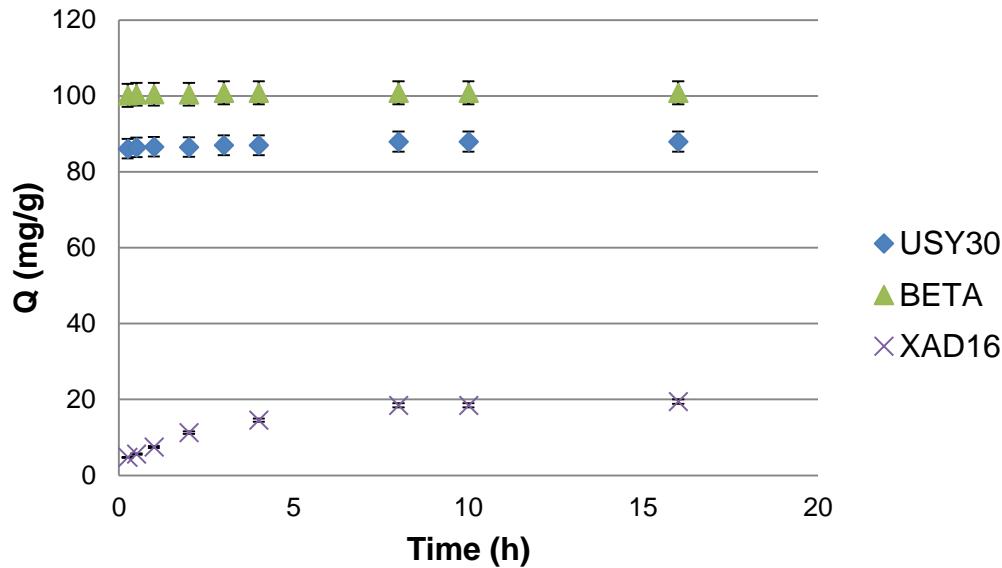
Ex :

Ferulic acid

$C_i = 200 \text{ mg.L}^{-1}$

$m = 50 \text{ mg}$

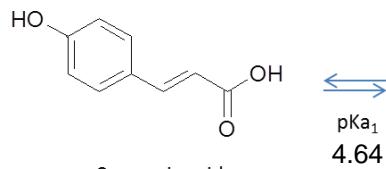
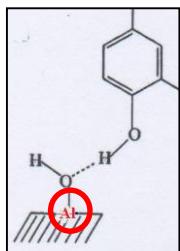
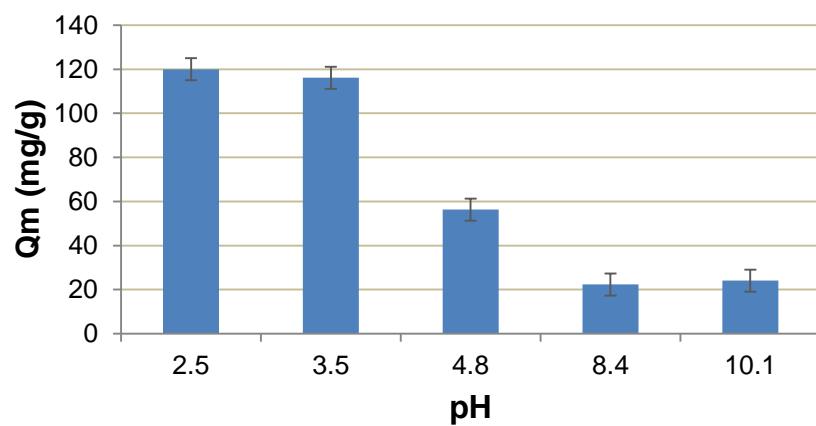
pH = 3.5



Contact time : zeolite → 2h, XAD16 → 10h

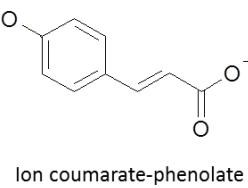
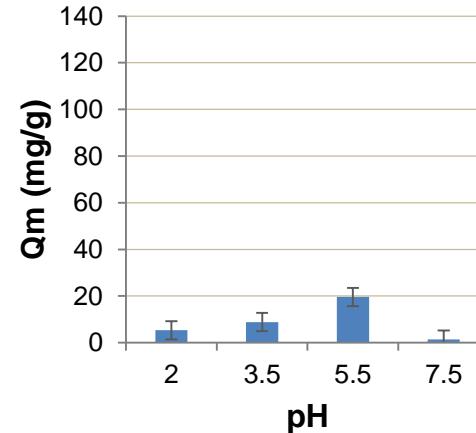
Influence of pH value

p-coumaric acid - BETA (zeolite Si/Al)



→ pH = 3.5

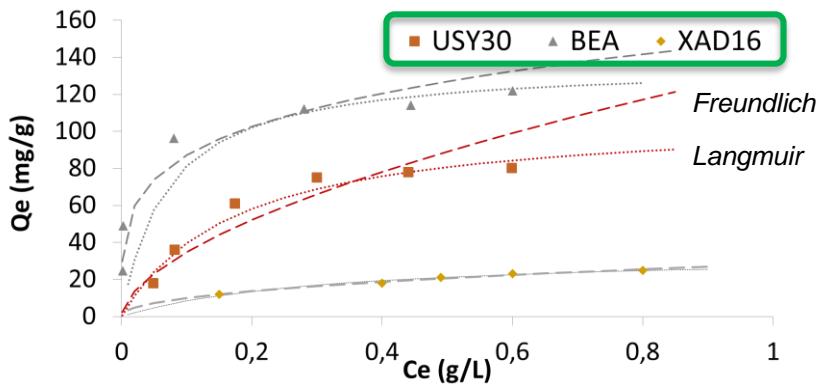
ferulic acid - Sicade-1 (Si)



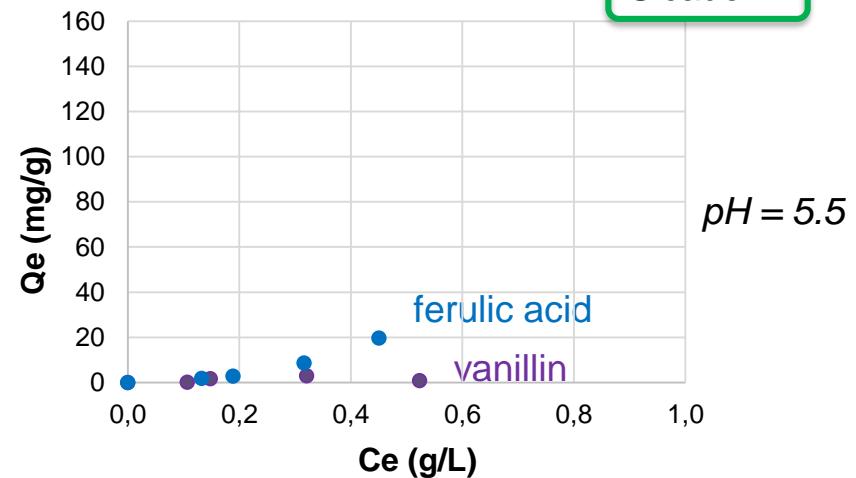
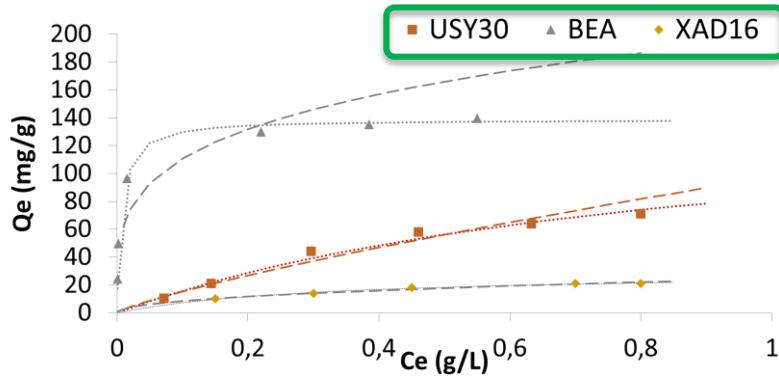
→ pH = 5.5

Isotherms

p-coumaric acid $pH = 3.5$



ferulic acid $pH = 3.5$



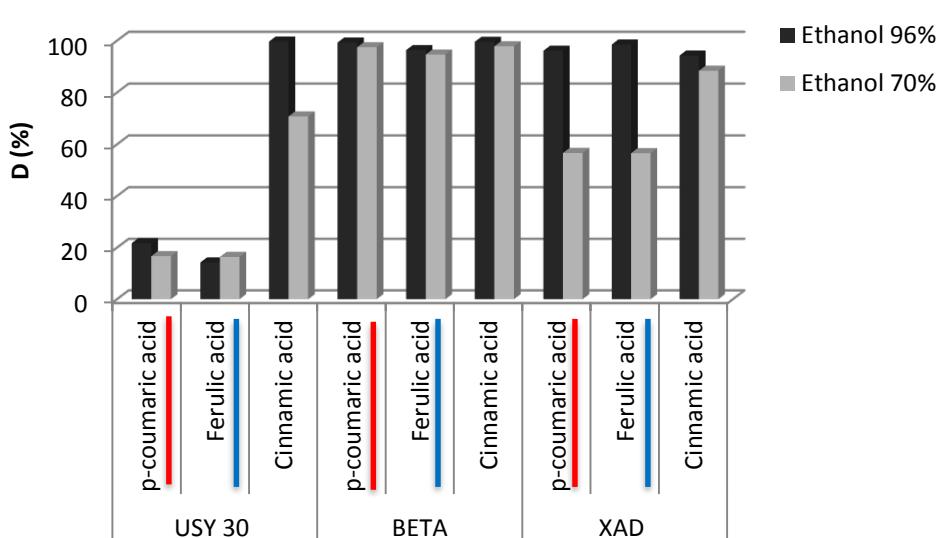
- **Langmuir model** : better description for the adsorption
- **Amberlite XAD16** : less effective than zeolites (factor 3.5-4)
- **Maximum adsorption capacities :**
 - ferulic acid** 139 mg.g^{-1} BETA 29 mg.g^{-1} XAD16
 - p*-coumaric acid** 122 mg.g^{-1} BETA 34 mg.g^{-1} XAD16

Desorption - regeneration

DESORPTION

Solid dried at 60°C-24h, + 2mL desorbing solvent/50mg zeolite)

Mixture : 60°C-3h-1300 rpm



REGENERATION

Decrease of adsorption capacity for the second use (%)

	<i>p</i> -coumaric acid	ferulic acid
USY30	13	14
BETA*	21	23
BETA**	7	9
XAD16	0	11

Zeolite dried at * 140°C and ** 200°C before the second adsorption

- ⇒ Ethanol 96% > ethanol 70%
- ⇒ USY30 → D = 10-20 %
- ⇒ BETA → D ~ 100 %

- ⇒ Loss of zeolite efficiency

Application to vegetable extracts

Hemp wood

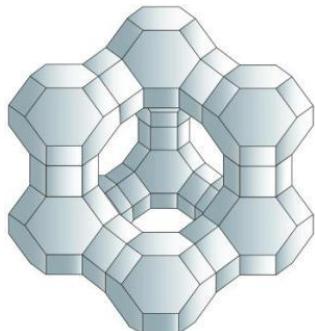


Adsorption rates (%) (contact time 2h)

		<i>p</i> -coumaric acid	ferulic acid
Hemp wood extract <u>(microwave)</u> <i>p</i> -coumaric : ~ 20 mg.L ⁻¹ ferulic acid: < LOQ	USY30	68 ± 6	n.d.
	BETA	94 ± 6	n.d.
	XAD16	8 ± 3	n.d.
Hemp wood extract <u>(twin screw)</u> <i>p</i> -coumaric : ~ 30 mg.L ⁻¹ ferulic acid: < LOQ	USY30	63 ± 5	n.d.
	BETA	92 ± 4	n.d.
	XAD16	n.d.	n.d.
Synthetic solution at 200 mg.L ⁻¹	USY30	51 ± 3	n.d.
	BETA	94 ± 5	n.d.
	XAD16	6 ± 1	n.d.

- ⇒ Presence of other phenolic compounds : does not seem to affect the adsorption of *p*-coumaric acid
- ⇒ Adsorption rates (hemp extracts) equivalent to those obtained from synthetic solution.

Conclusion



USY30 (FAU) and BETA (*BEA) zeolites / XAD16 :
⇒ better adsorption capacities for *p*-coumaric and ferulic acids
⇒ faster adsorption

- Adsorption capacity = $f(pH)$ $pH < pK_{a_1}$
 - Maximum adsorption capacities : BETA 139 mg.g^{-1} ferulic acid
 122 mg.g^{-1} *p*-coumaric acid
 - Desorption (BETA) : close to 100% with ethanol 96%
- ↳ New application of zeolites as adsorbents for high added value molecules (ferulic and *p*-coumaric acids) detected in the plant extracts

