Bioelectrochemical Conversion of Carbon Dioxide to Methane for Biogas Upgrading

Christy M. Dykstra and Spyros G. Pavlostathis School of Civil & Environmental Engineering Georgia Institute of Technology Atlanta, GA 30332-0512, USA

College of Environmental and Chemical Engineering Nanchang Hangkong University Nanchang, Jiangxi Province, P.R. China

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Opportunities for CO₂ reuse and energy recovery in municipal wastewater treatment plants (WWTP), now referred to as Water Resource Recovery Facilities (WRRF)









Bioelectrochemical Systems (BES)



- A, Resistor (MFC) or applied potential (MEC)
- B, Proton exchange membrane
- R1, Reactant in the anode (oxidation half reaction)
- P1, Product in the anode
- R2, Reactant in the cathode (reduction half reaction)
- P2: Product in the cathode

Microbial Fuel Cell (MFC) Produces electrical current

Microbial Electrolysis Cell (MEC)

Produces hydrogen (H₂)

Microbial Electromethanogenesis *Produces methane (CH₄)*

Microbial Electrosynthesis (MES)

Produces 2+ carbon compounds (e.g., acetate, methanol, etc.)

 $2H^{+} + 2e^{-} \rightarrow H_{2}$ $E_{H}^{\circ \prime} = -0.414 \text{ V}$ $CO_{2} + 8H^{+} + 8e^{-} \rightarrow CH_{4} + 2H_{2}O$ $E_{H}^{\circ \prime} = -0.244 \text{ V}$ $CO_{2} + 4H_{2} \rightarrow CH_{4} + 2H_{2}O$ $\Delta E^{\circ \prime} = 0.170 \text{ V}$

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Overall Objective

To develop and test bioelectrochemical systems (BESs) to directly convert CO_2 to CH_4 for anaerobic digester biogas upgrading



Materials & Methods

Batch-fed systems at 22±2°C Hydraulic retention time, 7 days

ANODE

- Carbon felt electrode/SS collector
- Acetate-fed (1.5 g COD/L)
- N₂-flushed headspace
- Potential allowed to fluctuate; measured against an adjacent Ag/AgCl reference electrode
- 300 mL total volume
- 250 mL liquid anolyte (phosphate buffer, pH 7.0; trace minerals; vitamins)
- Inoculated with biofilm-attached carbon felt from an active MFC

CATHODE

- Carbon felt electrode/SS collector
- CO₂-fed (1.6 atm, absolute)
- CO₂-flushed headspace
- Potential fixed at -0.8 V (vs. SHE) using an adjacent Ag/AgCl reference electrode
- 300 mL total volume
- 250 mL liquid catholyte (phosphate buffer, pH 7.0; trace minerals; vitamins)
- Inoculated with a suspended-growth, enriched hydrogenotrophic culture





Materials & Methods

Gases

Pressure transducer GC-TCD for gas composition

Liquids

GC-FID for acetate measurement Dissolved CO_2 measured by sample acidification (6 N H₂SO₄) followed by composition analysis of evolved gas (conditional calibration)

Solids and Biomass

TSS/VSS for suspended biomass Protein analysis of biofilm and suspended biomass

Molecular Analysis

DNA extraction using UltraClean Soil DNA Kit and PowerSoil DNA Isolation Kit (Mo Bio Laboratories, Carlsbad, CA) 16S rRNA gene sequencing (Illumina MiSeq) Phylogenetic analysis using Mega 7.0 software Diversity analyses performed with QIIME 1.9.0 and R



Results

Biocathode performance with respect to:

- Methanogenic inoculum
- □ Hydrogen sulfide (H₂S) gas feed contaminant
- □ Anaerobic digester biogas feed (upgrading)



Biocathode Performance – Effect of Inoculum

Biocathode methanogenic inocula: MM, mixed; EHM, pre-enriched hydrogenotrophic

inoculated

inoculated

EHM-





Dykstra, C.M.; Pavlostathis, S.G. 2017. Methanogenic biocathode microbial community development	t
and the role of Bacteria. Environ. Sci. Technol. 51(9) 5306-5316.	

 0.59 ± 0.03

 0.64 ± 0.19

Biocathode Performance – Effect of Inoculum

Biocathode methanogenic inocula: MM, mixed; EHM, pre-enriched hydrogenotrophic



- Biocathode archaeal communities converged on the same phylotypes, *Methanobrevibacter arboriphilus*
- Inoculum pre-enrichment with H₂/CO₂ selects for methanogens that are also selected for by biocathode conditions (faster biocathode start-up)



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electron shuttle mediators

Oxidized

carbon

Biocathode Performance – Effect of Inoculum

- The bacterial community of a biocathode has a significant effect on archaeal CH₄ production
- Increased biocathode CH₄ production occurs with a bacterial community enriched in:
 - Putative producers of electron shuttles/mediators
 - Proteobacteria
 - Exoelectrogens





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Biocathode Performance – Effect of H₂S



Biocathode Performance – Effect of H₂S

Gas transport between biocathode and bioanode



Dykstra, C., Pavlostathis, S.G. (2017), "Evaluation of gas and carbon transport in a methanogenic bioelectrochemical system (BES)", *Biotechnology & Bioengineering*, 114(5), 961-969.







Beorgia biocathode CH₄ production

Biocathode Performance – Effect of H₂S



- H₂S stimulated total biomass growth in both anode and cathode
- H₂S stimulated SRB growth in the anode biofilm







- SRB phylotypes in the BES2 anode biofilm represented 32% of *Deltaproteobacteria* and 1% of total Bacteria.
- Identified SRB phylotypes include *Desulfobulbus propionicus, Desulfovibrio* sp. and *Syntrophobacterales* spp.





- Day 14: Switched from feeding the biocathode 100% CO₂ to feeding anaerobic digester biogas (53-66% CH₄ and 34-47% CO₂).
- No CH₄ production for the first 2 biogas feedings. However, after the 2 days, the biocathode CH₄ production rate increased substantially.
- Although less total CO₂ was removed during biogasfed cycles than during CO₂-fed cycles, the remaining CO₂ was consistently lower at the end of biogas-fed cycles.
- Hydrogen production occurred after switching to biogas, likely due to the increase in current density and slowed methanogenesis.



- Maximum CH_4 production rate occurred during a biogas-fed cycle (1.85 mmol/d), which was 350% higher than the maximum CH_4 production rate during a CO_2 -fed cycle (0.41 mmol/d).
- No significant correlation between the CH₄ production rate and the initial CO₂ or CH₄ partial pressure.





APPLIED POTENTIAL (V vs. SHE)

- At a more positive applied cathode potential, the cell potential (driving force for electron transport) decreased and the anode potential decreased.
- At lower anode potentials, the transfer of electrons from a substrate to the anode is less energetically favorable.
- However, anode acetate removal did not reflect the biocathode CH₄ production rate, likely due to microbial acetate uptake and storage.

	Mean CH ₄			Anode	Anode	
Cathode	Production	Final	Final	Acetate	Potential	Cell
Potential	Rate ^a	Biocathode	Biocathode	Removal ^a	(V vs.	Potential
(V vs. SHE)	(mmol/d)	CH₄ ª (%)	CO ₂ a (%)	(%)	Ag/AgCl)	(V)
-0.80	1.22 ± 0.07	79.9 ± 1.4	3.7 ± 0.1	21.2 ± 0.3	1.14-1.17	2.28-2.33
-0.75	0.98 ± 0.04	76.1 ± 0.9	4.1 ± 0.1	9.3 ± 1.1	1.09-1.10	2.14-2.17
-0.70	0.87 ± 0.12	78.3 ± 2.5	4.8 ± 0.1	NR ^b	1.04-1.07	2.05-2.08
-0.65	0.97 ± 0.05	78.4 ± 1.0	5.4 ± 0.1	9.1 ± 5.3	1.03-1.04	1.98-2.01
-0.60	0.74 ± 0.04	72.4 ± 0.9	6.2 ± 0.2	13.4 ± 0.4	1.02-1.04	1.93-1.94
-0.55	0.86 ± 0.14	70.7 ± 2.7	6.4 ± 0.1	NR	1.02-1.05	1.88-1.90
-0.50	0.53 ± 0.08	76.7 ± 1.7	8.3 ± 0.1	4.0 ± 0.1	0.16-0.36	1.15-1.34

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^a Mean ± standard deviation; *n* = 3; ^b No removal.

Do biogas components contribute to BES current?

- Other biogas components (CH₄, H₂S and NH₃) may contribute to increasing current and CH₄ production.
- CO₂, CH₄, N₂, H₂ and H₂S can be transported as dissolved gases across a Nafion 117 proton exchange membrane when there is a concentration gradient.¹
- As reduced species, CH₄, H₂S and NH₃ could become oxidized at the bioanode, donating electrons to the electrode and contributing to current production.

¹Dykstra, C., Pavlostathis, S.G. (2017), "Evaluation of gas and carbon transport in a methanogenic bioelectrochemical system (BES)", *Biotechnology & Bioengineering*, 114(5), 961-969.



Do biogas components contribute to BES current?



- At more negative applied cathode potentials, the maximum possible contribution of CH₄, H₂S and NH₃ to the charge transferred during a 1-d feeding cycle was minimal.
- NH₃ was not an important contributor to charge due to its low abundance in biogas.
- At -0.80 V cathode potential, the difference in the amount of charge transferred in the biogas-fed cycle and the CO₂-fed cycle cannot be completely explained by the oxidation of biogas CH₄, H₂S and NH₃ at the anode.
- Changes in microbial community and/or gene expression? (Under investigation)



Conclusions

- The biocathode bacterial community significantly affects archaeal CH₄ production. Exoelectrogenic heterotrophs may promote biocathode CH₄ production within a biofilm fed only with CO₂.
- H₂S, a common biogas contaminant, is transported across the proton exchange membrane from cathode to anode, where it is oxidized and contributes electrons to the anode.
- At low H₂S concentrations (≤ 3%, v/v), H₂S increases biocathode CH₄ production due to increased current. At high H₂S concentrations (≥ 4%, v/v), H₂S may be inhibitory to the methanogenic biofilm and reduce overall biocathode CH₄ production.
- Anaerobic digester biogas was successfully upgraded using a methanogenic bioelectrochemical system.



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For further information contact: S. G. Pavlostathis

E-mail: spyros.pavlostathis@ce.gatech.edu CEE Website: http://www.ce.gatech.edu/people/faculty/961/overview



Extra Slides



Efficiency Calculations

CE, Coulombic Efficiency: The ratio of total Coulombs actually transferred to the anode from the substrate, to maximum possible Coulombs if all substrate removal produced current. ^[1]

CCE, Cathode Capture Efficiency: The ratio of total Coulombs actually transferred to the CH_4 from the cathode, to maximum possible Coulombs if all current produced CH_4 .^[2]

Electrochemical Analyses

Ohm's Law: I = V/R where I is the current, V is the voltage between the anode and cathode and R is the sum of all resistances within the circuit.





Non-reversible rxn



[1] Logan et al., 2006. ES&T; [2] Villano et al., 2013. Bioresource Technol.; [3] http://www.ceb.cam.ac.uk/research/groups/rg-eme/teachingnotes/linear-sweep-and-cyclic-voltametry-the-principles

EFFECT OF CATHODE H₂S ON BES PERFORMANCE

- Corrosive, toxic (NIOSH, IDLH = 100 ppm)
- Produced by sulfate-reducing bacteria during anaerobic digestion and by the breakdown of HScontaining compounds (e.g., cysteine)
- Inhibitory to methanogenesis during anaerobic digestion ^[1]



Desulfovibrio vulgaris

• Feedstock C:S ratio predicts biogas H₂S^[2]

Feedstock	C/S (g/g)	Theoretical Biogas H₂S (%, range)
Grease trap waste	798	0.0-0.1
Biological sludge	59	0.6 - 1.9
Industrial WW biological sludge	46	0.8 – 2.0
Pig bristles	19	2.0 - 4.9
Harvested green seaweed	7	5.5 – 17.7

[1] Chen, Y., et al., 2008. Biores. Technol. 99(10), 4044-4064.

[2] Peu, P., et al., 2012. Bioresource Technol. 121, 419-424.







Linear biocathode CH₄ production during the first 3 days of a feeding cycle



EFFECT OF CATHODE H₂S ON BES PERFORMANCE

Abiotic H₂S Transport within a BES

H₂S Dissolution in the Cathode

- Abiotic BES with Pt-coated carbon cloth cathode and carbon felt anode
- Open circuit conditions
- Magnetically mixed
- 3% H₂S added to the headspace of the cathode
- Cyclic voltammetry from -1.2 V to 0.2 V (vs. Ag/AgCl) at 100 mV/s; Measured current at 0.2 V.

H₂S Transport Across the Membrane

- Abiotic BES with Pt-coated carbon cloth anode and carbon felt cathode
- Open circuit conditions
- Magnetically mixed
- 3% H₂S added to the headspace of the cathode
- Cyclic voltammetry from -1.2 V to 0.2 V (vs. Ag/AgCl) • at 100 mV/s
- Sodium sulfide calibration curve constructed to convert current at 0.2 V vs. Ag/AgCl to sulfide ions



0.02

0.00 0

20

40

TIME (min)

60

80



EFFECT OF CATHODE H₂S ON BES PERFORMANCE



Above 4% $H_2S v/v$, the cathode biofilm is significantly inhibited.

