UNIVERSITAT DE **START-UP OF A SEQUENCING BATCH REACTOR FOR THE** -+-1111 1111-+-BARCELONA **SELECTION OF POLYHYDROXYALKANOATES ACCUMULATING CULTURES BY MEANS OF A CARBON AND NITROGEN DECOUPLING STRATEGY**

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Introduction and objectives

Wastewater treatment plants (WWTPs) are being transformed into resource recovery facilities (RRF). These plants are also known as biorefineries being a network of facilities that integrate biomass into bioproducts as polyhydroxyalkanoates (PHA) ^{[1] [2] [3]}.



This study is focused on the start-up of a SBR select PHA to accumulating reactor microorganisms and determine their PHA accumulation capacity in aerobic batch tests.

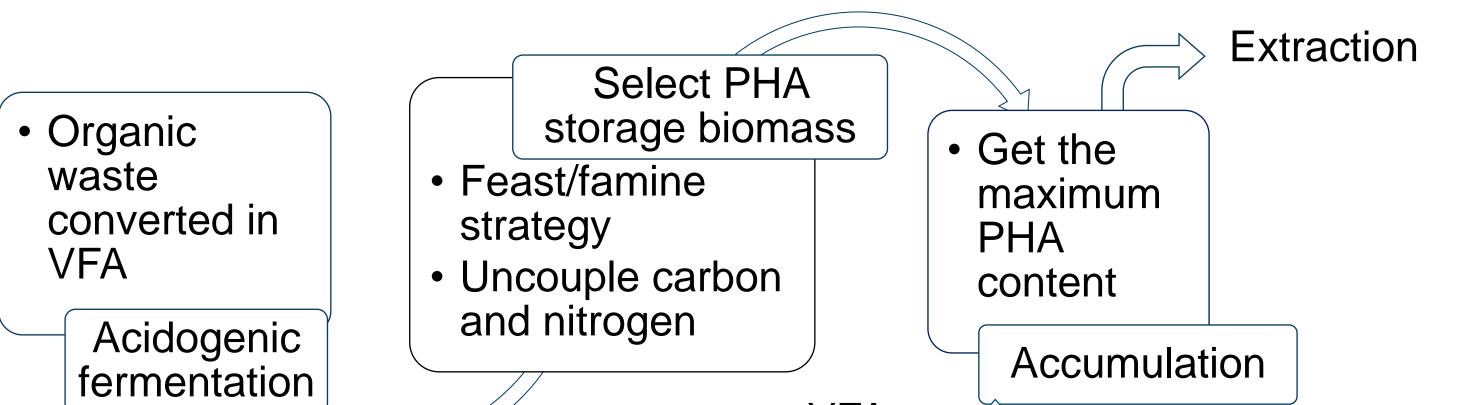




Figure 1. General scheme of the process

Materials and methods

Selection SBR

A sequencing batch reactor (SBR) at 30 °C was used to select PHA accumulating microorganisms. The SBR was inoculated with waste activated sludge (WAS) with 12.3 g TSS ·L⁻¹ and 9.1 g VSS ·L⁻¹.



Table 1. Operating	parameters of SBR
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Parameter	Units	Stage I	Stage II	Stage II
Days of operation	-	1-117	118-169	170-209
HRT	days	1.25	1.25	1.25
SRT	days	4.8	4.8	4.8
Feast/total cycle ratio	% time	>20%	<17%	<17%
Organic loading rate	g COD · L ⁻¹ ·day ⁻¹	2.0	2.0	2.8
VFA feed	g COD · L ⁻¹	2.5	2.5	3.5
Influent acetic acid	% COD	53.1	53.1	53.1
Influent propionic acid	% COD	21.3	21.3	21.3
Influent butyric acid	% COD	25.6	25.6	25.6
NH ₄ +-N loading rate	mg NH ₄ +-N · L ⁻¹ ·day ⁻¹	72	96	96

Accumulation SBR

A reactor of 1.5 L at 30 °C was used for accumulation tests, where the PHA content of the purged biomass of the selection SBR increased following a feed-on-demand strategy.



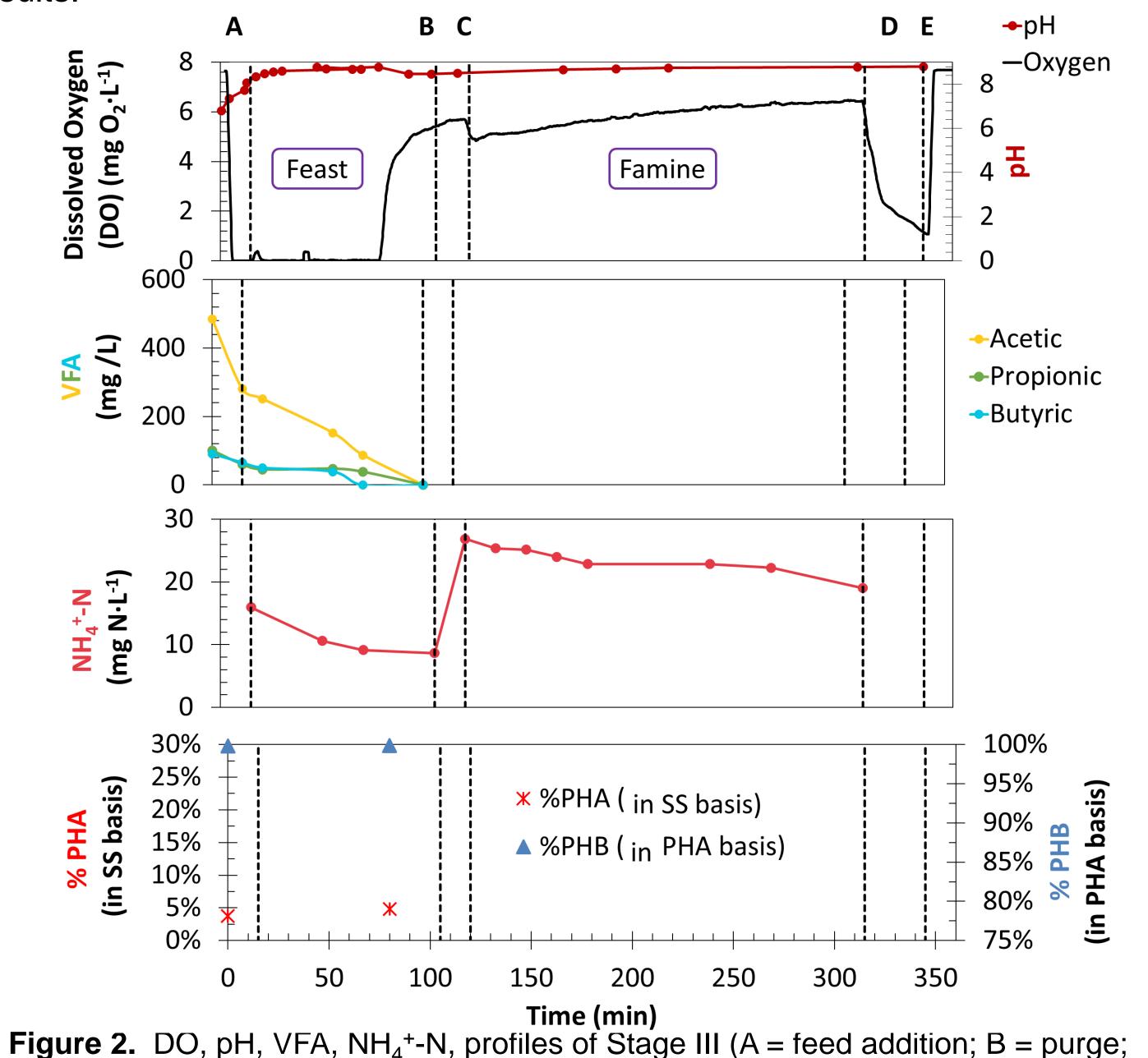
Table 2. Operating conditions of accumulation test

Parameter		Units
SBR purge (inoculum)	800	mL
Duration	7	h
VFA _{feed}	5	gCOD-L ⁻¹
Number of VFA _{feed} spikes	5	-
Volume of VFA _{feed} /spike	100	mL
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Results and discussion

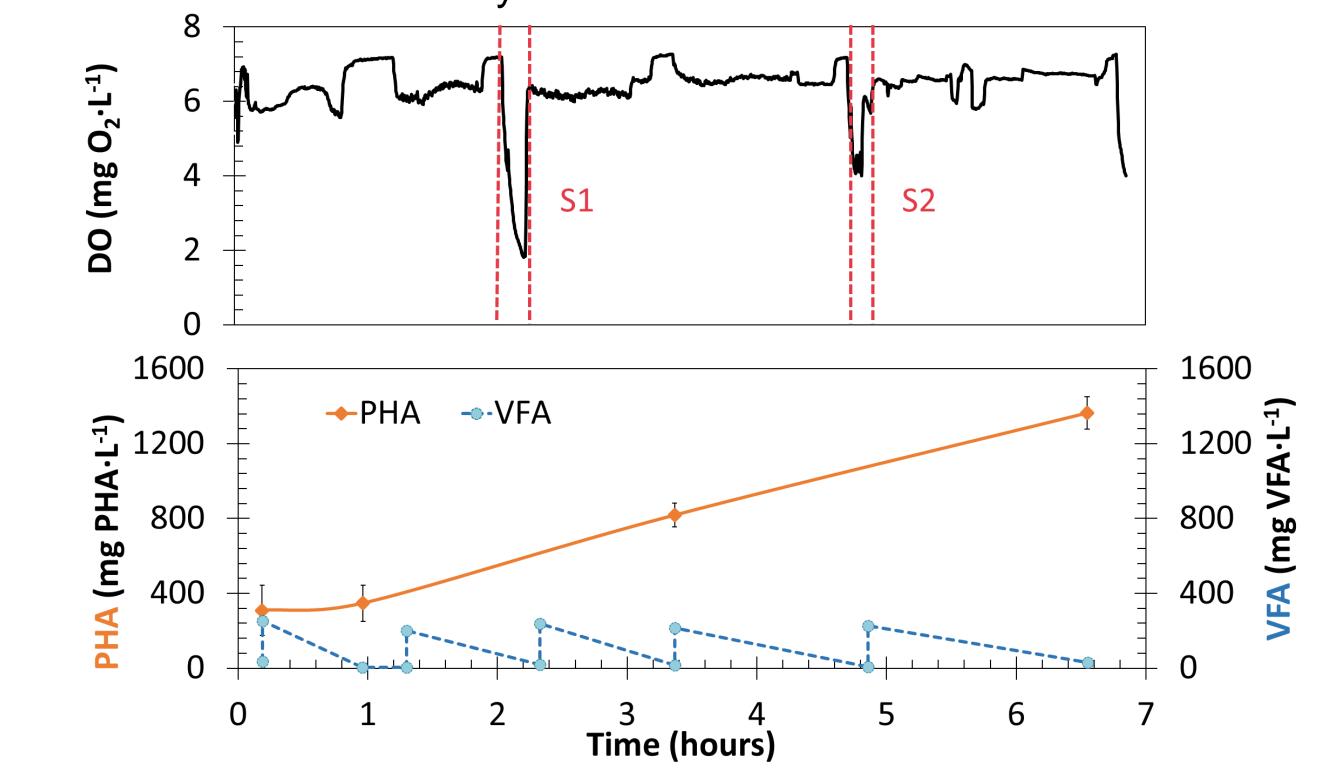
Selection SBR performance

In Stage III, the DO in the feast phase (A-B) was nearly 0 mg·L⁻¹ which means that microorganism consumed the carbon source supplied (VFA). VFA were totally depleted in the purge. Feast phase was much shorter than famine phase (0.17). During the second aerobic phase (C-D) microorganisms consumed the stored PHA together with the NH₄+-N supplied for biomass growth. The PHA concentration measured in the purge had 7% in SS basis in majority as PHB whereas at the beginning was less than 4% in SS. Stage II provided similar results.



PHA Accumulation

The purged biomass obtained in Stage II has a TSS and VSS concentration of 1.59 and 1.45 g·L⁻¹, respectively. Although the VFA dosage was the same in each spike, over time, microorganisms become more satiated and took longer to consume the acids. Microorganisms had an initial intracellular PHA with concentration of 309 ± 134 mg PHA · L⁻¹ (~9% PHA in SS basis) arriving to 1363 ± 8 mg PHA · L⁻¹ (~44% PHA in SS basis) in the last sample of the assay. At Stage III, 46% PHA in SS basis was obtained after accumulation assays.



C = ammonia addition; D = sedimentation; E = effluent discharge) - (Stage III results)

References

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[2] Reis, M., Albuquerque, M., Villano, M., Majone, M.: 6.51 – Mixed Culture Processes for Polyhydroxyalkanoate Production from Agro-Industrial Surplus/Wastes as Feedstocks. Comprehesive Biotechnology (Second Edition), vol. 6, pp. 669-683 (2011) [3] Basset, N., Katsou, E., Frison, N., Malamis, S., Dosta, J., Fatone, F. Integrating the selection of PHA storing biomass and nitrogen removal via nitrite in the main wastewater treatment line. Bioresource Technology, 200, 820-829 (2016).

Figure 3. Accumulation of Stage II of the selective reactor with COD of 5 g COD · L⁻¹ (Stage II results). S1 and S2 represent settling phase.

Conclusions

- ✓ The SBR working conditions at both 2.0 and 2.8 gCOD·L⁻¹ were beneficial for a proper microorganism selection.
- ✓ Accumulation assays showed that **PHA-storing bacteria were** successfully selected in the SBR.
- ✓ The percentage of PHA was above 40% in SS basis, a value that could lead to **commercially viable PHA recovery.**

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