## Specific Methanogenic Activity of anaerobic sludge from different wastewater treatment systems

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Keywords: methane, anaerobic digestion, bioenergy. Presenting author email: julianocuri2015@gmail.com

Anaerobic technology in wastewater treatment is widespread in Brazil, being benefited by climate conditions, besides presenting advantages such as low cost, low solids production, and tolerance to high organic loads. In anaerobic systems occurs the process known as anaerobic digestion, which is the degradation of complex organic matter by microorganisms in the absence of oxygen, producing the biofuel known as biogas, composed mainly of methane (CH<sub>4</sub>), carbon dioxide (CO<sub>2</sub>), water and hydrogen sulfide (H<sub>2</sub>S). However, the monitoring of an adapted biomass with high microbial activity in anaerobic reactors is essential for ensuring the anaerobic process efficiency. Several methods have been proposed to evaluate the anaerobic microbial activity, based on the characterization of Specific Methanogenic Activity (SMA). SMA is defined as the maximum CH<sub>4</sub> production capacity by an anaerobic microbial community (or anaerobic sludge), where the conversion of organic substrates into CH<sub>4</sub> occurs in a controlled manner in laboratory, such as substrate addition and temperature control, in order to favor the metabolism of methanogenic archaea. We aimed to analyze SMA from different anaerobic samples to select the biomass with higher methanogenic capacity for subsequent inoculation in a pilot-scale UASB reactor, in addition to allowing the monitoring of the anaerobic treatment operational performance of different wastewater systems.

This study assessed the SMA of three biomasses from different anaerobic systems: i) a septic tank sludge from a kennel; ii) a prototype UASB reactor sludge for swine wastewater treatment; and iii) a real scale UASB reactor sludge from a wastewater treatment plant (WWTP) treating university sewage. The experiment was performed to evaluate the maximum capacity of the three sludges, under anaerobic conditions and in laboratoryscale bioreactors, in converting organic substrates to CH<sub>4</sub>. After the sampling in each system, the concentration of total volatile solids (TVS) was measured according to APHA (2012), to obtain the volume of sludge to be added to 100 mL flasks, using a substrate/microorganism ratio of 0.5 gCOD/gTVS. The experiment was performed in triplicate. The flasks were sealed with rubber bung and aluminum sealing, maintaining anaerobic atmosphere after the expulsion of oxygen by N2 and incubated at 30±2 °C. Sodium acetate was used as a substrate in combination with macro and micronutrient solutions. The volume of CH<sub>4</sub> daily produced was directly measured through CH<sub>4</sub> volume measurement (Aquino et al, 2007) by washing biogas with NaOH 15%. After 30 consecutive days, accumulated CH<sub>4</sub> volume data was processed in programming language R 3.6.3 for SMA determination. For each anaerobic sludge, a sigmoidal model was adjusted to the observed data (Figure 1). Logistic and Gompertz models were used for comparison and all model coefficients were significant at 0.001 probability. SMA values obtained in mL<sub>CH4</sub> were converted to gCOD<sub>CH4</sub> using stoichiometric conversion factor (F = 394 mL<sub>CH4</sub>.(gCOD<sub>CH4</sub>)<sup>-1</sup>, considering temperature of 30 °C and pressure of 1 atm).

Table 1 presents SMA values obtained for each anaerobic sludge sample, in addition to the TVS values and TVS/TS ratio (Total Solids). The SMA of the prototype UASB sludge sample was the highest (0.045  $gCOD_{CH4}$  (gTVS day)<sup>-1</sup>) among the analyzed sludge samples; however, the inflection point of the curve (Figure 1b) occurred previously (4<sup>th</sup> day) if compared with that of WWTP UASB sludge. This demonstrates that prototype UASB biomass had faster adaptation (or lag phase) to the environment. Likewise, it presented a shorter exponential phase (or log phase), occurring in approximately 6 days (from the 3<sup>rd</sup> to the 9<sup>th</sup> day). This is the phase that occurs the largest methanogenesis activity, allowing to obtain the maximum CH<sub>4</sub> production rate through the higher curve slope. On the other hand, the lag and log phases were longer for WWTP UASB biomass (Figure 1c), which were respectively up to the 8th and 25th days, with a SMA of 0.034 gCOD<sub>CH4</sub>.(gTVS day)<sup>-1</sup> and an inflection point occurring on the 17<sup>th</sup> day. Thus, the phase of higher CH<sub>4</sub> yield occurred in a wider time interval for this sample. These facts explain the higher CH<sub>4</sub> accumulated volume during the test period by the WWTP UASB sludge (100.1  $mL_{CH4}$ ) compared to that of the prototype UASB sludge sample (57.7 mL<sub>CH4</sub>). Furthermore, the curve was better adapted to the data of the WWTP UASB sludge ( $R^2 = 0.9989$ ) in relation to those of the prototype UASB sludge  $(R^2 = 0.9777)$ . SMA values obtained for these two sludge samples from different-scales UASB reactors were according to some results found in the literature. Alves et al (2005) recorded, for swine wastewater biodigester sludge, a SMA of 0.0331 gCOD<sub>CH4</sub>.(gTVS day)<sup>-1</sup>, using the same method used in this study, whereas Almeida et al (2011) reported, for UASB reactor sludge treating dairy wastewater, a SMA of 0.040 gCOD<sub>CH4</sub>.(gTVS day)<sup>-1</sup>. In a previous study carried out by Paez (2019), the value of 0.055 gCOD<sub>CH4</sub>.(gTVS day)<sup>-1</sup> was obtained for the same WWTP UASB sludge used in this study. For domestic sewage, the usual values are in the range of 0.1 to 0.4

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 $gCOD_{CH4.}(gTVS day)^{-1}$  (Chernicharo, 2007). Regarding the sludge sample from the kennel septic tank, despite the similarity of its curve shape (Figure 1a) with that of the WWTP UASB sludge, it presented a SMA of 0.007  $gCOD_{CH4.}(gTVS day)^{-1}$  and a CH<sub>4</sub> accumulated yield of 9.1 mL<sub>CH4</sub>, low values comparing with those achieved by the other two sludge samples tested and those found in the literature.

WWTP UASB sludge presented higher CH<sub>4</sub> accumulated yield in a longer log phase period, despite not presenting the highest SMA among the samples. Therefore, we concluded that it is the most suitable sludge to be used as inoculum for the pilot-scale UASB reactor, which will possibly allow higher substrate (wastewater) degradation efficiency and biogas yield.

Table 1. SMA of the anaerobic sludge samples and their respective values of TVS concentration, TVS/TS ratio, and CH<sub>4</sub> accumulated yield.

Sludge sample	TVS (g L <sup>-1</sup> )	TVS/TS ratio	CH4 accumulated yield (mL)	SMA (gCOD <sub>CH4</sub> .(gTVS day) <sup>-1</sup> )
Kennel tank septic	47.3	0.45	9.1	0.007
Prototype UASB	30.8	0.42	57.7	0.045
WWTP UASB	49.7	0.36	100.1	0.034



Figure 1. Sigmoidal curves adjusted to CH<sub>4</sub> accumulated daily yield data over 30 days of SMA testing, for the following sludge samples and respective adjustment models: (a) kennel tank septic and (b) prototype UASB, both adjusted by the Gompertz model; and (c) WWTP UASB, by the Logistic model.

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