

# USE OF WASTEWATER TREATMENT PLANT BIOGAS FOR THE OPERATION OF SOLID OXIDE FUEL CELLS (SOFCs)

*P. Champagne<sup>a,b,c</sup>, J. Lackey<sup>a,c</sup>, B. Peppley<sup>b,c</sup>*

*<sup>a</sup>Department of Civil Engineering Queen's University*

*<sup>b</sup>Department of Chemical Engineering Queen's University*

*<sup>c</sup>Queen's – RMC Fuel Cell Research Centre*

*Kingston, Ontario, Canada*

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# PROJECT BACKGROUND

- Biogas from WWTPs is a readily available fuel source that when used in SOFC's is often considered 'carbon neutral'
- Biogas can be reformed to increase hydrogen concentration and reduce constituents that are harmful to SOFC technologies
- Biogas that is variable in composition may damage or starve SOFCs
- Knowing typical and extreme concentration ranges is important

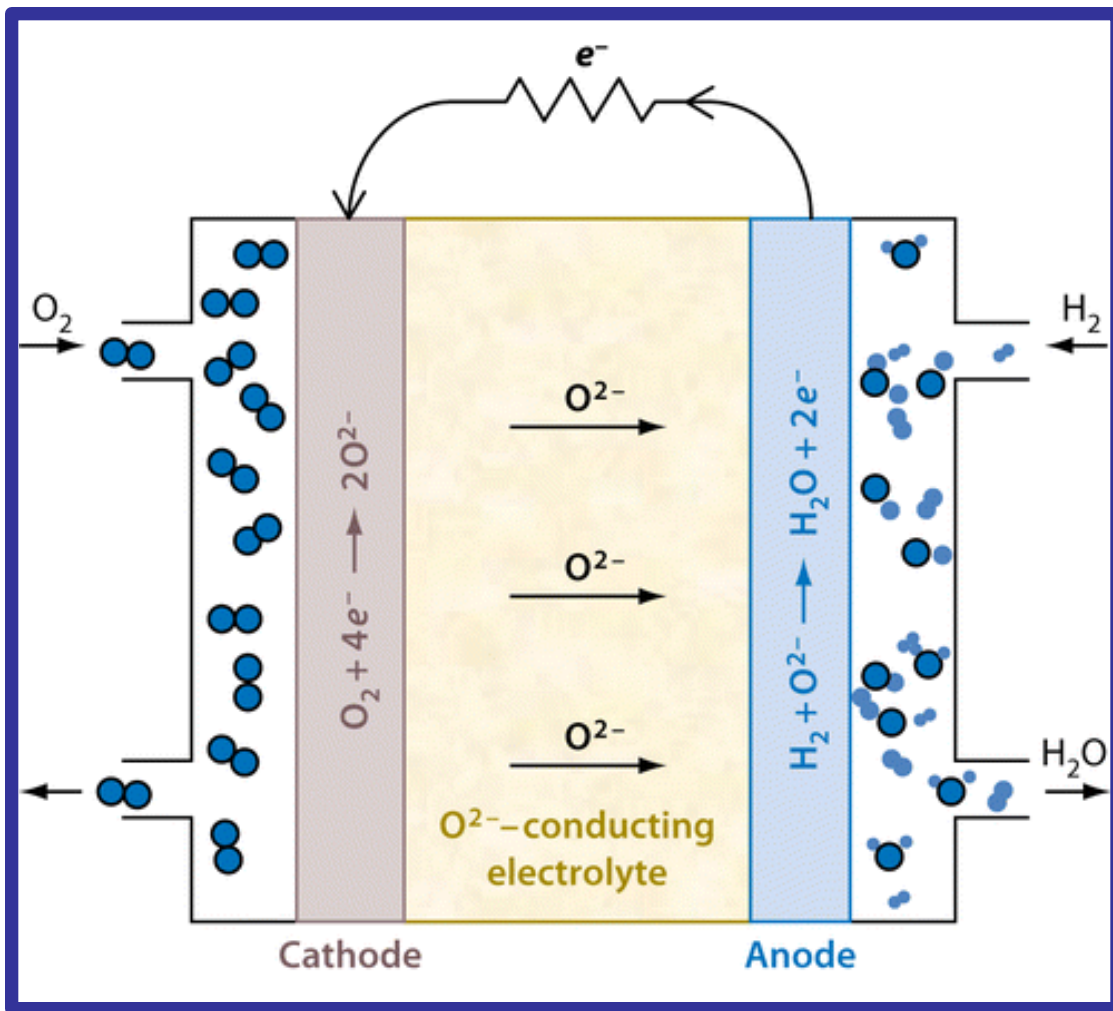


# Kingston Ontario Application

- Utilities Kingston is taking pro-active measures to reduce its environmental footprint
  - The Kingston Ravensview WWTP currently processes approximately 19,000 m<sup>3</sup> of wastewater per day and uses over 4 million kWh per year of electrical power
  - The installation of a waste-to-energy system at the Kingston Ravensview WWTP could offset electrical needs as well as assist with the heat requirement of the anaerobic digesters, further reducing electrical needs
- This research project will result in the construction of a pilot scale plant at the Utilities Kingston Ravensview WWTP and a lasting relationship between the City of Kingston and renewable energy sources



# FUEL CELL BASICS



- Anode material is: Ni-YSZ
- Cathode material is: LSM
- Solid electrolyte material is: YSZ

Catalysis in Solid Oxide Fuel Cells. *Annual Review of Chemical and Biomolecular Engineering*. JULY 2011, Vol. 2 / 10.1146

# PROJECT OUTLINE

- **Task 1:** Compile biogas variability data across North America to determine fuel composition
- **Task 2:** Determine the sensitivity of a SOFC to fuel dilution that is typically found in biogas produced by AD
- **Task 3:** Simulate expected system performance and GHG emissions when operating on dilute H<sub>2</sub>
- **Task 4:** Conduct testing with simulated biogas reformat

# Task 1

## Biogas Variability

Lackey, J., A. Maier, P. Champagne\* and B. Peppley (2015) *A Review of Biogas Composition and Uses in North America*. Waste Management and Research (*In Press*)

# TASK 1: BIOGAS VARIABILITY

Voluntary survey of WWTPs in North America produced the following data:

Compound	# Urban Areas	Average	Standard Deviation	Median	Minimum	Maximum	Average Variability	Max Variability
Methane (CH <sub>4</sub> )	16	63%	2%	63%	50%	69%	9%	28%
Carbon Dioxide (CO <sub>2</sub> )	15	37%	4%	38%	24%	45%	14%	38%
Nitrogen (N <sub>2</sub> )	13	1%	2%	0.3%	0.0%	9%	N/A	N/A
Oxygen (O <sub>2</sub> )	12	0%	0.7%	0%	0%	3%	N/A	N/A
Hydrogen Sulphide (H <sub>2</sub> S)	14	134ppm	186ppm	18ppm	0ppm	855ppm	258%	651%
Si Equivalence	11	12ppm	10ppm	10ppm	0.2ppm	38ppm	137%	340%

- Urban areas with populations above 150,000 in the U.S. and above 50,000 in Canada were solicited
- Data was reported from 16 different locations

# TASK 1: BIOGAS VARIABILITY

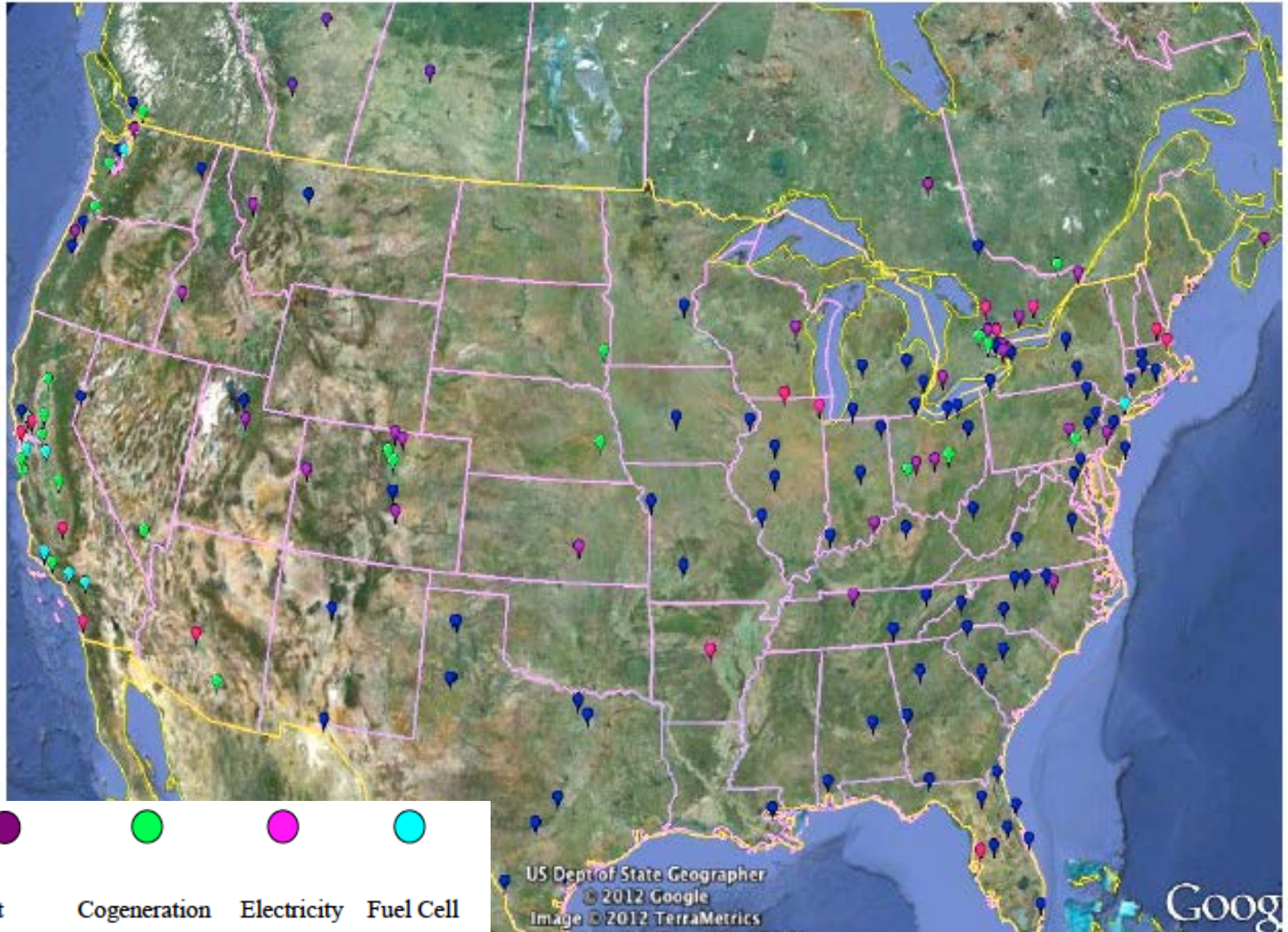
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- CH<sub>4</sub> and CO<sub>2</sub> variability are not significant concerns
  - Lower variability than more poisonous compounds
- H<sub>2</sub>S and Si compound variability are more troublesome

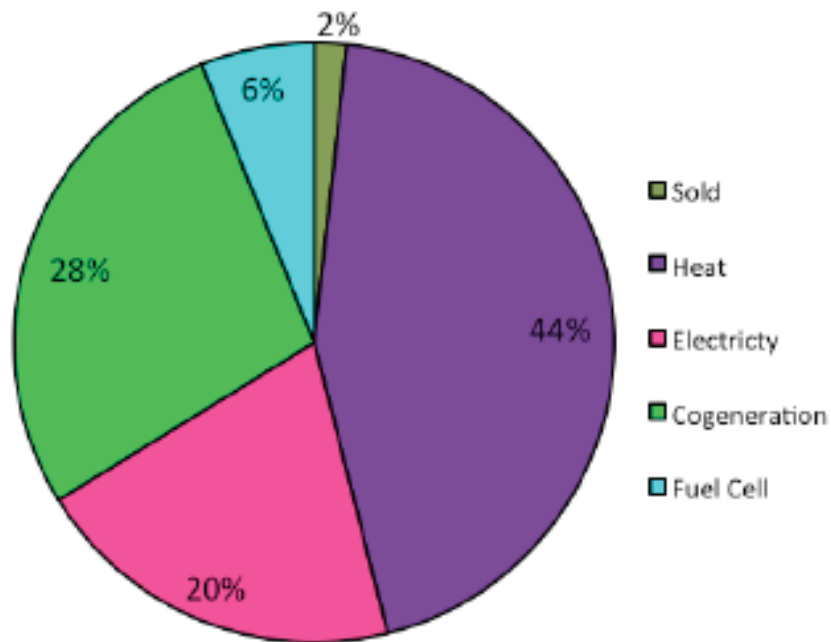


# TASK 1: BIOGAS VARIABILITY



Unknown Heat Cogeneration Electricity Fuel Cell

# TASK 1: BIOGAS VARIABILITY



- Few trends in biogas composition
  - Sociopolitical trends in some regions
- Heat is the predominant end use of biogas
  - Most prevalent in Northern states
  - Population trends with respect to biogas end use

# Task 2

## SOFCs Operating on Dilute H<sub>2</sub>



# TASK 2: SOFCs OPERATING ON DILUTE H<sub>2</sub>

N<sub>2</sub>, Ar and CO<sub>2</sub> were used as diluents at concentrations of 65%, 25% and 10% H<sub>2</sub> + 2.3mol% H<sub>2</sub>O as steam + diluent

## Cell Characteristics:

Ni-YSZ anode  
LSM cathode  
YSZ electrolyte

## Test Characteristics:

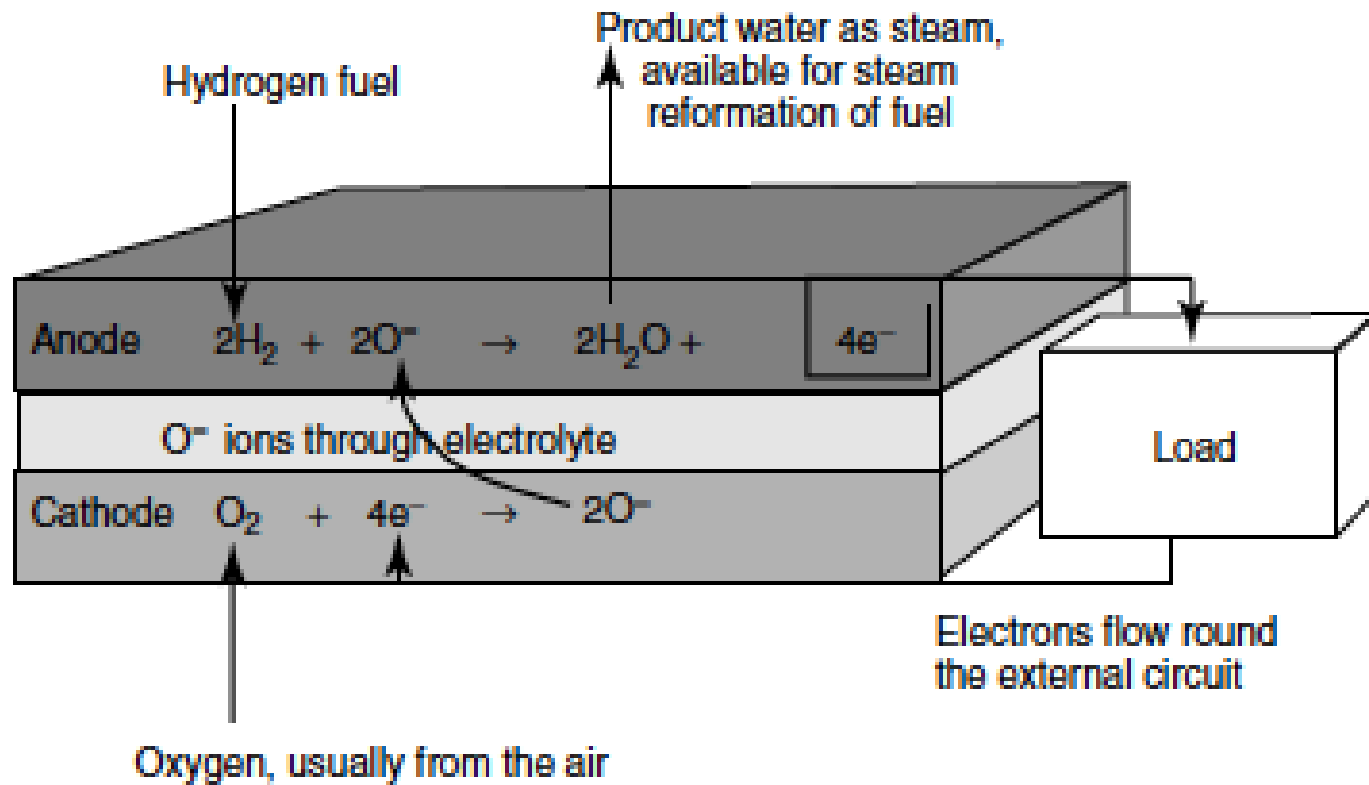
800° C  
1 bar  
80% Fuel utilization  
20% Oxidant utilization



Jiang *et al.* Journal of the Electrochemical Society 2003, 150 (7) A942.

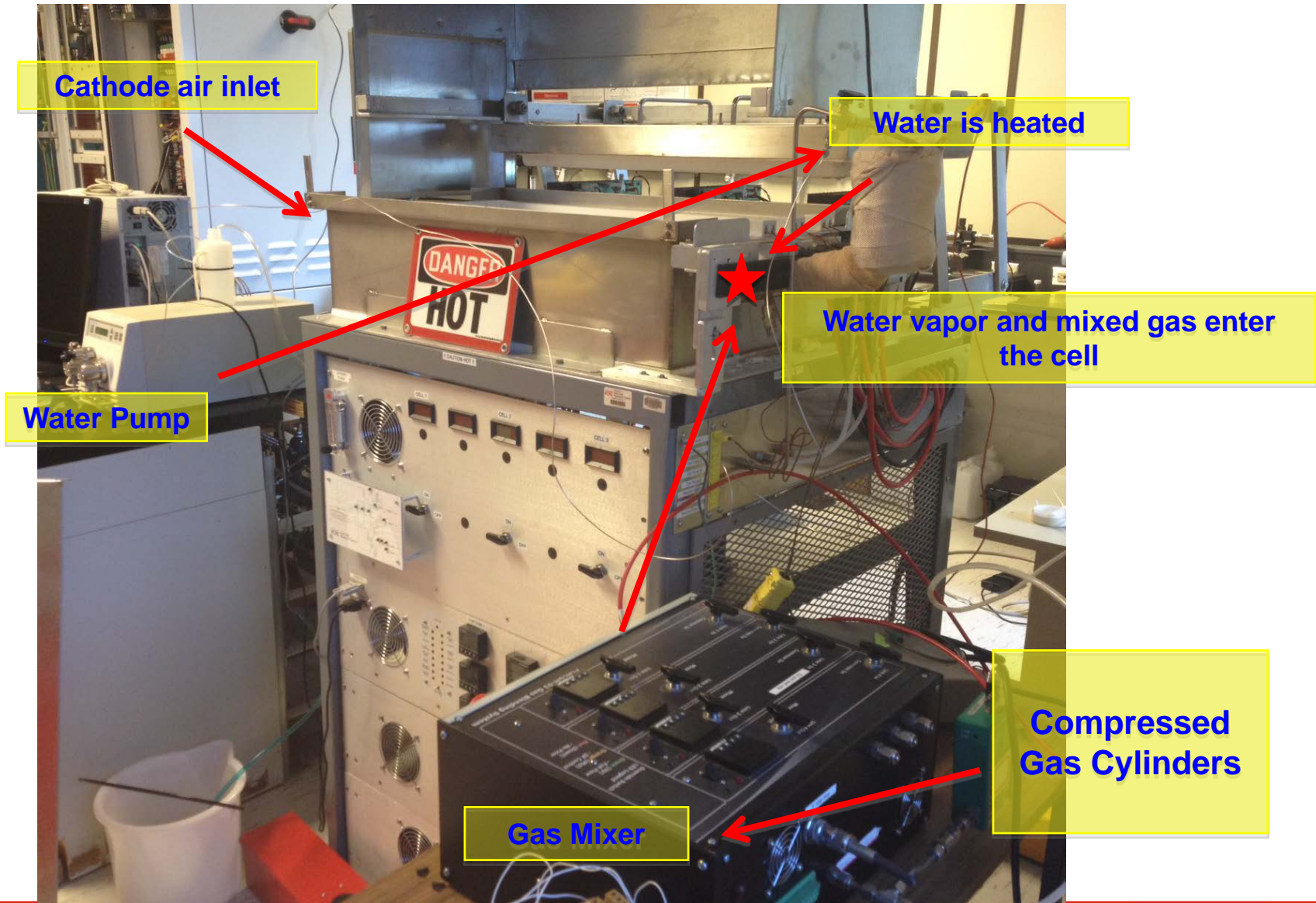


# TASK 2: SOFCs OPERATING ON DILUTE H<sub>2</sub>



Larminie *et al.* *Fuel Cell Systems Explained* 2003, 2, 208.

# TASK 2: SOFCs OPERATING ON DILUTE H<sub>2</sub>



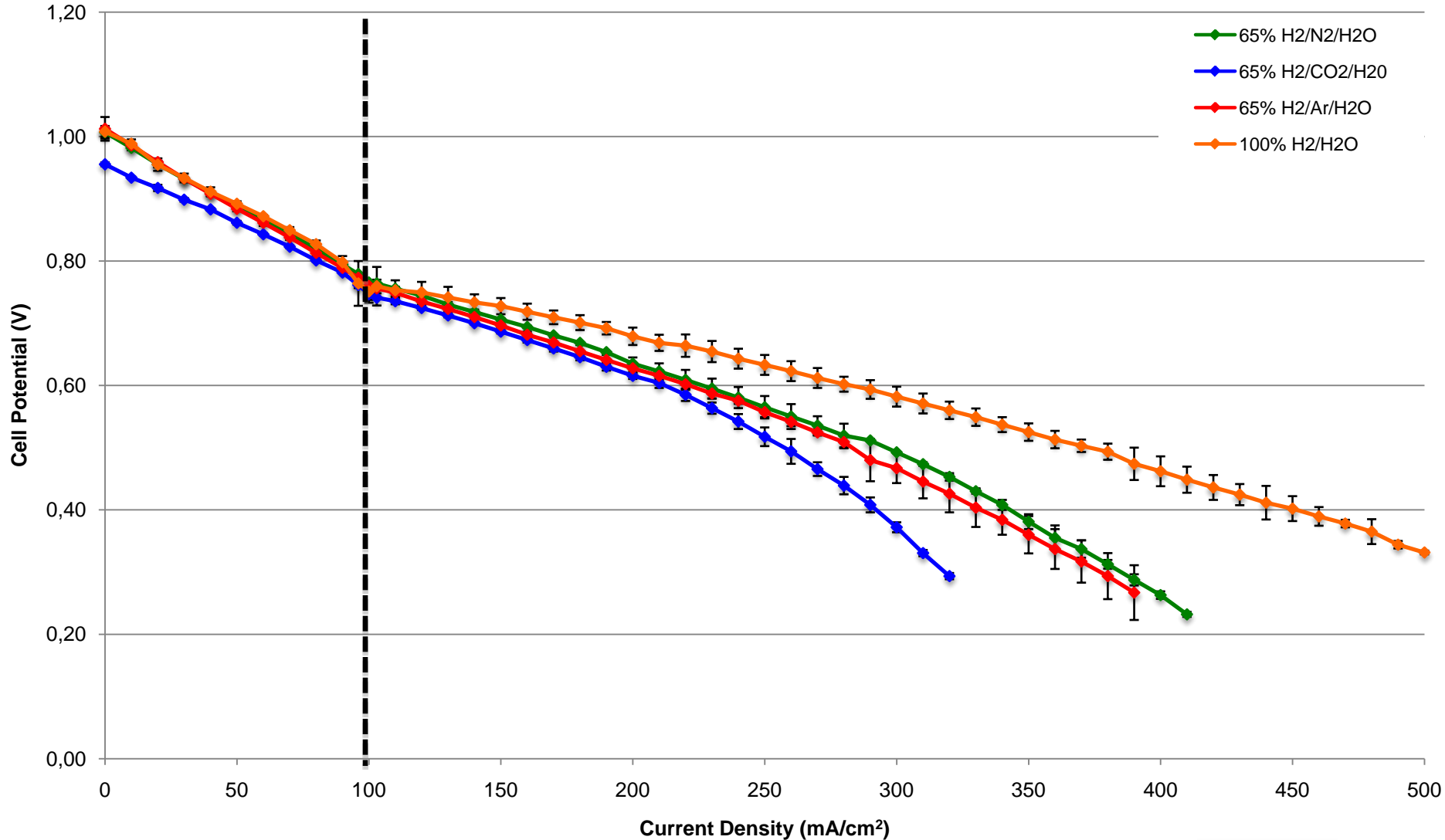
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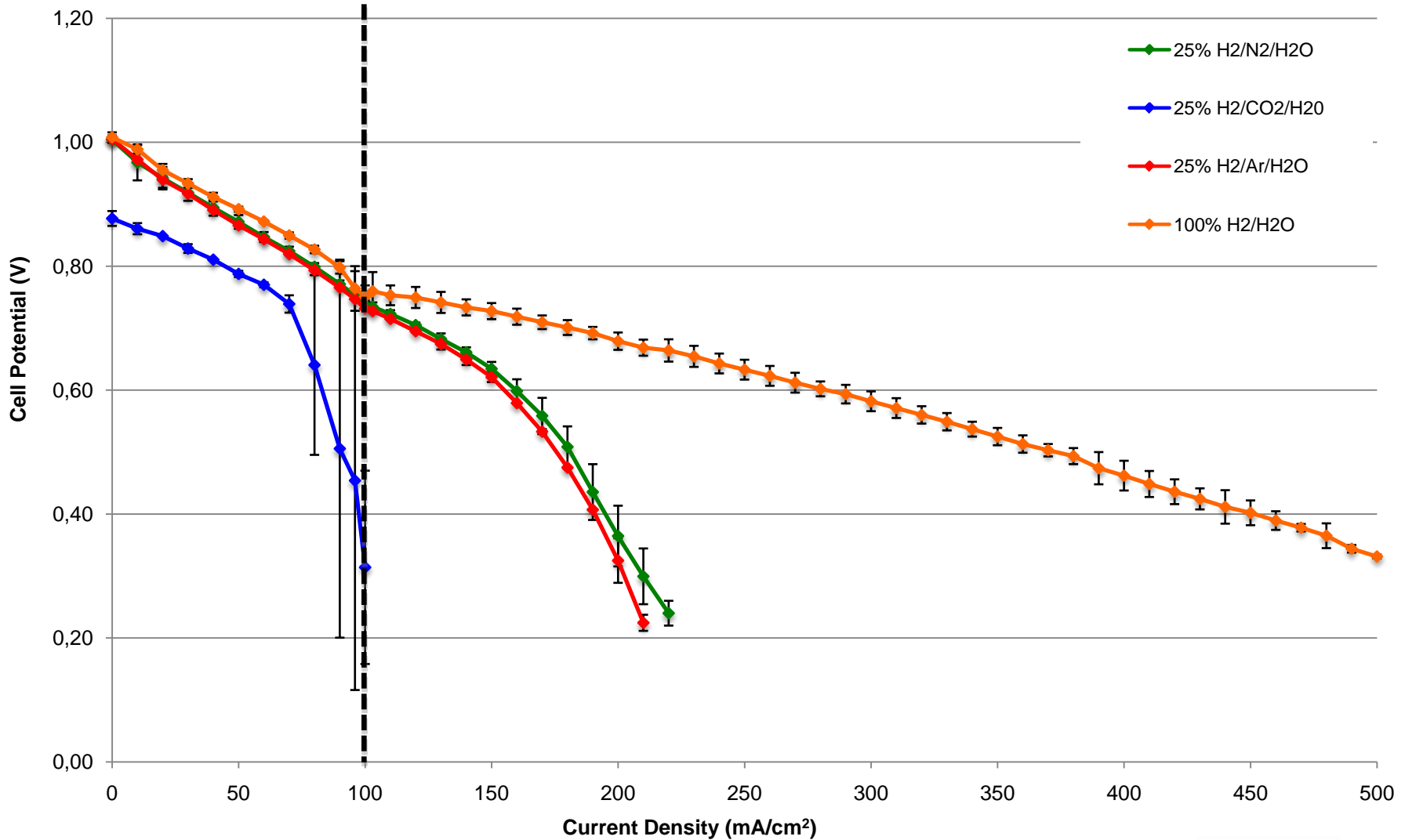
## 65% H<sub>2</sub> Cell Potential





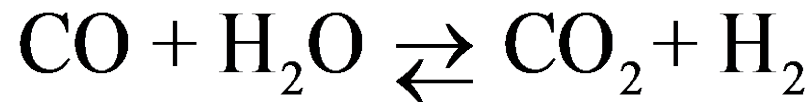
# TASK 2: SOFCs OPERATING ON DILUTE H<sub>2</sub>

## 25% H<sub>2</sub> Cell Potential



## TASK 2: SOFCs OPERATING ON DILUTE H<sub>2</sub>

- Dilute H<sub>2</sub> tests were designed to assist with the prediction of cell performance when operating on simulated WWTP biogas reformat
- The water-gas shift (**WGS**) reaction can produce or consume H<sub>2</sub> depending on the reactants



- Contributes to decreased cell performance in the presence of CO<sub>2</sub> as a diluent

# Task 3

# SOFC System Simulation

# TASK 3: SOFC SYSTEM SIMULATION

- Model developed to simulate system performance using dilute H<sub>2</sub> data
- Empirical model was incorporated into the computer simulation developed in UniSIM

$$V = C_1 + C_2 \ln \left( \frac{P_{H_2}^{0.5} P_{O_2}}{P_{H_2O}} \right) - C_3 i + C_4 \ln \left( 1 - \frac{P_{CO_2}}{P_{Total}} \right)$$

Parameter	Parameter Value
C1	0.9130 V
C2	0.0168 V
C3	0.0016 kΩcm <sup>2</sup>
C4	0.0229



# TASK 3: SOFC SYSTEM SIMULATION

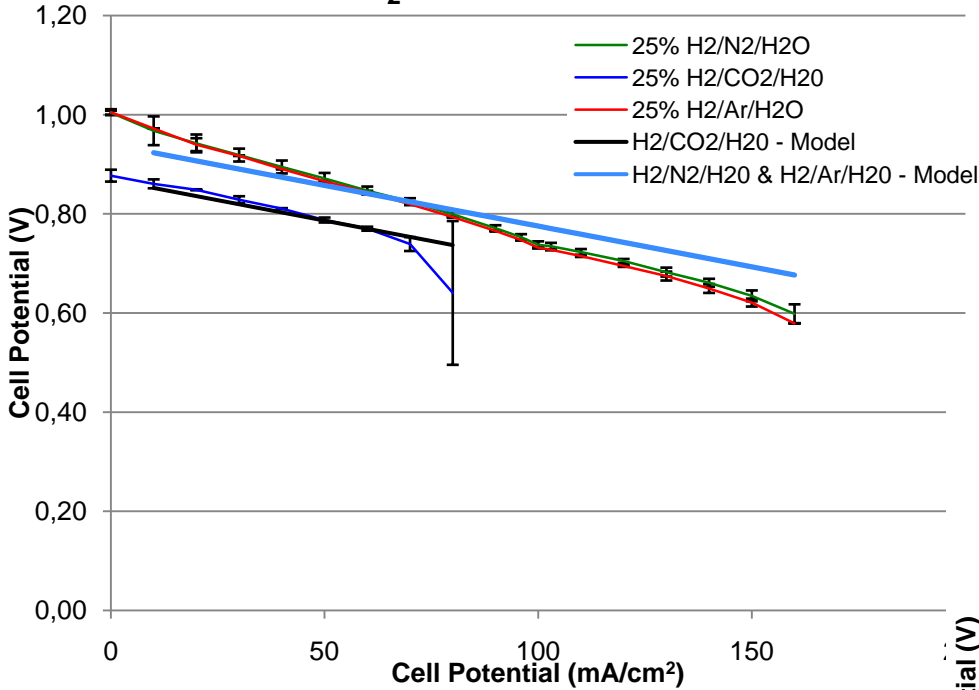
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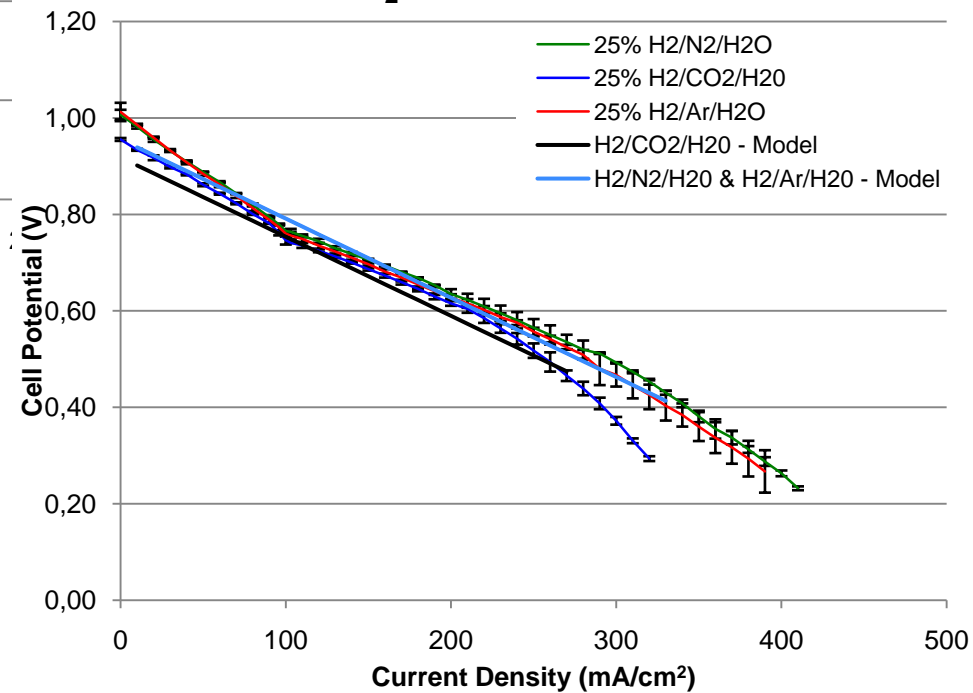
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# TASK 3: SOFC SYSTEM SIMULATION

## 25% H<sub>2</sub> with Diluent Tests



## 65% H<sub>2</sub> with Diluent Tests

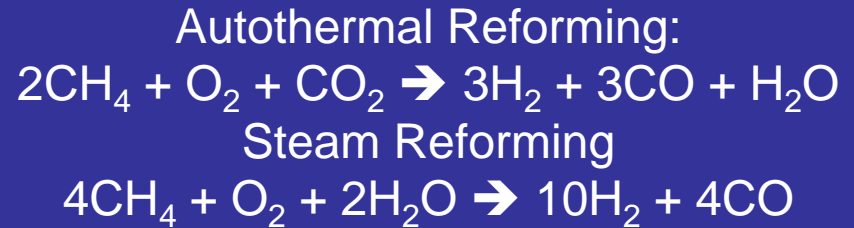
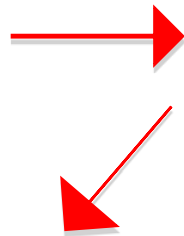


# Task 4

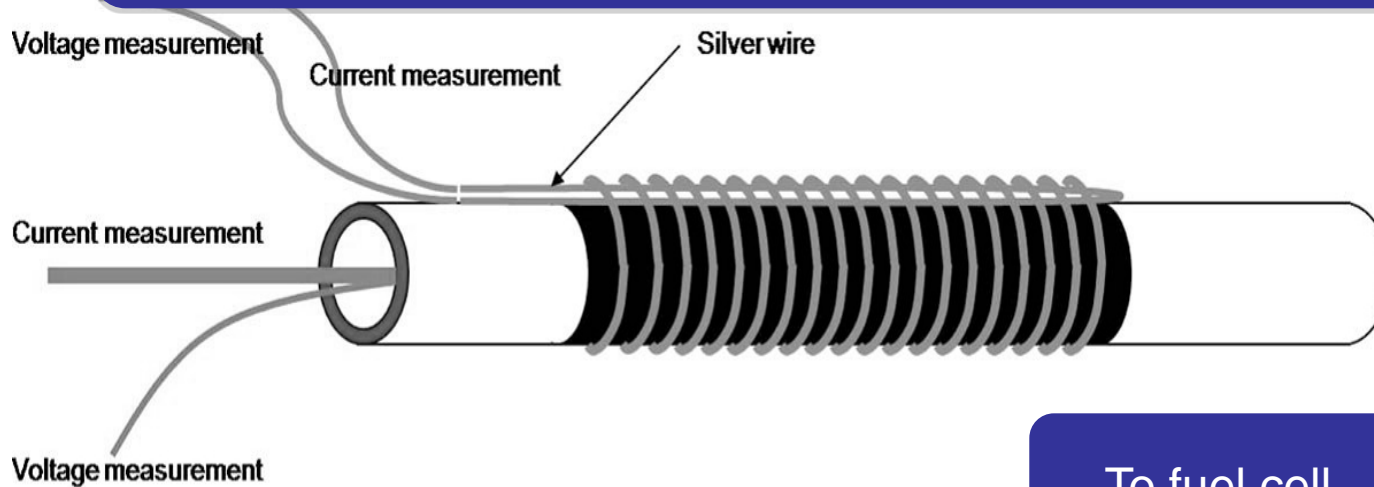
## Operation on Simulated Biogas Reformate

# DATA COLLECTION

AD-derived WWTP biogas: 58-70% CH<sub>4</sub>, 30-43% CO<sub>2</sub> and 1.2-7.1% N<sub>2</sub> with trace quantities of H<sub>2</sub>S, O<sub>2</sub>, H<sub>2</sub>O, CO and Si compounds



Simulated biogas reformate mixture was developed using UniSim software:  
66.7% H<sub>2</sub>, 16.5% CO<sub>2</sub>, 16.2% CO and 0.7% N<sub>2</sub>



Addition of H<sub>2</sub>O at 2.3% or 20mol% of total fuel flow rate

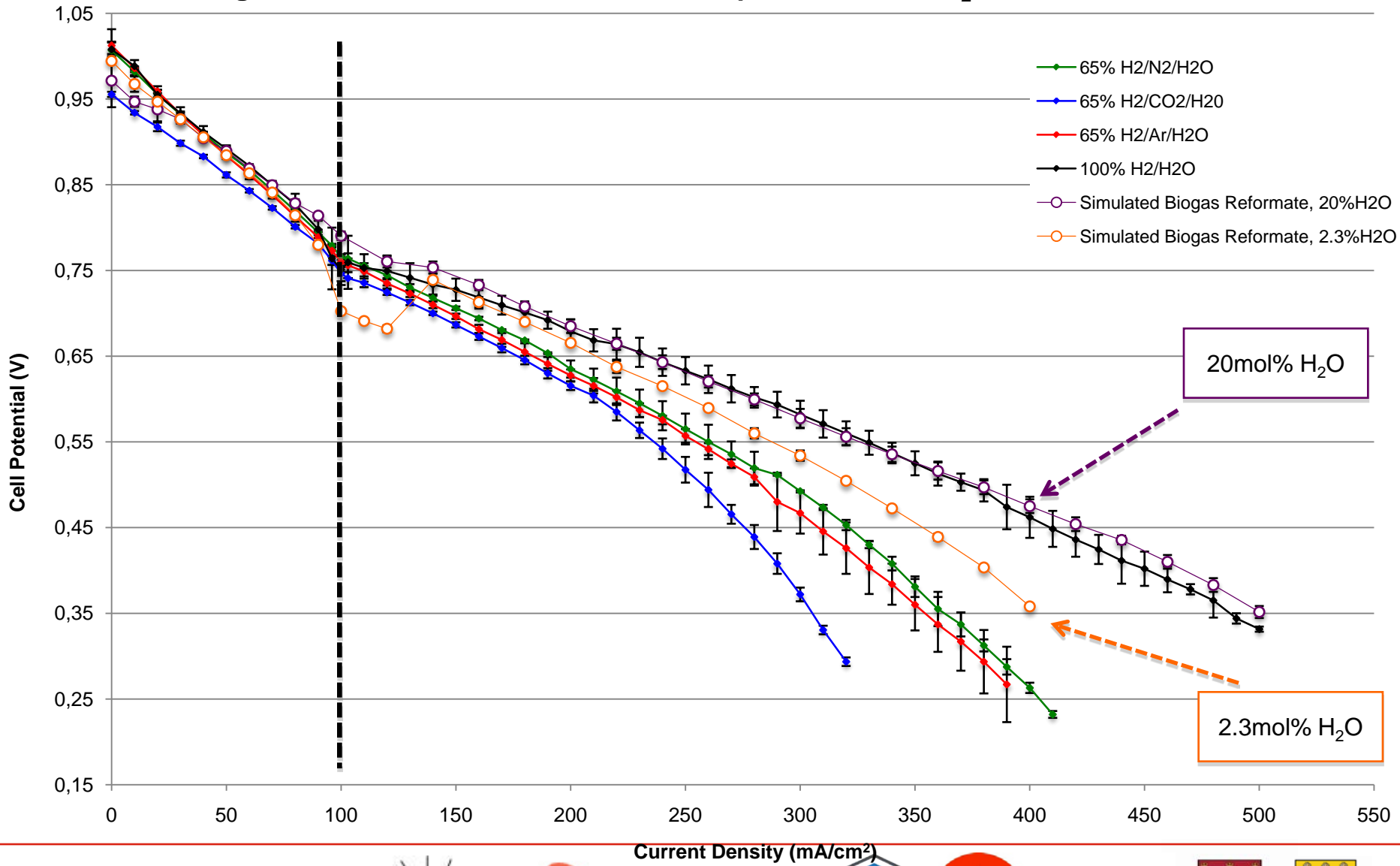
To fuel cell

Song *et al.* Journal of Fuel Cell Science and Technology 2010, 7, 97.



# TASK 4: OPERATION ON SIMULATED BIOGAS REFORMATE

## Biogas Reformate Cell Performance Compared to Dilute H<sub>2</sub> Cell Performance



# TASK 4: OPERATION ON SIMULATED BIOGAS REFORMATE

- Increased cell performance when operating on the simulated biogas reformat mixture is due the forward WGS reaction producing  $H_2$  in the presence of CO and  $H_2O$
- Tests conducted with 20mol%  $H_2O$  showed increases in cell performance that can be attributed to the presence of additional  $H_2O$ 
  - Increased reaction rate:

$$K = \frac{[CO_2][H_2]}{[CO][H_2O]}$$

# Conclusions

- Biogas composition is variable from site to site
- Dilution testing helped understand the cell performance decreases that occur when H<sub>2</sub> concentration decreases
  - **Recommendation:** Conduct tests using CO as a diluent gas
- Dilution model predicted system performance and efficiency when dilute H<sub>2</sub> was used as a fuel
  - **Recommendation:** Adapt to simulation to predict performance of a pilot scale system; include thermal efficiency
- Simulated biogas reformat tests showed good cell performance
  - **Recommendation:** Complete pilot scale testing at Ravensview WWTP



# Questions?